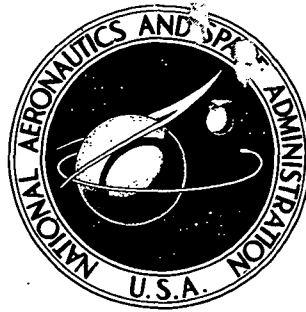


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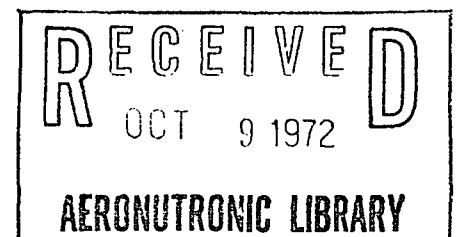


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A PROGRAM FOR CALCULATING  
EXPANSION-TUBE FLOW QUANTITIES  
FOR REAL-GAS MIXTURES AND  
COMPARISON WITH EXPERIMENTAL RESULTS

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A PROGRAM FOR CALCULATING EXPANSION-TUBE  
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SUMMARY

A computer program written in FORTRAN IV language is presented which determines expansion-tube flow quantities for real test gases  $\text{CO}_2$ ,  $\text{N}_2$ ,  $\text{O}_2$ , Ar, He, and  $\text{H}_2$ , or mixtures of these gases, in thermochemical equilibrium. The effects of dissociation and first and second ionization are included. Flow quantities behind the incident shock into the quiescent test gas are determined from the pressure and temperature of the quiescent test gas in conjunction with (1) incident-shock velocity, (2) static pressure immediately behind the incident shock, or (3) pressure and temperature of the driver gas (imperfect hydrogen or helium). The effect of the possible existence of a shock reflection at the secondary diaphragm of the expansion tube is included. Expansion-tube test-section flow conditions are obtained by performing an isentropic unsteady expansion from the conditions behind the incident shock or reflected shock to either the test-region velocity or the static pressure. Both a thermochemical-equilibrium expansion and a frozen expansion are included. Flow conditions immediately behind the bow shock of a model positioned at the test section are also determined. Results from the program are compared with preliminary experimental data obtained in the Langley 6-inch expansion tube.

A listing of the program is presented along with a description of required inputs, a flow chart, and sample data printouts. Some typical solutions are presented for  $\text{CO}_2$ , Ar, and air and for Mars, Venus, and Jovian atmospheric models.

INTRODUCTION

Several experimental studies to be performed in the Langley 6-inch expansion tube will use various gas mixtures as test media at hypersonic conditions. Before such studies are performed, it is essential to ascertain the theoretical performance of the expansion tube for the gas mixture being tested. The wide range of flow conditions and the very short test times of the expansion tube impose rather stringent requirements on facility instrumentation. Thus, in preparing the facility for a test, it is necessary that the magnitude of the physical quantities to be measured be known to within reasonable limits.

Following a test, it is desirable to have convenient means for determining expansion-tube flow quantities from the measured flow quantities.

Relatively little effort has been directed towards the calculation of expansion-tube flow quantities for arbitrary gas mixtures. One such study, reported in reference 1, is basically a shock-tube program which can generate expansion-tube flow conditions. However, several effects which may markedly alter calculated flow quantities are not included in the program of reference 1. Also, the program of reference 1 requires inputs other than the actual flow quantities measured during a test.

A primary purpose of the present study is to fulfill the need for a convenient, versatile program for determining expansion-tube flow quantities in real gases  $\text{CO}_2$ ,  $\text{N}_2$ ,  $\text{O}_2$ , Ar, He, and  $\text{H}_2$  or mixtures of these gases from several combinations of routinely measured flow quantities. Included in this program are the effect (ref. 2) of an imperfect (intermolecular force) driver gas (helium or hydrogen), the possible existence of a shock reflection at the secondary diaphragm (ref. 3), and the calculation of both a thermochemical-equilibrium expansion and a frozen expansion. Flow quantities immediately behind the bow shock of a test model, including stagnation-point heat-transfer rate, are calculated.

## SYMBOLS

The International System of Units (SI) is used for all physical quantities in the present study. Conversion factors relating SI Units to U.S. Customary Units are given in reference 4.

a	speed of sound, m/sec
B	second virial coefficient, $\text{m}^3/\text{kg}$
C	third virial coefficient, $(\text{m}^3/\text{kg})^2$
$c_p W_0/R$	nondimensional specific heat at constant pressure
$c_v W_0/R$	nondimensional specific heat at constant volume
h	specific enthalpy, $\text{m}^2/\text{sec}^2$ (J/kg)
$h_0$	standard heat of formation at $T = 0 \text{ K}$ , J/kmol
M	Mach number, $U/a$

$M_S$	incident-shock Mach number, $U_S/a$
$N_{Re}$	Reynolds number per meter, $\rho U/\mu$
$p$	pressure, $N/m^2$
$\dot{q}$	heat-transfer rate, $W/m^2$
$R$	universal gas constant, $8.31434 \text{ kJ/kmol-K}$
$r$	nose radius, $m$
$sW_O/R$	nondimensional specific entropy
$T$	temperature, $K$
$U$	velocity, $m/sec$
$U_S$	velocity of incident shock, $m/sec$
$W$	molecular weight, $kg/kmol$
$W_O$	molecular weight of undissociated gas or gas mixture, $kg/kmol$
$X_i$	mole fraction, $kmol$ of species $i$ per $kmol$ of mixture
$Y_i$	number of $kmol$ s of species $i$ per mass of mixture, $kmol$ of species $i$ per $kg$ of mixture
$Z$	compressibility factor, $pW_O/\rho RT$
$Z^*$	number of $kmol$ s of dissociated gas mixture per number of $kmol$ s of undissociated gas mixture, $W_O/W$
$\gamma$	ratio of specific heats
$\gamma_E$	isentropic exponent, $\left(\frac{\partial \log p}{\partial \log \rho}\right)_{sW_O/R}$
$\eta_i$	parameter defined in equation (25), $kg/m^{3/2}\text{-sec}\text{-(N/m}^2)^{1/2}$

$\mu$  viscosity, N-sec/m<sup>2</sup>

$\rho$  density, kg/m<sup>3</sup>

Subscripts:

A denotes region (2) for no standing shock at secondary diaphragm or region (2,s) for a standing shock

act active or available

f frozen

i individual species

mix mixture

perf perfect-gas behavior

ref reference state

w model-wall conditions

1 state of quiescent test gas in front of incident normal shock

2 state of test gas behind incident normal shock in intermediate section

2,s state of test gas behind shock at secondary diaphragm

3 state of expanded driver gas

4 driver-gas conditions at time of primary-diaphragm rupture

5 state of test gas flow in acceleration section (free-stream conditions)

5,s static conditions behind bow shock of model positioned at expansion-tube test section

5,t stagnation conditions behind bow shock of model positioned at expansion-tube test section

4

- 10 state of quiescent acceleration gas in front of incident normal shock
- 20 state of acceleration gas behind incident normal shock in acceleration section

Approximate value is denoted by superscript  $\sim$ .

## ANALYSIS AND PROCEDURE

Before the procedures for determining expansion-tube flow quantities are discussed, a brief description of the Langley 6-inch expansion tube and its operating sequence is given. This facility is basically a cylindrical tube, having a 15.24-cm inside diameter, divided by two diaphragms into three sections (fig. 1(a)). The most-upstream section is the driver or high-pressure section. This section is pressurized at ambient temperature with a gas having a high speed of sound, such as hydrogen or helium. (Greater operation efficiency is realized with gases having high speed of sound.) The pressure and speed of sound of the driver gas may be increased further by heating the gas with a 3-MW resistance heater or by utilizing an arc discharge into the gas from a 10-MJ capacitor bank. The intermediate section is usually referred to as the driven section. This section is evacuated and then filled with the test gas at ambient temperature. The most-downstream section is denoted as the acceleration or expansion section. This section is also evacuated and is generally filled with helium at a low pressure and at ambient temperature. For unheated or resistance heating of the driver gas, the driver and driven sections are separated by a double-diaphragm apparatus capable of withstanding a maximum pressure differential of  $68.95 \text{ MN/m}^2$ . (By controlling the pressure level in the small chamber between these diaphragms, the time of diaphragm rupture can be controlled.) For arc heating, a single diaphragm is used between the driver and driven sections. A weak, low-pressure diaphragm (secondary diaphragm) separates the driven and acceleration sections. The test section and the model are located at the downstream exit of the acceleration section.

The operating sequence, which is shown schematically in figure 1(a), begins with the rupture of the primary or high-pressure diaphragm. A primary shock wave propagates into the static test gas and an expansion wave propagates into the driver gas. The shock wave then encounters and ruptures the secondary or low-pressure diaphragm. The flow energy lost in rupturing this diaphragm results in an upstream-facing shock wave reflected from the diaphragm (ref. 3). This is shown schematically in figure 1(b). A secondary shock wave propagates into the low-pressure acceleration gas while an upstream-expansion wave moves into the test gas. In passing through this upstream-expansion wave, which is being washed downstream since the shock-heated test gas is supersonic, the test

gas undergoes an isentropic unsteady expansion resulting in an increase in the flow velocity (ref. 5). Testing takes place in the flow that has passed through the expansion. This test region is denoted as region (5) in figure 1.

### Determining Flow Quantities in Region (2)

The first step in determining expansion-tube flow conditions is to calculate the flow quantities in region (2) (fig. 1). In the Langley 6-inch expansion tube, the quiescent-test-gas pressure  $p_1$  and temperature  $T_1$  (ambient) are known, as is the test-gas composition  $X_i$ . The incident-shock velocity  $U_{s,1}$  is routinely inferred from microwave measurements and from the response of instrumentation spaced at known intervals along the driven section, and the pressure behind the incident normal shock in the intermediate section  $p_2$  is measured directly. The flow quantities in region (2) may be determined by using either  $U_{s,1}$  or  $p_2$  as an input, in conjunction with  $p_1$ ,  $T_1$ , and  $X_i$ . Also considered is the case where  $p_4$  and  $T_4$  are known for the hydrogen or helium driver gas and are used in conjunction with  $p_1$ ,  $T_1$ , and  $X_i$ .

The basic equations required in determining flow quantities in region (2) are the conservation relations for mass, momentum, and energy for a normal shock moving through region (1), which are

$$\rho_1 U_{s,1} = \rho_2 (U_{s,1} - U_2) \quad (1)$$

$$p_1 + \rho_1 U_{s,1}^2 = p_2 + \rho_2 (U_{s,1} - U_2)^2 \quad (2)$$

$$h_1 + \frac{1}{2} U_{s,1}^2 = h_2 + \frac{1}{2} (U_{s,1} - U_2)^2 \quad (3)$$

and the equation of state (that is, source of thermodynamic properties for real-gas mixtures). Thermodynamic properties for  $\text{CO}_2$ ,  $\text{N}_2$ ,  $\text{O}_2$ , Ar, He, and  $\text{H}_2$  gases or mixtures of these gases in thermochemical equilibrium are obtained by the procedure of references 6 and 7. The procedure of references 6 and 7 is included in the present study as a subroutine and is referred to herein as ROGO. An iterative-interpolation scheme which enables determination of thermodynamic properties from ROGO, for input combinations of  $h$ ,  $p$ ,  $sw_0/R$ , and  $\rho$ , is also a subroutine and is referred to herein as FIND (I). (See appendix A for a detailed discussion of the source of thermodynamic and transport properties for the arbitrary gas mixtures used in the present study.)

Since  $p_1$  and  $T_1$  are known, the corresponding thermodynamic quantities in region (1) (that is,  $\rho_1$  and  $h_1$ ) appearing on the left sides of equations (1) to (3) are obtained from the perfect-gas relations



$$\rho_1 = \frac{p_1 W_o}{RT_1} \quad (4)$$

and

$$h_1 = \frac{\gamma_1}{\gamma_1 - 1} \frac{R}{W_o} T_1 + \sum_i \frac{X_{i,1} h_{o,i}}{W_o} \quad (5)$$

The corresponding  $a_1$  is obtained from the relation

$$a_1 = \left( \gamma_1 \frac{R}{W_o} T_1 \right)^{1/2} \quad (6)$$

where

$$\gamma_1 = \frac{\sum_i X_{i,1} \left( \frac{c_p W_o}{R} \right)_i}{\sum_i X_{i,1} \left( \frac{c_v W_o}{R} \right)_i} \quad (7)$$

For the Langley 6-inch expansion tube,  $T_1$  is the ambient temperature and  $p_1$  is generally less than  $1.0 \text{ MN/m}^2$ . For these conditions, imperfect-gas effects are negligible. The iterative procedures for determining the quantities in region (2) from equations (1) to (3) for inputs  $U_{s,1}$ ,  $p_2$ , and  $p_4$  and  $T_4$  are now discussed individually. For all three cases, the flow in region (2) is assumed to be in thermochemical equilibrium.

Case where  $U_{s,1}$  is known.- When  $U_{s,1}$  is known, the terms appearing on the left sides of equations (1) to (3) are known. An initial estimate of  $\rho_2 = 10\rho_1$  is made and the corresponding values of  $U_2$ ,  $p_2$ , and  $h_2$  are obtained. The  $p_2$  and  $h_2$  are used as inputs to FIND (2) to obtain a value of  $\rho_2$ . This  $\rho_2$  from FIND (2) is compared with the initial guess of  $\rho_2$  and, if it is not within 0.1 percent, the  $\rho_2$  from FIND (2) is used in equations (1) to (3) to obtain upgraded values of  $U_2$ ,  $p_2$ , and  $h_2$ . This iterative procedure, commonly referred to as the method of successive approximations, is continued until successive values of  $\rho_2$  are within 0.1 percent.

Case where  $p_2$  is known.- When  $p_2$  is known, an initial estimate of  $\rho_2$  is made. The corresponding  $U_{s,1}$  is obtained from equations (1) and (2) in the form

$$U_{s,1} = \left[ \frac{p_2 - p_1}{\rho_1 \left( 1 - \frac{\rho_1}{\rho_2} \right)} \right]^{1/2} \quad (8)$$

$U_2$  is found from equation (1), and  $h_2$  is found from equation (3). The  $p_2$  and  $h_2$  are used in FIND (2) to obtain a corresponding value of  $\rho_2$ . The method of successive approximations is employed on  $\rho_2$  until successive values are within 0.1 percent.

Case where  $p_4$  and  $T_4$  are known.- The thermodynamic properties in region (4) are determined from the imperfect-gas relations of appendix B. The unsteady expansion which occurs from region (4) to region (3) (fig. 1(a)) upon rupture of the primary diaphragm is assumed to be isentropic. An array of thermodynamic properties  $p$ ,  $h$ ,  $Z$ ,  $a$ , and  $\rho$  is generated in region (3) by varying  $T_3$  from a maximum value ( $T_4$ ) to a minimum value and by knowing  $s_3W_3/R$  ( $s_3W_3/R = s_4W_4/R$ ). The  $U_3$  corresponding to each value of  $T_3$  is obtained by using the differential equation for a one-dimensional, unsteady expansion. Across an upstream-facing unsteady-expansion wave, the velocity increment is related to the thermodynamic properties by the differential equation (ref. 5)

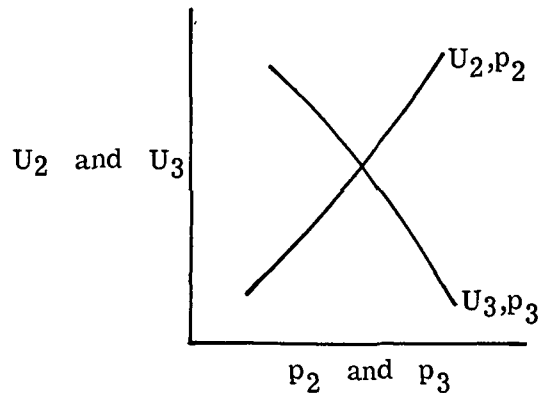
$$dU = -\left(\frac{dh}{a}\right)_{sW_0}/R \quad (9)$$

Integrating equation (9) between regions (3) and (4) gives

$$U_3 = -\int_{h_4}^{h_3} \left(\frac{dh}{a}\right)_{s_4W_4/R} \quad (10)$$

where  $U_4$  is zero. The  $U_3$  is found by performing the integration of equation (10) numerically. Thus, a unique correspondence between  $U_3$  and  $p_3$  at constant  $s_4W_4/R$  is obtained.

By varying  $U_{s,1}$  over a range, an array of  $U_2$  and  $p_2$  may also be obtained. A solution is found by requiring that  $p_3$  equal  $p_2$  and  $U_3$  equal  $U_2$ , as is illustrated in the sketch



The solution is the intersection of the  $U_2, p_2$  curve and the  $U_3, p_3$  curve. The other thermodynamic properties in region (2) are obtained from ROGO, where  $T_2$  is obtained by interpolation and  $U_{s,1}$  is determined from equation (1).

### Determining Flow Quantities in Region (2,s)

As discussed in references 3 and 8, the flow energy lost in the rupture of the secondary diaphragm must result in an upstream-facing shock wave reflected from the diaphragm. In reference 9, this shock-wave reflection is observed to be, for a short period of time, approximately a standing wave, as illustrated in figure 1(b). Therefore, the possible existence of a standing normal shock at the secondary diaphragm, due to shock-wave reflection from this diaphragm, is considered. The conservation relations for this standing shock are

$$\rho_2 U_2 = \rho_{2,s} U_{2,s} \quad (11)$$

$$p_2 + \rho_2 U_2^2 = p_{2,s} + \rho_{2,s} U_{2,s}^2 \quad (12)$$

and

$$h_2 + \frac{1}{2} U_2^2 = h_{2,s} + \frac{1}{2} U_{2,s}^2 \quad (13)$$

Since the quantities in region (2) are known (that is, have been calculated previously), equations (11) to (13) are solved by the method of successive approximations to yield the quantities behind the standing normal shock (that is, flow quantities in region (2,s)). As in region (2), the flow in region (2,s) is assumed to be in thermochemical equilibrium.

### Determining Flow Quantities in Region (5)

Upon rupture of the secondary diaphragm, an upstream-expansion wave moves into the test gas. In passing through this upstream-expansion wave, the test gas undergoes an isentropic, unsteady expansion to region (5). Integrating equation (9) between regions (A) and (5) (where region (A) denotes region (2) for no standing shock at the secondary diaphragm or region (2,s) for a standing shock and where the conditions are as yet unknown in region (5)) gives

$$\Delta U = U_5 - U_A = - \int_{h_A}^{h_5} \left( \frac{dh}{a} \right)_{s_A} W_0 / R \quad (14)$$

Since  $p_5$  and  $U_5$  are measured in the Langley 6-inch expansion tube, both quantities are considered, individually, as inputs necessary for the solution of equation (14). As is typical of high-enthalpy facilities, the assumption of thermochemical-equilibrium flow is subject to question. Hence, both equilibrium-flow and frozen-flow cases are considered in the present program.

Thermochemical-equilibrium unsteady expansion. - If the case where  $U_5$  is an input is considered first, then  $\Delta U$  of equation (14) is known. The expansion in velocity

from region (A) to region (5) corresponds to a decrease in pressure  $p$  between these regions. Thus, with  $s_A W_0/R$  and a range of  $p$  from an upper limit of  $p_A$  to a lower limit of  $p_{5,f}$  (calculation of  $p_{5,f}$  is discussed subsequently), FIND (3) is used to generate a plot of  $1/a$  against  $h$  for the real-gas mixture. The temperature limits, as required by FIND (I), used in generating this plot are  $T_A$  as an upper limit and  $T_{5,f}$  as a lower limit. Equation (14) is integrated numerically (Simpson's rule) between the known limit  $h_A$  and the unknown limit  $h_5$ . The  $h_5$  is the value of  $h$  which equates the integral of equation (14) to  $\Delta U$ . The corresponding  $p_5$  and  $T_5$  are obtained by interpolation and the other thermodynamic quantities in region (5) are obtained from ROGO.

For the case of an equilibrium expansion where  $p_5$  is an input,  $s_A W_0/R$  and  $p_5$  are used as inputs in FIND (3) to obtain the corresponding thermodynamic properties in region (5). With the limits of integration known, the integral of equation (14) is evaluated numerically. Once a value for  $\Delta U$  is obtained and with  $U_A$  known,  $U_5$  may be found. Additional free-stream (region (5)) quantities that are calculated are  $M_5 = U_5/a_5$  and  $N_{Re,5} = \rho_5 U_5/\mu_5$ .

Frozen unsteady expansion.- Frozen flow is defined herein as that in which the vibrational energy and chemistry remain unchanged during the expansion process. In the present program, this freezing of the vibrational energy and chemistry is assumed to occur in region (A). Hence the energy in region (A) may be viewed as consisting of an active or available part, which provides the energy for flow expansion, and a frozen or nonavailable part. In the frozen expansion,  $\gamma_f$  remains constant and the test-gas mixture behaves as a perfect gas. By using the perfect-gas relation

$$dh = \frac{2}{\gamma_f - 1} a da \quad (15)$$

equation (14) may be evaluated in closed form to yield

$$U_{5,f} - U_A = \frac{2}{\gamma_f - 1} (a_{A,f} - a_{5,f}) \quad (16)$$

By freezing (that is, maintaining constant) the vibrational energy,  $c_p W_0/R$  becomes 7/2 for a diatomic molecule and 9/2 for a triatomic molecule. The  $c_p W_0/R$  for an atom is 5/2. By using the perfect-gas relation

$$\frac{c_v W_0}{R} = \frac{c_p W_0}{R} - 1 \quad (17)$$

the specific-heat ratio  $\gamma_f$  is obtained from equation (7) as

•

$$\gamma_f = \frac{\sum_i X_{i,A} \left( \frac{c_p W_o}{R} \right)_i}{\sum_i X_{i,A} \left( \frac{c_v W_o}{R} \right)_i}$$

The speed of sound in region (A) is determined from the relation

$$a_{A,f} = \left( \gamma_f \frac{R}{W_o} Z^*_{A} T_A \right)^{1/2} \quad (18)$$

and the active enthalpy is determined from the relation

$$h_{A,act} = \frac{a_{A,f}^2}{\gamma_f - 1} + \frac{\sum_i X_{i,A} h_{o,i}}{W_o} \quad (19)$$

Ionized species in region (A) are not included in the calculation of  $h_{A,act}$  from equation (19). The values of  $h_o$  for species N, N<sub>2</sub>, O, O<sub>2</sub>, NO, C, CO, CO<sub>2</sub>, and Ar are given in reference 6 and those for He, H, and H<sub>2</sub> are obtained from reference 10. The enthalpy is given by the relation

$$h_{A,f} = h_A - h_{A,act} \quad (20)$$

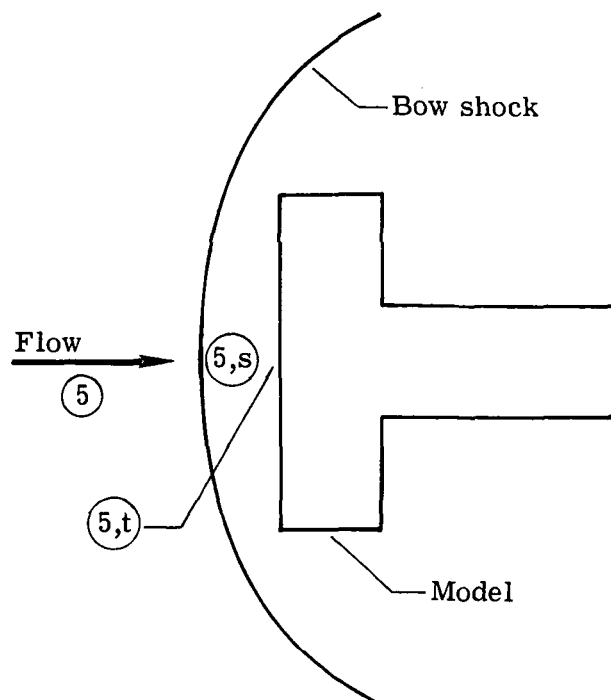
For the case where  $U_5$  (that is,  $U_{5,f}$ ) is known,  $a_{5,f}$  may be found from equation (16) and the corresponding frozen-flow thermodynamic quantities in region (5) are determined from the isentropic perfect-gas relations of reference 11. For the case where  $p_5$  (that is,  $p_{5,f}$ ) is known,  $a_{5,f}$  is determined from the isentropic perfect-gas relation

$$a_{5,f} = a_{A,f} \left( \frac{p_{5,f}}{p_A} \right)^{\gamma_f - 1 / 2\gamma_f} \quad (21)$$

Corresponding frozen-flow quantities in region (5) are determined similarly, and with  $a_{5,f}$  known,  $U_{5,f}$  may be obtained from equation (16).

#### Determining Flow Quantities Behind Bow Shock of Test Model

In most tests in the Langley 6-inch expansion tube, a test model (for example, a pitot probe) is positioned at the test section (tube exit). Hence, it is desirable to determine the flow quantities behind the bow shock in front of a blunt test model. In the present study, flow quantities are calculated for the static conditions immediately behind the portion of the bow shock that is essentially a standing normal shock (region (5,s)) and for the stagnation conditions (point (5,t)). These conditions are illustrated in the following sketch:



The conservation relations for a standing normal shock about a blunt body in the expansion-tube test section are given in equations (11) to (13) where the subscripts 2 and 2,s are now replaced by 5 and 5,s. In the present study three combinations concerning the flow chemistry in the free-stream region (region (5)) and the post-normal-shock region (region (5,s) and point (5,t)) are considered. These combinations are designated cases (1) to (3) as follows:

Case	Region (5)	Region (5,s) and point (5,t)
(1)	Equilibrium	Equilibrium
(2)	Frozen	Equilibrium
(3)	Frozen	Frozen

For case (1) or (2), where post-normal-shock flow conditions are assumed to be in thermochemical equilibrium and free-stream conditions are either in thermochemical equilibrium or frozen, the conservation relations are solved by iteration for the static conditions immediately behind the shock. In this solution, the flow quantities in region (5) are considered known and the initial estimate of  $\rho_{5,s}$  is taken to be  $10\rho_5$ . For the post-normal-shock stagnation conditions, solutions are found by assuming that the flow region from immediately behind the normal shock to the stagnation point is isentropic (that is,  $s_{5,t} W_0/R = s_{5,s} W_0/R$ ). Now, the variations in conditions from immediately downstream

of the shock to the stagnation point are relatively small (that is,  $\gamma_{E,5,s} \approx \gamma_{E,5,t}$  and  $Z_{5,s}^* \approx Z_{5,t}^*$ ). Thus, the gas in this region may be considered to behave as a perfect gas. The  $p_{5,t}$  can be accurately determined from the perfect-gas isentropic relation (ref. 11)

$$p_{5,t} = p_{5,s} \left( 1 + \frac{\gamma_{E,5,s} - 1}{2} M_{5,s}^2 \right)^{\frac{\gamma_{E,5,s}}{\gamma_{E,5,s} - 1}} \quad (22)$$

Now, for case (1),  $h_{5,t}$  is determined from the energy relation (eq. (13)) to be

$$h_{5,t} = h_5 + \frac{1}{2} U_5^2 \quad (23)$$

whereas, for case (2), the energy equation becomes

$$h_{5,t} = h_{5,s} + \frac{1}{2} U_{5,s}^2 = h_{5,f} + h_{A,f} + \frac{1}{2} U_{5,f}^2 \quad (24)$$

that is, for case (2), the nonavailable energy in the expansion process or free stream is made available to the post-normal-shock flow. The  $p_{5,t}$  from equation (22) and the  $h_{5,t}$  from equation (23) or (24) are used as inputs to FIND (2) to obtain the corresponding thermodynamic properties at the stagnation point. The stagnation-point heat-transfer rate is calculated by using the relation (ref. 12)

$$\dot{q}_{5,t} = \frac{W_o}{\sum_i \frac{X_i W_i}{\eta_i}} \sqrt{\frac{p_{5,t}}{r}} (h_{5,t} - h_w) \quad (25)$$

where the constants  $\eta_i$  are given in the following table:

Species i	$\eta_i$
CO <sub>2</sub>	$4.3102 \times 10^{-4}$
N <sub>2</sub>	3.6285
O <sub>2</sub>	4.3102
Ar	5.4788
He	2.5038
H <sub>2</sub>	1.2786

The values of  $\eta_i$  for CO<sub>2</sub>, N<sub>2</sub>, Ar, and H<sub>2</sub> are taken directly from table I of reference 12, whereas the value for He is obtained from table II of reference 13. Since a value of  $\eta_i$  for O<sub>2</sub> is not presented in reference 12, the  $\eta_i$  for O<sub>2</sub> is set equal to that for CO<sub>2</sub> in the present study (ref. 13).

For case (3) (both free-stream and post-normal-shock flow conditions frozen),  $\gamma_5 = \gamma_{5,s} = \gamma_{5,t}$ . Hence, the perfect-gas normal-shock relations of reference 11 are used to determine the properties for static and for stagnation post-normal-shock conditions.

#### Determining Quiescent-Acceleration-Gas Pressure

An important parameter in the operation of an expansion tube is the quiescent pressure of the acceleration gas  $p_{10}$ . For a given condition in region (A), it is  $p_{10}$  and acceleration-gas temperature and molecular weight which determine the extent of the unsteady flow expansion (that is, the velocity obtained in region (5)); conversely, a particular value of  $p_{10}$  is required to obtain a given value of  $U_5$ . In most studies in an expansion tube,  $U_5$  is one of the principal flow quantities. Therefore, to generate a desired  $U_5$ , the required  $p_{10}$  must be known.

The momentum equation for the normal shock moving into region (10) is equation (2) where the subscript 10 replaces 1 and the subscript 20 replaces 2. At the interface of the acceleration gas and the test gas, it is required that  $p_{20}$  equal  $p_5$  and  $U_{20}$  equal  $U_5$ . Two cases providing a range of  $p_{10}$  are considered. The first is where the incident shock into the acceleration gas is traveling at the same velocity as the interface of the acceleration gas and the test gas (ref. 14). For this case, equation (2) in conjunction with the equation of state (where  $Z_{10}$  is unity, because of relatively low values of  $p_{10}$ , and  $T_{10}$  is equal to  $T_1$ ) becomes

$$p_{10} = \frac{p_5}{1 + \frac{W_{10}}{RT_1} U_5^2} \quad (26)$$

The second case considered is where (ref. 5)

$$U_{s,10} = \frac{\gamma_{10} + 1}{2} U_5 \quad (27)$$

Now, in the Langley 6-inch expansion tube, helium is generally employed as the acceleration gas. For values of  $U_{s,10}$  less than 10 km/sec or so, helium behaves as a perfect gas (ref. 15); hence, the perfect-gas relation of reference 11 gives, for  $\gamma_{10} = 5/3$ ,

$$p_{10} = \frac{4p_5}{5M_{s,10}^2 - 1} \quad (28)$$

where

$$M_{s,10}^2 = \frac{U_{s,10}^2}{a_{10}^2} = \frac{W_{10} U_{s,10}^2}{\gamma_{10} RT_1}$$



At  $U_{s,10}$  greater than 10 km/sec, the helium acceleration gas departs from perfect-gas behavior because of ionization, and equation (28) is not valid. For example, at a  $M_{s,10}$  of 20, equation (28) yields a value of  $p_{10}$  that is approximately 1.2 times the value computed for real helium at a  $p_{10}$  of 1 N/m<sup>2</sup>. The effects of a real-helium acceleration gas are not included in the present program; hence, for  $U_{s,10}$  greater than 10 km/sec, reference 15 should be consulted for more accurate values of  $p_{10}$  than those calculated by equation (28).

## DISCUSSION

Flow quantities in region (A) are obtained by using basic measured inputs in the following combinations:

Case (1)  $p_1$ ,  $T_1$ ,  $X_i$ , and  $U_{s,1}$

Case (2)  $p_1$ ,  $T_1$ ,  $X_i$ , and  $p_2$

Case (3)  $p_1$ ,  $T_1$ ,  $p_4$ ,  $T_4$ ,  $W_4$ , and  $X_i$

For each combination, the option of a standing shock at the secondary diaphragm may be exercised. The values in regions (2) and (2,s) for case (1) where  $U_{s,1}$  is an input are compared, for several mixtures, to those calculated by using the program of reference 16. This comparison shows excellent agreement (all parameters within 0.5 percent) as expected, since both reference 16 and the present study employ references 6 and 7 as the source of thermodynamic properties. For case (2) where  $p_2$  is an input, the values of  $p_2$  calculated for case (1) where  $U_{s,1}$  is an input are in turn used as inputs; this cross-check shows excellent agreement between the results. For case (3) where  $p_4$  and  $T_4$  are inputs, the values in region (2) are observed to be in good agreement ( $U_{s,1}$  within 0.2 percent) with those of reference 1 for helium driver gas when imperfect-gas effects are negligible.

Combinations of measured input and options for obtaining stagnation-point conditions in region (5), when it is assumed that the flow conditions in region (A) are known, are summarized in the following table:

Case	Measured input	Unsteady expansion	Postnormal shock
(1)	$U_5$ or $p_5$	Equilibrium	Equilibrium
(2)	$U_5$ or $p_5$	Frozen	Equilibrium
(3)	$U_5$ or $p_5$	Frozen	Frozen

The flow quantities in region (5) for case (1) are compared with those obtained by using the real-air charts of reference 17. For this comparison, a 10-species ( $e^-$ , Ar, N,  $N^+$ ,  $N_2$ , O,  $O^+$ ,  $O_2$ , NO, and  $NO^+$ ) air model is employed in the present program, the air composition by volume being 78.08 percent  $N_2$ , 20.95 percent  $O_2$ , and 0.97 percent Ar. This comparison shows good agreement between the results obtained from the charts of reference 17 and from the present program. For the case where  $p_5$  is an input, the values of  $p_5$  calculated for the case where  $U_5$  is an input are in turn used as inputs. Results of this cross-check show good agreement. Quantities in regions (5,s) and (5,t) for thermochemical equilibrium are checked by comparing results with those obtained by using the program of reference 18.

The large number of gas mixtures that may be used as test media coupled to the wide range of flow conditions that may be generated with these mixtures in the expansion tube results in an extremely large number of possible flow states. For this reason the present program, which requires relatively long computer times (to be discussed subsequently), has not yet been exercised to generate a family of plots illustrating facility performance for several gases or gas mixtures. Instead, detailed sample calculations are presented.

In performing a test in an expansion tube, the first consideration is to calculate the theoretical flow quantities for the chosen mode of operation. From the experimenter's viewpoint, this is necessary in order to obtain the approximate magnitudes of velocity and pressure in the various regions. Knowledge of these magnitudes is required in the preparation of facility instrumentation for the test. Also, if several gas mixtures are to be used in a study, it may be desirable to determine conditions required to yield the same values of certain quantities for all gases (for example, velocity and/or pressure in the test section, or region (5)).

As an example, the expansion tube is assumed to be operated in a low-to-moderate performance mode. The driver gas is helium at ambient temperature ( $T_4 = 300$  K) and a pressure of 34.474 MN/m<sup>2</sup>. The acceleration gas is also helium at ambient temperature. Three test gases are considered, air ( $N_2$ - $O_2$ -Ar mixture), pure  $CO_2$ , and pure Ar. The  $p_1$  is varied from 861.9 N/m<sup>2</sup> to 6.895 kN/m<sup>2</sup> for all gases, and the  $T_1$  is ambient. The desired free-stream velocity  $U_5$  is 4.267, 4.877, 5.486, and 6.096 km/sec. For the experimenter, a knowledge is required of the approximate magnitudes of  $U_{s,1}$  and  $p_2$  in region (2);  $p_5$ ,  $p_{5,t}$ , and  $\dot{q}_{5,t}$  in region (5); and the  $p_{10}$  to produce the desired  $U_5$ . As shown in reference 18 a substantial reduction in computer time is realized by judicious selection of the number of species. Now, at such moderate performance, first and second ionization for air and for  $CO_2$  are negligible so that the species considered in the air model may be limited to Ar, N,  $N_2$ , O,  $O_2$ , and NO and the species considered for the  $CO_2$  are O,  $O_2$ , C, CO, and  $CO_2$ . For Ar, second ionization is assumed negligible and

the species considered are  $e^-$ , Ar, and  $Ar^+$ . The inputs to the program and the procedure for varying the number of species are discussed in appendix C. The species inputs, in FORTRAN IV language, for the composition of these gases are

	Air	CO <sub>2</sub>	Ar
NUMSP	6	5	3
JINDEX	3	2	2
IAR	1	0	2
IC	0	3	0
ICØ	0	4	0
ICØ2	0	5	0
IN	2	0	0
IN2	3	0	0
INØ	6	0	0
IØ	4	1	0
IØ2	5	2	0
PCØ2	0.0	1.0	0.0
PN2	0.78	0.0	0.0
PØ2	0.21	0.0	0.0
PAR	0.01	0.0	1.0
PMIX	1.0	1.0	1.0

The composition for the air model is  $X_{N_2} = 0.78$ ,  $X_{O_2} = 0.21$ , and  $X_{Ar} = 0.01$ . It should be noted that PMIX must satisfy the relation

$$PMIX = PCØ2 + PN2 + PØ2 + PAR$$

Symbols denoting position in species array (that is, IAR, IC, etc.) that are zero need not be included in the input.

For a given  $p_1$ , which in turn corresponds to a given set of flow quantities in region (A), four values of  $U_5$  are considered in this example; that is, four expansions from the given conditions in region (A) are to be performed. Hence, the inputs (appendix C) for this case are IREP = 1, U5I = 610, and NVEL = 4. For this example, the existence of a standing shock at the secondary diaphragm is assumed (LD = 1) and only a thermochemical-equilibrium expansion from region (A) to region (5) is considered (LG = 0).

Pertinent quantities calculated within the present program for the three test gases considered in this example are given in tables I to III.

The results for CO<sub>2</sub> (table II) and for Ar (table III) were obtained on a Control Data 6600 series computer, whereas the results for air (table I) were obtained on the slower

Control Data 6400 series computer. Three cases were also run for a 15-species CO<sub>2</sub> model and the same conditions as in table II for  $p_1 = 6.895 \text{ kN/m}^2$ . These cases were run on a Control Data 6600 series computer and the computer times required per case are compared in the following table:

Gas	No. of species	Computer time per case, sec
Ar	3	24
CO <sub>2</sub>	5	58
CO <sub>2</sub>	15	215

At the moderate velocities in regions (2) and (5) considered, the computed flow quantities for the 5-species CO<sub>2</sub> model and the 15-species CO<sub>2</sub> model are the same. Therefore, species should be selected judiciously to minimize computer time without sacrificing accuracy in calculated flow quantities.

Cases are also run, at an arbitrary  $p_1$  of  $3.447 \text{ kN/m}^2$ , for gas mixtures representing atmospheric models of Mars ( $X_{\text{CO}_2} = 0.85$  and  $X_{\text{Ar}} = 0.15$ ), Venus ( $X_{\text{CO}_2} = 0.95$  and  $X_{\text{N}_2} = 0.05$ ), and Jupiter ( $X_{\text{He}} = X_{\text{H}_2} = 0.5$ ). For the Mars model, the driver conditions are the same as in tables I to III and  $U_5$  is  $5.486 \text{ km/sec}$ . However, for the Venus model, maximum performance for resistance-heated helium driver gas in the Langley 6-inch expansion tube is utilized. This corresponds to  $p_4 = 68.95 \text{ MN/m}^2$  and  $T_4 = 600 \text{ K}$ . The  $U_5$  for this Venus model is  $10.97 \text{ km/sec}$ . For the Jovian model, maximum performance with resistance-heated hydrogen driver gas ( $p_4 = 68.95 \text{ MN/m}^2$  and  $T_4 = 600 \text{ K}$ ) is utilized and the  $U_5$  is  $12.19 \text{ km/sec}$ . Sample data printouts for these cases are presented in appendix C.

For an actual test in an expansion tube, a comparison of the measured flow quantities to the calculated flow quantities is desired. Such a comparison is illustrated in figure 2 where preliminary experimental results for several tests in the Langley 6-inch expansion tube are shown along with calculations from the present program.

For these tests, the test gas is air and the driver gas is unheated helium at a  $p_4$  of approximately  $34.474 \text{ MN/m}^2$ . For a  $p_1$  of  $3.447 \text{ kN/m}^2$ , the  $p_{10}$  is  $37 \text{ N/m}^2$  of helium and, for a  $p_1$  of  $1.379 \text{ kN/m}^2$ , the  $p_{10}$  is  $3.3 \text{ N/m}^2$  of argon. In figure 2(a), the ratio  $p_4/p_1$  is plotted against  $U_{s,1}$  and the solid line represents the calculated results shown in table I. From figure 2(a), it is observed that the  $U_{s,1}$  inferred from the response of ionization gages located in the intermediate section is actually greater than the predicted  $U_{s,1}$ , being approximately 1.2 times the predicted values for both values of  $p_1$ . This trend is consistently observed in the Langley 6-inch expansion tube and is believed to result from a combination of several effects. Among these effects are

the following: (1) The cross-sectional area of the driver section is somewhat larger than the intermediate section. The data of figure 2(a) are obtained for a ratio of driver-section cross-sectional area to intermediate-section cross-sectional area equal to 1.173, whereas this ratio is assumed to be unity in the present program. As shown in reference 19, an increase in  $U_{s,1}$  is to be expected for an increase in this ratio. (2) The double-diaphragm mode of operation resembles that of a buffered-shock tube. Upon rupture of the upstream diaphragm, a shock wave propagates through the short chamber between the diaphragms. This shock wave heats the gas, contained within this chamber, just prior to rupture of the second diaphragm. Gains in  $U_{s,1}$  obtained with buffered-shock tubes are illustrated in reference 19. (3) The relatively long opening times of the steel diaphragms may result in coalescing compressions and accelerating shock waves. It has been shown previously (ref. 20) that the finite opening time of the diaphragm produces faster shock waves for a given  $p_4/p_1$  than simple shock-tube theory predicts.

The  $p_5$  are plotted against  $U_5$  in figures 2(b) and 2(d) for  $p_1$  of 3.447 kN/m<sup>2</sup> and 1.379 kN/m<sup>2</sup>, respectively; the  $p_{5,t}$  are plotted against  $U_5$  in figures 2(c) and 2(e) for  $p_1$  of 3.447 kN/m<sup>2</sup> and 1.379 kN/m<sup>2</sup>, respectively. The solid lines in figures 2(b) and 2(c) represent calculated results shown in table I.

In figures 2(b) and 2(c), the experimental data show best agreement with the results calculated by the method which uses the measured  $U_{s,1}$  as an input, includes a standing shock at the secondary diaphragm, and assumes thermochemical equilibrium during the unsteady-expansion process. At the experimental values of  $p_5$  (fig. 2(b)) and  $p_{5,t}$  (fig. 2(c)), the calculated velocity from table I is approximately 20 percent less than the measured velocity. This low prediction is expected, because of the difference in  $U_{s,1}$  observed between theory and experiment in figure 2(a). The lower-density data of figures 2(d) and 2(e) indicate a departure from an equilibrium expansion; for example, the calculated free-stream static pressure for an equilibrium expansion (fig. 2(d)) is approximately 2.7 times the measured value, but this measured value is about 26 times as high as the calculated value for a frozen expansion (if it is assumed that a standing shock exists at the secondary diaphragm).

## CONCLUDING REMARKS

A computer program written in FORTRAN IV language is presented which determines expansion-tube flow quantities for real test gases CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, He, and H<sub>2</sub>, or mixtures of these gases, in thermochemical equilibrium. This program permits, as input data, a number of possible combinations of flow quantities, which are generally measured during an expansion-tube test. The versatility of the program is enhanced by the inclusion of such effects as imperfect driver gas and shock reflection at the secondary diaphragm and by consideration of both a thermochemical-equilibrium flow expansion and a frozen flow expansion.

The usage of the program in preparing the expansion tube for testing with several gases is illustrated by sample calculations. Results from the program are also compared with preliminary data obtained experimentally in the Langley 6-inch expansion tube. This comparison shows that the measured incident-shock velocity  $U_{s,1}$  and the measured interface velocity  $U_5$  are approximately 1.2 times the calculated values, when driver-gas pressure and temperature are inputs. This discrepancy is attributed to several effects believed to be present in the Langley 6-inch expansion tube. Agreement between calculated and measured test-section flow quantities is significantly improved when measured incident-shock velocity is employed as an input.

Langley Research Center,  
National Aeronautics and Space Administration,  
Hampton, Va., August 2, 1972.

## APPENDIX A

### THERMODYNAMIC AND TRANSPORT PROPERTIES FOR ARBITRARY GAS MIXTURES

Thermodynamic properties for real gases CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, He, and H<sub>2</sub>, or mixtures of these gases, are obtained by the procedure of references 6 and 7 and include dissociation and first and second ionization. Basic assumptions used in obtaining these properties are

- (1) The mixture is composed of ideal gases
- (2) For diatomic species the rigid-rotor harmonic-oscillator model is used with vibrational-rotational corrections for each electronic configuration
- (3) Only electronic levels with principal quantum number less than or equal to 5 are included

The procedure of references 6 and 7 is based upon the free-energy-minimization method of reference 21. For a given pressure and temperature, the free energies for individual species are computed from the partition function of statistical mechanics. The equilibrium composition is then obtained by minimization of the free energy. When the composition for a given pressure and temperature is determined, the corresponding thermodynamic properties are computed directly.

The 5 components and 26 species considered in references 6 and 7 are listed in appendix C. These 26 species permit modeling of Earth, Mars, and Venus atmospheres but not of proposed Jovian atmospheres which are believed to consist primarily of helium and hydrogen. Therefore, the components H and He and the species H, H<sub>2</sub>, H<sup>+</sup>, He, He<sup>+</sup>, and He<sup>++</sup> are also included in the present study. However, no provision is included for combinations of hydrogen with any of the other species. The energy-level constants for the 26 species considered in references 6 and 7 are tabulated in reference 6, whereas the energy-level constants for the 6 additional species are obtained from reference 22.

The procedure of references 6 and 7 is included in the present study as a subroutine and is referred to herein as ROGO. The basic inputs to ROGO, other than the energy-level constants, are pressure, temperature, and initial estimates of the species concentrations. (In the free-energy-minimization method for determining the composition of a gas mixture, the initial estimates of  $Y_i$  are somewhat arbitrary.) In the present study, the partial pressures of the quiescent test gas in the intermediate chamber are assumed known. The corresponding mole fractions for these gases are obtained from Dalton's law

$$X_i = \frac{p_i}{p_{\text{mix}}} \quad (\text{A1})$$

# APPENDIX A – Continued

and the molecular weight is given by

$$W_o = \sum_i X_i W_i \quad (A2)$$

The initial estimates for the species concentrations for CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, Ar, He, and H<sub>2</sub> are obtained from

$$Y_i = \frac{X_i}{W_o} \quad (A3)$$

For the remaining 26 species the initial estimates for the concentrations are set equal to 10<sup>-20</sup>. (If Y<sub>i</sub> for O<sub>2</sub> is not known, the initial estimate is set equal to 10<sup>-5</sup>.) Thermodynamic properties obtained from ROGO, for a given p and T, are a, h, sW<sub>o</sub>/R, X<sub>i</sub>, Z\*, γ<sub>E</sub>, and ρ.

Combinations of input thermodynamic properties other than p and T are required in the present study. An iterative-interpolation scheme is derived in reference 18 so as to enable determination of thermodynamic properties from combinations of h, p, sW<sub>o</sub>/R, and ρ. This scheme is referred to herein as FIND (I), and the inputs for a given I are as follows:

I	Inputs to FIND (I)
1	p, ρ
2	p, h
3	p, sW <sub>o</sub> /R
4	h, ρ

A detailed discussion of FIND (I) is presented in reference 18.

The viscosity μ is calculated by using the expressions presented in reference 18. Since He and H<sub>2</sub> are also included in the present study, expressions for the viscosity of these species are derived. The viscosity for He is obtained by applying a curve fit to the results of references 23 to 25 for temperatures to 5000 K. The resulting expression is

$$\mu = 3.92 \times 10^{-7} T^{0.7} \quad (A4)$$

The expression for Ar is (ref. 18)

$$\mu = 3.33 \times 10^{-7} T^{0.739} \quad (A5)$$

Simple expressions for the viscosity, in the form

$$\mu = (b_0 + b_1 T + b_2 T^2) \times 10^{-7} \quad (A6)$$

are obtained for the diatomic species N<sub>2</sub> and O<sub>2</sub> and for the triatomic species CO<sub>2</sub> in reference 18. For convenience, the constants of equation (A6) for these species along with



# APPENDIX A – Concluded

those for H<sub>2</sub> obtained from the results of references 25 to 27 are presented in the following table:

Gas	T, K	b <sub>0</sub>	b <sub>1</sub>	b <sub>2</sub>
CO <sub>2</sub>	150 to 1000	$-9.7303 \times 10^{-1}$	$5.5222 \times 10^{-1}$	$-1.6139 \times 10^{-4}$
	1000 to 5000	$1.5029 \times 10^2$	$2.4890 \times 10^{-1}$	$-6.1747 \times 10^{-6}$
N <sub>2</sub>	150 to 1000	$2.2992 \times 10^1$	$5.5586 \times 10^{-1}$	$-1.8436 \times 10^{-4}$
	1000 to 5000	$1.6388 \times 10^2$	$2.4601 \times 10^{-1}$	$-7.7388 \times 10^{-6}$
O <sub>2</sub>	150 to 1000	$1.9939 \times 10^1$	$6.6236 \times 10^{-1}$	$-2.0410 \times 10^{-4}$
	1000 to 5000	$2.3030 \times 10^2$	$2.5597 \times 10^{-1}$	$-2.2643 \times 10^{-6}$
H <sub>2</sub>	150 to 1000	$2.3877 \times 10^1$	$2.1918 \times 10^{-1}$	$-4.4304 \times 10^{-5}$
	1000 to 5000	$6.3197 \times 10^1$	$1.4093 \times 10^{-1}$	$-8.6387 \times 10^{-6}$

These expressions should provide reasonably accurate (within 10 percent or so) values of  $\mu$  for T less than 5000 K, with the accuracy decreasing with further increase in T. For T greater than 8000 K,  $\mu$  is not calculated in the present program.

## APPENDIX B

### THERMODYNAMIC PROPERTIES FOR IMPERFECT HELIUM AND HYDROGEN

The driver gas for the Langley 6-inch expansion tube is usually helium or hydrogen. For unheated and resistance-heated driver gas, pressures up to 70 MN/m<sup>2</sup> and temperatures from 300 K to 600 K are obtained. For such conditions, the assumption of perfect helium or hydrogen is inadequate because of intermolecular-force effects (for example, see refs. 28 and 29). The relations used to calculate imperfect-gas effects at these driver-gas conditions are taken from reference 28 and are based on the virial form of the equation of state which, where interactions involving four or more molecules are neglected, can be written as

$$p = \rho \frac{R}{W_0} T Z = \rho \frac{R}{W_0} T \left[ 1 + \rho B(T) + \rho^2 C(T) \right] \quad (B1)$$

For helium, the virial coefficients are given by

$$B(T) = 3.3565 \times 10^{-6} (15.8922 - \ln T)^3 \\ - 2.0085 \times 10^{-3} \exp \left[ - (3.7156 \times 10^{-3}) T \right] \quad (B2)$$

and

$$C(T) = 5.6330 \times 10^{-12} (15.8922 - \ln T)^6 \quad (B3)$$

These expressions for  $B(T)$  and  $C(T)$  are employed in the imperfect-helium study of reference 28 for a temperature range of 200 K to 15 000 K.

For hydrogen a curve fit is applied to the second-virial-coefficient results of reference 30. These results include a temperature range of 273 K to 473 K and the curve-fit expression is

$$B(T) = 1.6994 \times 10^{-3} T^{1/4} \quad (B4)$$

Although equation (B4) is obtained for temperatures to only 473 K, this expression is assumed to be valid for temperatures to 600 K. (This temperature represents the maximum value of  $T_4$  considered herein.) To obtain an expression for  $C(T)$  for hydrogen, the results of reference 29 are used. In reference 29 compressibility factors are calculated by using the Beattie-Bridgeman equation of state for temperatures from 30 K to 1000 K and for pressures from 10 kN/m<sup>2</sup> to 10<sup>2</sup> MN/m<sup>2</sup>. Now, for pressures to 10 MN/m<sup>2</sup>, the compressibility factors obtained from equations (B1) and (B4), where  $C(T) = 0$ , are within 1 percent of the values presented in reference 29 for temperatures from 300 K to 1000 K. However, at higher pressures ( $10 \text{ MN/m}^2 < p < 10^2 \text{ MN/m}^2$ ), these compressibility factors are as much as 20 percent less than those of reference 29, since interactions involving three molecules are ignored (that is,  $C(T) = 0$ ). Hence, values of

## APPENDIX B - Continued

$C(T)$  are calculated which bring the compressibility factors from equation (B1) into agreement with those of reference 29 for a pressure of  $10^2 \text{ MN/m}^2$ . For a temperature range of 300 K to 1000 K, these values of  $C(T)$  vary from  $2.002 \times 10^{-4}$  to  $2.195 \times 10^{-4}$ . With no appreciable loss of accuracy,  $C(T)$  is set equal to the constant  $2.1 \times 10^{-4}$  for the temperature range of 300 K to 600 K. The  $B(T)$  of equation (B4) and this constant value of  $C(T)$  result in compressibility factors within approximately 1 percent of those of reference 29 for the temperature range of 300 K to 1000 K and the pressure range of  $10^2 \text{ kN/m}^2$  to  $10^2 \text{ MN/m}^2$ .

The thermodynamic relations, in terms of the virial coefficients, for  $hW_o/RT$ ,  $sw_o/R$ ,  $c_v W_o/R$ , and  $a^2$  are (ref. 28)

$$\frac{hW_o}{RT} = \left( \frac{hW_o}{RT} \right)_{\text{perf}} + \rho \left[ B(T) - T \frac{dB(T)}{dT} \right] + \frac{\rho^2}{2} \left[ 2C(T) - T \frac{dC(T)}{dT} \right] \quad (\text{B5})$$

$$\frac{sw_o}{R} = \left( \frac{c_v W_o}{R} \right)_{\text{perf}} \ln T - \ln \rho - \rho \left[ B(T) + T \frac{dB(T)}{dT} \right] - \frac{\rho^2}{2} \left[ C(T) + T \frac{dC(T)}{dT} \right] + \left( \frac{sw_o}{R} \right)_{\text{ref}} \quad (\text{B6})$$

$$\frac{c_v W_o}{R} = \left( \frac{c_v W_o}{R} \right)_{\text{perf}} - T \left\{ \rho \left[ 2 \frac{dB(T)}{dT} + T \frac{d^2 B(T)}{dT^2} \right] + \frac{\rho^2}{2} \left[ 2 \frac{dC(T)}{dT} + T \frac{d^2 C(T)}{dT^2} \right] \right\} \quad (\text{B7})$$

$$a^2 = \left( \frac{\partial p}{\partial \rho} \right)_T + \frac{T}{c_v \rho^2} \left( \frac{\partial p}{\partial T} \right)_\rho^2 \quad (\text{B8})$$

where, from differentiation of equation (B1),

$$\left( \frac{\partial p}{\partial T} \right)_\rho = \frac{\rho R}{W_o} \left\{ 1 + \rho \left[ B(T) + T \frac{dB(T)}{dT} \right] + \rho^2 \left[ C(T) + T \frac{dC(T)}{dT} \right] \right\} \quad (\text{B9})$$

and

$$\left( \frac{\partial p}{\partial \rho} \right)_T = \frac{RT}{W_o} \left[ 1 + 2\rho B(T) + 3\rho^2 C(T) \right] \quad (\text{B10})$$

The  $(sw_o/R)_{\text{ref}}$  of equation (B6) is obtained for  $p = 1.01325 \times 10^2 \text{ kN/m}^2$  and  $T = 300 \text{ K}$  by using reference 10 for both helium and hydrogen. For helium, a value of  $(sw_o/R)_{\text{ref}} = 4.8024$  is calculated and, for hydrogen,  $(sw_o/R)_{\text{ref}} = -1.0363$ . (It should be noted that  $(sw_o/R)_{\text{ref}}$  is omitted in reference 28; hence, the values of  $sw_o/R$  plotted for helium in reference 28 differ from equation (B6) by a constant  $(sw_o/R)_{\text{ref}}$ .)

## APPENDIX B – Concluded

In the thermodynamic relations shown in equations (B5) to (B10), the independent variables are  $T$  and  $\rho$ . Hence, in generating an array of thermodynamic properties in region (3) for a range of  $T_3$  and a known  $s_3W_3/R$  (see section entitled "Determining Flow Quantities in Region (2)"), the corresponding  $\rho_3$  must be known. These  $\rho_3$  are determined iteratively from the implicit relation given by equation (B6). With  $T_3$  known and the corresponding  $\rho_3$  determined, corresponding values of  $Z$  and  $p$ ,  $h$ , and  $a$  may be calculated from equations (B1), (B5), and (B8), respectively.

## APPENDIX C

### COMPUTER-PROGRAM INPUTS, LISTING, AND FLOW CHART WITH SAMPLE DATA PRINTOUTS

The present program is written in FORTRAN IV language for Control Data 6000 series computers. Minimum machine requirements are 70 000 octal locations of core storage. The FORTRAN NAMELIST capability is used for data input with INP as the NAMELIST name. The units for the inputs which are physical quantities are given in the section entitled "Symbols." The program symbols and a brief description of the inputs necessary to utilize the computer program are listed as follows:

Program symbol	Description
P1	Pressure of quiescent test gas in region (1)
T1	Temperature of quiescent test gas in region (1)
US1	Incident-shock velocity into region (1)
P2	Static pressure in region (2)
P4	Driver-gas pressure in region (4)
T4	Driver-gas temperature in region (4)
U5	Velocity in region (5)
P5	Static pressure in region (5)
PCO <sub>2</sub>	Partial pressure of CO <sub>2</sub>
PN <sub>2</sub>	Partial pressure of N <sub>2</sub>
P <sub>O</sub> <sub>2</sub>	Partial pressure of O <sub>2</sub>
PAR	Partial pressure of Ar
PHE	Partial pressure of He
PH <sub>2</sub>	Partial pressure of H <sub>2</sub>
PMIX	Mixture pressure
TW	Model surface temperature

# APPENDIX C – Continued

Program symbol	Description
BNR	Model nose radius
RUN	Facility test number
NUMSP	Number of species considered (30 maximum)
JINDEX	Number of components considered (8 maximum)
IAR	Position in species array of Ar
IC	Position in species array of C
ICØ	Position in species array of CO
ICØ2	Position in species array of CO <sub>2</sub>
IN	Position in species array of N
IN2	Position in species array of N <sub>2</sub>
INØ	Position in species array of NO
IØ	Position in species array of O
IØ2	Position in species array of O <sub>2</sub>
IHE	Position in species array of He
IH	Position in species array of H
IH2	Position in species array of H <sub>2</sub>
NDRIV	NDRIV = 0 denotes helium driver gas NDRIV = 1 denotes hydrogen driver gas
LB	LB = 0 denotes inputs $p_1$ , $T_1$ , and $U_{s,1}$ used to find region ② quantities LB = 1 denotes inputs $p_1$ , $T_1$ , and $p_2$ used to find region ② quantities LB = 2 denotes inputs $p_1$ , $T_1$ , $p_4$ , and $T_4$ used to find region ② quantities

# APPENDIX C - Continued

Program symbol	Description
ISTET	ISTET = 0 denotes only quantities in regions (2) and (2,s) determined
	ISTET = 1 denotes all expansion-tube flow quantities determined
LF	LF = 1 denotes $U_5$ is basic input in region (5)
	LF = 2 denotes $p_5$ is basic input in region (5)
LD	LD = 0 denotes no standing shock at secondary diaphragm
	LD = 1 denotes existence of standing shock at secondary diaphragm
	LD = 2 denotes both cases (LD = 0 and LD = 1) are performed
LG	LG = 0 denotes frozen expansion is not performed
	LG = 1 denotes frozen expansion is performed
IREP	IREP = 0 denotes only a single value of $U_5$ is of interest for given region (A) quantities
	IREP = 1 denotes several $U_5$ of interest for given region (A) quantities
U5I	Velocity increment for IREP = 1
NVEL	Total number of $U_5$ of interest for IREP = 1 (10 maximum)
NUMUS	Number of $U_{s,1}$ in array for LB = 2

To minimize the number of inputs required for running cases on the computer, inputs are assigned values within the program as follows:

<u>Program symbol</u>	<u>Assigned value</u>
TW	300
BNR	0.0127
RUN	1.0
NDRIV	0

# APPENDIX C - Continued

<u>Program symbol</u>	<u>Assigned value</u>
ISTET	1
LD	2
LG	1
IREP	0
U5I	0
NVEL	0
NUMUS	16

These values may be changed from their assigned values by inclusion in the NAMELIST INP. For a given LB, only the basic parameters  $p_1$ ,  $T_1$ , and  $U_{s,1}$  ( $LB = 0$ ),  $p_2$  ( $LB = 1$ ), or  $p_4$  and  $T_4$  ( $LB = 2$ ) need be included in INP. Similarly, for a given LF, only  $U_5$  ( $LF = 1$ ) or  $p_5$  ( $LF = 2$ ) need be included in INP. Only the partial pressures of the quiescent test gas in region (1) need be included in conjunction with PMIX. It should be noted that the condition

$$PMIX = PC\emptyset 2 + PN2 + P\emptyset 2 + PAR + PHE + PH2$$

must be satisfied. Along with LB and LF, NUMSP and JINDEX must also be specified for each case. However, only the positions in the species array (for example, IAR, IC, IC $\emptyset$ , and so forth) of the species being considered need be included.

The 26 species and 5 components considered in references 6 and 7 and employed in the present program are as follows:

<u>Species</u>			<u>Components</u>
e <sup>-</sup>	O	C	e <sup>-</sup>
Ar	O <sup>+</sup>	C <sup>+</sup>	Ar
Ar <sup>+</sup>	O <sup>++</sup>	C <sup>++</sup>	N
Ar <sup>++</sup>	O <sup>-</sup>	C <sup>-</sup>	O
N	O <sub>2</sub>	CO	C
N <sup>+</sup>	O <sub>2</sub> <sup>+</sup>	CO <sup>+</sup>	
N <sup>++</sup>	O <sub>2</sub> <sup>-</sup>	CN	
N <sub>2</sub>	NO	CO <sub>2</sub>	
N <sub>2</sub> <sup>+</sup>	NO <sup>+</sup>		



## APPENDIX C – Continued

The thermodynamic data for these species, which are tabulated in reference 6, are read into the computer program from cards. A listing of these cards is presented in reference 18. An additional 6 species and 2 components considered in the present study are as follows:

<u>Species</u>		<u>Components</u>
H	He	He
H <sup>+</sup>	He <sup>+</sup>	H
H <sub>2</sub>	He <sup>++</sup>	

The thermodynamic data for these species are obtained from reference 22 and are also read into the computer program from cards.

A listing of this program, including subroutines, comments, sample input, and thermodynamic data for a mixture of He and H<sub>2</sub>, is reproduced in the following pages.

```

JOB.1,0700,070000,1000.          A3731  RGK143          1250          CENT
USER.MILLER, CHARLES G  III       000605575N 64720
RUN(S).
SETINDF. .
LGO. .
- .
PROGRAM MILLER(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT)
C DATA REDUCTION PROCEDURE FOR CO2-N2-O2-AR MIXTURES
C THERMODYNAMIC PROPERTIES OBTAINED FROM PROGRAM OF ALLISON
  DIMENSION TABH(50), TABA(50), TABANS(50), TABP(50), P5K(50), P5G(5
  10), TABT(50)
  DIMENSION RESULT(2)
  DIMENSION TABT1(50), TABR1(50), TABP1(50), TABH1(50)
  DIMENSION TABA1(50), TABU1(50)
  DIMENSION US11(30), U21(30), P21(30), H21(30), TABP21(30), TABT21(
  130)
  DIMENSION XSLM(5), BNON(5), R2X(5), U2X(5), H2X(5), T2X(5), P2X(5)
  1, A2X(5), RXR(5), RXH(5), RXU(5), RXP(5), RXT(5), RXA(5)
  DIMENSION XMOLE(30), SPECIE(30)
  REAL MS1,M2,M5,M55,MX,MN,MNS,MS,MA,M5F,M5SF,M5SFF
  EXTERNAL FOFX,FOFR,FOFMS
  COMMON /BLK1/ BT4,CT4,RHOG,T1,GAM4,W4,T4,P4,P1,T11,A1,Z1,G1,SR
  COMMON /BLK2/ BT1,CT1,T1,CVR1,S4R,SREF,DBT1,DCT1
  COMMON /BLK3/ LB,LD,LF,LG,NON,LU,NDRIV,ICOUNT,SAR,LCODE,DELU
  COMMON /BLK4/ NUMSP,JINDX,IAR,IN2,IO2,IC02,SOZ,XAR,XN2,XO2,XCO2
  COMMON /BLK5/ TMAX1,TMAX2,TMIN1,TMIN2,XMOLE,SPECIE
  COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
  COMMON /BLK7/ GE,WO
  NAMELIST /INP/ T1,P1,US1,P2,LB,LD,LF,LG,U5,P5,IREP,U51,NVEL,P4,T4,
  1RUN,1STET,NUMUS,NDRIV,TW,BNR,PCO2,PN2,PO2,PAR,PMIX,NUMSP,JINDX,ICO
  22,IN2,IO2,IAR,INO,ICO,IN,IO,IC,IH,IH2,IHE,PHE,PH2
  BOZ=0.
  CALL DAYTIM (RESULT)

  SHOCK TUBE PHASE
  NDRIV=0 DENOTES IMPERFECT HELIUM DRIVER GAS
  NDRIV=1 DENOTES IMPERFECT HYDROGEN GAS
  LB=0 DENOTES SHOCK TUBE INPUTS P1,T1,U51
  LB=1 DENOTES SHOCK TUBE INPUTS P1,T1,P2
  LB=2 DENOTES SHOCK TUBE INPUTS P1,T1,P4,T4
  1STET DENOTES PHASE(S) CALCULATED

```

# APPENDIX C - Continued

```

C      1STET=0 DENOTES SHOCK TUBE PHASE ONLY      A 39
C      1STET=1 DENOTES EXPANSION TUBE PHASE      A 40
C      LG=0 FROZEN EXPANSION NOT PERFORMED      A 41
C      LG=1 FROZEN EXPANSION IS PERFORMED      A 42
C      IREP=0 SINGLE VALUE OF US OF INTEREST      A 43
C      IREP=1 SEVERAL US OF INTEREST-FOR SETTING UP EXPANSION TUBE      A 44
C      US1 IS US INCREMENT FOR IREP=1      A 45
C      NVEL IS TOTAL NUMBER OF US OF INTEREST FOR IREP=1      A 46
C      RU=8.31434E+3      A 47
C      MM=0      A 48
C      US1=P2=P4=T4=US=P5=U=I=PCO2=PN2=P02=PAR=PHE=PH2=0.0      A 49
C      IAR=IN2=IN=I02=I0=INO=ICO=IC=IHE=IH=IREP=NVEL=NDRIV=0      A 50
C      1STET=LG=1      A 51
C      LD=2      A 52
C      NUMUC=15      A 53
C      RUN=1.      A 54
C      TW=300.      A 55
C      BNR=.0127      A 56
C      READ (5,INP)      A 57
C      IF (FNDFILE 5) 58.2      A 58
C      CONTINUE      A 59
C      PRINT 109, RESULT(1)      A 60
C      PRINT 70      A 61
C      PRINT 71      A 62
C      PRINT 72      A 63
C      PRINT 73      A 64
C      PRINT 74      A 65
C      PRINT 75, RUN,P1,T1,US1,P2,P4,T4      A 66
C      LU=0      A 67
C      NN=0      A 68
C      XCO2=PCO2/PMIX      A 69
C      XN2=PN2/PMIX      A 70
C      XO2=PO2/PMIX      A 71
C      XAR=PAR/PMIX      A 72
C      XHE=DHE/PMIX      A 73
C      XH2=DH2/PMIX      A 74
C      W0=44.011*XCO2+28.016*XN2+32.*XO2+39.944*XAR+4.003*XHE+2.016*XH2      A 75
C      PRINT 76      A 76
C      PRINT 75, W0,XCO2,XN2,XO2,XAR,XHE,XH2      A 77
C      ZMIX=1.E+4*(7.2906*XAR+10.2109*XCO2+7.7211*XN2+7.4243*XO2+1.5988*X      A 78
C      33      A 79
C      33      A 80
C      33      A 81

```

# APPENDIX C - Continued

	1HE+1.5767*XH2)/WO	A	82
	RHO1=(P1*WO)/(RU*T1)	A	83
	HW=(RU*TW*(4.5*XC02+3.5*(X02+XN2+XH2)+2.5*(XAR+XHE))/WO)-(3.93146E	A	84
	1+8*XC02/WO)	A	85
	H1=(RU*T1*(4.5*XC02+3.5*(X02+XN2+XH2)+2.5*(XAR+XHE))/WO)-(3.93146E	A	86
	1+8*XC02/WO)	A	87
	CPE=4.5*XC02+3.5*(XN2+X02+XH2)+2.5*(XHE+XAR)	A	88
	CVE=3.5*XC02+2.5*(XN2+X02+XH2)+1.5*(XHE+XAR)	A	89
	GE=CPE/CVE	A	90
	A1=SQRT(GE*RU*T1/WO)	A	91
	PRINT 59	A	92
	PRINT 60	A	93
	PRINT 79, P1,RHO1,T1,H1,GE,A1	A	94
	TMIN2=T1	A	95
	IF (LB.EQ.2) GO TO 5	A	96
	IF (LB.EQ.1) GO TO 3	A	97
	MS1=US1/A1	A	98
	GO TO 4	A	99
3	MS1=SQRT((.8*P2/P1)+.2)	A	100
4	TMAX2=1.05*T1*(2.*GE*MS1**2-GE+1.)*((GE-1.)*MS1**2+2.)/((GE+1.))*2	A	101
	1*MS1**2)	A	102
	CALL SC (RHO2,U2,P2,H2,RHO1,US1,P1,H1,W0)	A	103
	S2R=SR	A	104
	T2=TI1	A	105
	A2=A1	A	106
	Z2=Z1	A	107
	GAM2=G1	A	108
	M2=U2/A2	A	109
	MS1=US1/A1	A	110
	RE2=0.	A	111
	IF (T2.GT.8000.) GO TO 28	A	112
	CALL VISC (T2,VIS2)	A	113
	RE2=RHO2*U2/VIS2	A	114
	GO TO 28	A	115
	LU=20	A	116
5	R=8.11434E+3	A	117
	IF (NDRIV.EQ.1) GO TO 6	A	118
C		A	119
C	HELIUM	A	120
C		A	121
	HWRT=2.5	A	122
	CVRI=1.5	A	123
	SREF=4.8024	A	124
	GAM4=1.66667	A	125

```

W4=4.003
RHOG=(P4*W4)/(R*T4)
ALOW=.70*RHOG
GO TO 7
C
HYDROGEN
C
HVRT=3.5
CVR1=2.5
SREF=-1.0363
GAM4=1.4
W4=2.016
RHOG=(P4*W4)/(R*T4)
ALOW=.50*RHOG
AUP=1.05*RHOG
DELTX=(AUP-ALOW)/100.
E1=.1E-6
CALL BDT (BT4,CT4,DBT4,DCT4,D2BT4,D2CT4,T4)
RHOG=1.2*RHOG
CALL ITR1 (RHOG,DELTX,FOFX,E1,E1,200,ICODE)
IF (ICODE) 8,11,8
8 GO TO (9,10,10,10), ICODE
9 PRINT 77
GO TO 1
PRINT 78, ICODE
10 GO TO 1
Z4=1.+RHOG*BT4+RHOG**2*CT4
H4=(R*T4/W4)*(HVRT+RHOG*(BT4-T4*DBT4)+(RHOG**2/2.)*(2.*CT4-T4*DCT4
11)
S4R=CVR1*(ALOG(T4)-ALOG(RHOG)-RHOG*(BT4+T4*DBT4)-(RHOG**2/2.)*(CT4+
1T4*DCT4))+SREF
CVR=CVR1-T4*(RHOG*(2.*DBT4+T4*D2BT4)+(RHOG**2/2.)*(2.*DCT4+T4*D2CT
14))
PPTR=(RHOG*R/W4)*(1.+RHOG*(BT4+T4*DBT4)+(RHOG**2
1)
PPRT=(T4*R/W4)*(1.+2.*RHOG*BT4+3.*RHOG**2*CT4)
A4=SQRT(PPRT+((T4*W4)/(CVR*R*RHOG**2))*PPTR**2)
TABT1(1)=T4
TABP1(1)=P4
TABR1(1)=RHOG
TABZ1(1)=Z4
TABH1(1)=H4
TABAI(1)=1./A4
DELT=T4/49.

```

A 126  
A 127  
A 128  
A 129  
A 130  
A 131  
A 132  
A 133  
A 134  
A 135  
A 136  
A 137  
A 138  
A 139  
A 140  
A 141  
A 142  
A 143  
A 144  
A 145  
A 146  
A 147  
A 148  
A 149  
A 150  
A 151  
A 152  
A 153  
A 154  
A 155  
A 156  
A 157  
A 158  
A 159  
A 160  
A 161  
A 162  
A 163  
A 164  
A 165  
A 166  
A 167  
A 168  
A 169

```

12  NU=1
    DO 12 I=2,50
      TABTI(I)=T4-FLOAT(I-1)*DELT
    CONTINUE
    TABTI(50)=TABTI(50)+4.5
    AUP=1.1*RHO4
    ALLOW=.0001
    DELR=(AUP-ALLOW)/200.
    RI=RHO4
    DO 19 I=2,50
      TI=TABTI(I)
      CALL BDT (BTI,CTI,DBTI,DCTI,D2BTI,D2CTI,TI)
      CALL ITR2 (RI,ALLOW,AUP,DELR,FOFR,EI,E1,400,ICODE)
      IF (ICODE) 13,18,13
13   GO TO (14,15,15,16), ICODE
14   PRINT 77
      GO TO 17
15   PRINT 78, ICODE
      GO TO 17
16   PRINT 80, ICODE,RI,DELR
17   PRINT 61
      PRINT 62, NU
18   TABRI(I)=RI
      TABZI(I)=1.+RI*BTI+RI**2*CTI
      TABPJ(I)=TI*(R/W4)*RI*TABZI(I)
      TABHI(I)=(R*TI/W4)*(HWRT+RI*(BTI-TI*DBTI)+(RI**2/2.)*(2.*CTI-TI*DC
        ITI))
      CVIR=CVRI-TI*(RI*(2.*DBTI+TI*D2BTI)+(RI**2/2.)*(2.*DCTI+TI*D2CTI))
      PPTRI=(RI*R/W4)*(1.+RI*(BTI+TI*DBTI)+(RI**2)*(CTI+TI*DCTI))
      PPRTI=(TI*R/W4)*(1.+2.*RI*BTI+3.*RI**2*CTI)
      TABAI(I)=1./(SQRT(PPRTI+((TI*W4)/(CVIR*RI**2))*PPTRI**2))
      NU=NU+1
19   CONTINUE
      CALL SIMR (TABHI,TABAI,NU,NU,TABANS)
      MS=1.4
      DELS=.2
      CALL ITR1 (MS,DELS,FOFMS,EI,E1,200,ICODE)
      IF (ICODE) 20,23,20
20   GO TO (21,22,22), ICODE
21   PRINT 77
      GO TO 1
22   PRINT 78, ICODE
      GO TO 1
23   USMAX=1.1*A1*MS

```

A 170  
 A 171  
 A 172  
 A 173  
 A 174  
 A 175  
 A 176  
 A 177  
 A 178  
 A 179  
 A 180  
 A 181  
 A 182  
 A 183  
 A 184  
 A 185  
 A 186  
 A 187  
 A 188  
 A 189  
 A 190  
 A 191  
 A 192  
 A 193  
 A 194  
 A 195  
 A 196  
 A 197  
 A 198  
 A 199  
 A 200  
 A 201  
 A 202  
 A 203  
 A 204  
 A 205  
 A 206  
 A 207  
 A 208  
 A 209  
 A 210  
 A 211  
 A 212  
 A 213

```

USMIN=.65*USMAX
US11(1)=USMAX
DEL1=(USMAX-USMIN)/FLOAT(NUMUS)
MS1=US11(1)/A1
TMAX2=1.05*T1*(2.*GE*MS1**2-GE+1.)*((GE-1.)*MS1**2+2.)/((GE+1.))**2
1*MS1**2)
DO 24 I=1,NUMUS
US11(I)=USMAX-FLOAT(I-1)*DEL1
CALL SC (RH2I,U2I(I),P2I(I),H2I(I),RHO1,US11(I),PI,HI,WO)
TABT2I(I)=T1I
TABP2I(I)=P2I(I)
TMAX2=T1I
CONTINUE
CALL SOLUT (TABANS,TABPI,U2I,P2I,NU,NUMUS,UR,P)
P2=P
U2=UR
CALL FTLUP (P2,T2,-2,NUMUS,TABP2I,TABT2I)
P2U=P2/1.01325E+5
CALL ROGO (P2U,RHO2,H2,S2R,T2,A2,Z2,GAM2,WO)
US1=U2/(1.-RHO1/RHO2)
MS1=US1/A1
M2=U2/A2
RE2=0.
IF (T2.GT.8000.) GO TO 25
CALL VISC (T2,VIS2)
RE2=RHO2*U2/VIS2
IF (LB.NE.2) GO TO 28
IF (NDRIV.EQ.0) GO TO 26
PRINT 81
GO TO 27
PRINT 82
PRINT 83
PRINT 84
PRINT 85, P4,RHO4,T4,H4,S4R,Z4,A4,W4
PRINT 86
PRINT 87
PRINT 88, P2,RHO2,T2,H2,S2R,Z2,GAM2,A2,U2,M2,RE2
RAP=P2/P1
RARHO=RHO2/RHO1
RAT=T2/T1
RAH=H2/H1
PRINT 89
PRINT 90
PRINT 91, RAP,RARHO,RAT,RAH,MS1,US1

```

```

29 PRINT 92
C PRINT 93
C DO 29 I=1,NUMSP
C PRINT 94, SPECIE(I),XMOLE(I)
C CONTINUE
C
C STANDING SHOCK AT SECOND DIAPHRAGM
C
C LD=0 DENOTES NO STANDING SHOCK
C LD=1 DENOTES EXISTENCE OF STANDING SHOCK
C LD=2 DENOTES BOTH CASES WILL BE RUN
C
C IF (LD.EQ.0.AND.ISTET.EQ.0) GO TO 1
C IF (LD.EQ.0.OR.LD.EQ.2) GO TO 31
111 CALL SHOCK (BSNS2,CSNS2,DSNS2,RHO2,U2,P2,H2)
C RHOA=4.*RHO2
C UA=BSNS2/RHOA
30 PA=CSNS2-BSNS2*UA
C HA=DSNS2-.5*UA**2
C TMIN2=T2
C TMAX2=1.05*T2*(2.*GAM2*M2**2-GAM2+1.)*((GAM2-1.)*M2**2+2.)/((GAM2+
11.)*M2**2)
C CALL FIND (PA,RNEW,HA,SAR,TA,AA,ZA,GAMA,WO,2,2)
C IF (ABS(1.-RNEW/RHOA).LE..001) GO TO 32
C RHOA=RNEW
C GO TO 30
31 PA=P2
C RHOA=RHO2
C TA=T2
C SAR=S2R
C HA=H2
C AA=A2
C UA=U2
C ZA=Z2
C GAMA=GAM2
C REA=RE2
C MA=UA/AA
C GO TO 35
32 RHOA=RNEW
C MA=UA/AA
C REA=0.
C IF (TA.GT.8000.) GO TO 33
C CALL VISC (TA,VISA)
C REA=RHOA*UA/VISA

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# APPENDIX C - Continued

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33 PRINT 95
34 PRINT 87
35 PRINT 88. PA,RHOA,TA,HA,SAR,ZA,GAMA,AA,UA,MA,REA
36 PRINT 96
37 PRINT 93
38 DO 34 I=1,NUMSP
39 PRINT 97. SPECIE(I),XMOLE(I)
40 CONTINUE
41 IF (ISTET.EQ.0) GO TO 1
42
43 EXPANSION TUBE PHASE
44
45 LF=1 DENOTES U5 IS BASIC INPUT
46 LF=2 DENOTES P5 IS BASIC INPUT
47
48 FROZEN FLOW- EXPANSION TUBE
49
50 IF (IC02.NE.0) GO TO 36
51 XMOLE(IC0)=XMOLE(IC)=XMOLE(IC02)=0.
52 IF (IAR.NE.0) GO TO 37
53 XMOLF(IAR)=0.
54 IF (IN2.NE.0) GO TO 38
55 XMOLE(IN2)=XMOLE(INO)=XMOLE(IN)=0.
56 IF (IO2.NE.0) GO TO 39
57 XMOLE(IO2)=XMOLE(INO)=XMOLE(IO)=0.
58 IF (IHE.NE.0) GO TO 40
59 XMOLF(IHE)=0.
60 IF (IH2.NE.0) GO TO 41
61 XMOLE(IH2)=XMOLE(IH)=0
62 ATRO1=XMOLE(IN2)+XMOLE(IO2)+XMOLE(INO)+XMOLE(IC0)+XMOLE(IH2)
63 ATRO2=XMOLE(IAR)+XMOLE(IN)+XMOLE(IO)+XMOLE(IC)+XMOLE(IHE)+XMOLE(IH
64 1)
65 GAMACT=(9.*XMOLE(IC02)+7.*ATRO1+5.*ATRO2)/(7.*XMOLE(IC02)+5.*ATRO1
66 1+3.*ATRO2)
67 AACT=SQRT(GAMACT*ZA*RU*TA/WO)
68 HO1=1.E+8*(4.70729*XMOLE(IN)+2.46741*XMOLE(IO)+.8986*XMOLE(INO)-3.
69 193146*XMOLE(IC02)-1.13813*XMOLE(IC0)+7.11238*XMOLE(IC)+2.16013*XMO
70 2LE(IH))/WO
71 HACT=AACT**2/(GAMACT-1.))+HO1
72 HFRO=HA-HACT
73 IF (LF.EQ.2) GO TO 44
74 U5F=U5
75 ASF=AACT+((GAMACT-1.)/2.)*(UA-U5F)

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 A 344

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IF (ASF.GT.0.) GO TO 43
PRINT 63
TMAX1=TA
TMIN1=1.
P5F=.1
GO TO 47
P5F=PA*((ASF/AACT)**(2.*GAMACT/(GAMACT-1.)))
GO TO 45
P5F=P5
ASF=AACT*(P5F/PA)**((GAMACT-1.)/(2.*GAMACT))
U5F=2.*(AACT-ASF)/(GAMACT-1.)+UA
M5F=U5F/ASF
T5F=TA*(ASF/AACT)**2
IF (LG.EQ.0) GO TO 46
RH05F=P5F*W0/(RU*ZA*T5F)
S5RF=SAR
H5F=HACT*(T5F/TA)
Z5F=ZA
GAM5F=GAMACT
CALL VISC (T5F,V155F)
RESF=RH05F*U5F/V155F
PRINT 98
PRINT 87
PRINT 88. P5F,RH05F,T5F,H5F,S5RF,Z5F,GAM5F,ASF,U5F,M5F,RESF

SHOCK CROSSING - FROZEN EXPANSION - EQUILIBRIUM POST SHOCK

H5FSC=H5F+HFRO
TMIN2=TA
TMAX2=1.05*T5F*(2.*GAM5F*M5F**2-GAM5F+1.)*((GAM5F-1.)*M5F**2+2.)/(
1(GAM5F+1.))*2*M5F**2)
CALL SNS (R5SF,U5SF,P5SF,H5SF,S5SRF,T5SF,A5SF,Z5SF,G5SF,M5SF,RH05F
1,U5F,P5F,H5FSC,HT5F,PT5F,RT5F,ST5RF,TT5F,AT5F,ZT5F,GT5F,W0)
RR5SF=R5SF/RH05F
PRINT 102
PRINT 99
PRINT 104
PRINT 88. P5SF,R5SF,T5SF,H5SF,S5SRF,Z5SF,G5SF,A5SF,U5SF,M5SF,RR5SF
PRINT 106
PRINT 99
PRINT 107
QTZOF=(1./ZMIX)*SORT(PT5F/BNR)*(HT5F-HW)
PRINT 108. PT5F,RT5F,TT5F,HT5F,ZT5F,GT5F,AT5F,QTZOF,BNR

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43

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C

C

C

C

# APPENDIX C - Continued

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C      SHOCK CROSSING-FROZEN EXPANSION-FROZEN POSTSHOCK
C
PRINT 102
PRINT 100
PRINT 104
P5SFF=P5F*(2.*GAMACT*MSF**2-GAMACT+1.)/(GAMACT+1.)
R5SFF=(RH05F*(GAMACT+1.)*MSF**2)/(GAMACT-1.)*MSF**2+2.)
RR5SFF=R5SFF/RH05F
T5SFF=P5SFF*WO/(R5SFF*RU*ZA)
H5SFF=H5F*T5SFF/T5F
G5SFF=GAMACT
A5SFF=A5F*SQRT(T5SFF/T5F)
U5SFF=RH05F*U5F/R5SFF
MS5FF=U5SFF/A5SFF
S5SRFF=(ALOG(P5SFF/P5F)-GAMACT*ALOG(R5SFF/RH05F))/(GAMACT-1.)*S5RF
Z5SFF=ZA
PRINT 88. P5SFF,R5SFF,T5SFF,H5SFF,S5SRFF,Z5SFF,G5SFF,A5SFF,U5SFF,M
15SFF,RR5SFF
PRINT 106
PRINT 100
PRINT 107
HT5FF=H5F+.5*U5F**2
TT5FF=T5SFF*(1.+(GAMACT-1.)*MS5FF**2)/2.)
PT5FF=P5SFF*(1.+(GAMACT-1.)*MS5FF**2)/2.)**(GAMACT/(GAMACT-1.))
RT5FF=PT5FF*WO/(TT5FF*ZA*RU)
ZT5FF=ZA
GT5FF=GAMACT
AT5FF=A5SFF*SQRT(TT5FF/T5SFF)
QTZOFF=(1./ZMIX)*SQRT(PT5FF/BNR)*(HT5FF-HW)
PRINT 108. PT5FF,RT5FF,TT5FF,HT5FF,ZT5FF,GT5FF,AT5FF,QTZOFF,BNR
TMAX1=TA
TMIN1=T5F
IF (LF.EQ.2) GO TO 50
LF=1 CASE
DELU=U5-UA
PSK(1)=PA
P5G(1)=ALOG10(PA)
DELPG=(P5G(1)-ALOG10(P5F))/49.
TABH(1)=HA
TABA(1)=1./AA
TABP(1)=PSK(1)
TABT(1)=TA

```

```

DO 49 J=2,50
P5G(J)=P5G(J-1)-DELPG
P5K(J)=10.*P5G(J)
CALL FIND (P5K(J),RHOK,HK,SAR,TK,AK,ZK,GK,WO,3,1)
TABH(J)=HK
TABA(J)=1./AK
TABP(J)=P5K(J)
TABT(J)=TK
TMAX1=TK
CONTINUE
CALL SIMR (TABH,TABA,50,50,TABANS)
IF (LF.EQ.2) GO TO 51
CALL FTLUP (DELU,H5,2,NON,TABANS,TABH)
CALL FTLUP (H5,P5,-2,50,TABH,TABP)
CALL FTLUP (H5,T5,-2,50,TABH,TABT)
P5U=P5/1.01325E+5
CALL ROGO (P5U,R5,H5,S5R,T5,A5,ZZ5,GAM5,WO)
GO TO 52

C
C
C
50
LF=2 CASE
CALL FIND (P5,R5,H5,SAR,T5,A5,ZZ5,GAM5,WO,3,1)
P5K(1)=PA
P5G(1)=ALOG10(PA)
DELPG=(P5G(1)-ALOG10(P5))/49.
GO TO 48
U5=UA+TABANS(50)
M5=U5/A5
CALL VISC (T5,VIS5)
RES=R5*U5/VIS5
PRINT 101
PRINT 87
PRINT 88, P5,R5,T5,H5,SAR,ZZ5,GAM5,A5,U5,M5,RES
PRINT 64
PRINT 93
DO 53 I=1,NUMSP
PRINT 97, SPECIE(I),XMOLE(I)
CONTINUE
IF (IREP.EQ.0) GO TO 54
PTSES=.97*R5*U5**2
HTSES=H5+.5*U5**2
QTZOES=(1./ZMIX)*SQRT(PTSES/BNR)*(HTSES-HW)
P100=P5/(1.+(4.003/(RU*T1))*U5**2)
US10=1.333*U5

51
52
53

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A 475  
A 476

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A10=SQRT((1.6667*RU*T1)/4.003)
MS10=US10/A10
P10=4.*P5/(5.*MS10**2-1.)
US1C=3.281*US1
USC=3.281*US
P4C=1.45E-4*P4
P2C=1.45E-4*P2
P1C=1.45E-4*P1
P5C=1.45E-4*P5
PT5C=1.45E-4*PT5ES
QTZOEC=QTZOES/1.1349F+4
P10C=7.501E-3*P10
P100C=7.501E-3*P100
PRINT 65
PRINT 66
PRINT 67
PRINT 68
PRINT 105, P1C,P4C,P2C,P5C,PT5C,US1C,USC,QTZOEC,P10C,P100C
TMIN2=TA
TMAX2=1.05*T5*(2.*GAM5*MS**2-GAM5+1.)*((GAM5-1.)*MS**2+2.)/((GAM5+
11.)*MS**2)
CALL SNS (RH05S,U5S,P5S,H5S,S5SR,T5S,A5S,Z5S,GAME5S,M5S,R5,U5,P5,H
15,HT5,PT5,RT5,ST5,TT5,AT5,ZT5,GAMET5,W0)
PRINT 102
PRINT 103
PRINT 104
RR5S=RH05S/R5
PRINT 88, P5S,RH05S,T5S,H5S,S5SR,Z5S,GAME5S,A5S,U5S,M5,RR5S
PRINT 106
PRINT 103
PRINT 107
QTZO=(1./ZMIX)*SQRT(PT5/BNR)*(HT5-HW)
PRINT 108, PT5,RT5,TT5,HT5,ZT5,GAMET5,AT5,QTZO,BNR
PRINT 69
PRINT 93
DO 55 I=1,NUMSP
PRINT 97, SPECIE(I),XMOLE(I)
CONTINUE
NN=NN+1
IF (IREP.EQ.0.OR.NVEL.EQ.NN) GO TO 57
IF (NN.GT.10) GO TO 57
U5=UR+U51
GO TO 42
IF (LO.NE.2) GO TO 110

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54

55

56

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110  US=US-(FLOAT(NVEL)-1.)*U5I
111  NN=0
112  LD=1
113  GO TO 111
114  IF (ISTET.EQ.1) GO TO 1
115  STOP
116
117  FORMAT (//34H 1 CONDITIONS - QUIESCENT TEST GAS)
118  FORMAT (//55H P RHO T H GAM
119  1A)
120  FORMAT (//26H NUMBER OF P3.T3 IN ARRAY)
121  FORMAT (15)
122  FORMAT (//45H ASF IS NEGATIVE - FROZEN FLOW NOT CALCULATED)
123  FORMAT (//27H MOLE FRACTIONS IN REGION 5)
124  FORMAT (//45H IMPORTANT PARAMETERS FOR SETTING UP EXP TUBE)
125  FORMAT (//46H P1.P4.P2.P5.PT5 IN PSI - P10.P100 IN MM OF HG)
126  FORMAT (36H US1.U5 IN FPS - QT5 IN BTU/FTSQ-SEC)
127  FORMAT (//97H P1 P4 P2 P5 PT5
128  1S1 U5 QT5 P10 P100)
129  FORMAT (//28H MOLE FRACTIONS IN REGION T5)
130  FORMAT (//50H EXPANSION TUBE PROGRAM OF MILLER FOR GAS MIXTURES)
131  FORMAT (51H ALL PHYSICAL QUANTITIES IN MKS UNITS- NASA SP-7012)
132  FORMAT (//28H SHOCK TUBE PHASE OF PROGRAM)
133  FORMAT (//37H MEASURED INPUTS FOR SHOCK TUBE PHASE)
134  FORMAT (//66H RUN P1 T1 P2
135  1 P4 T4)
136  FORMAT (7E10.3)
137  FORMAT (//68H WO XC02 XN2 X02 XAR
138  1 XHE XH2)
139  FORMAT (20H MAX COUNT EXCEEDED )
140  FORMAT (17H DERIVATIVE = 0. .15)
141  FORMAT (6E10.3)
142  FORMAT (7H ICODE=.15.5H RI=.E12.3.7H DELR=.E12.3)
143  FORMAT (//30H IMPERFECT HYDROGEN DRIVER GAS)
144  FORMAT (//28H IMPERFECT HELIUM DRIVER GAS)
145  FORMAT (//13H 4 CONDITIONS)
146  FORMAT (//75H P RHO T H S/R
147  1 A W)
148  FORMAT (8E10.3)
149  FORMAT (//32H 2 CONDITIONS- REAL GAS MIXTURES)
150  FORMAT (//106H P RHO T M S/R
151  1Z GAME A U NRE)
152  FORMAT (11E10.3)

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89  FORMAT (//36H RATIO- 2 CONDITIONS TO 1 CONDITIONS)
90  FORMAT (/55H  P      RHO      T      H      MS1      US
11)
91  FORMAT (6E10.3)
92  FORMAT (//27H MOLE FRACTIONS IN REGION 2)
93  FORMAT (/29H SPECIE      MOLE FRACTION/)
94  FORMAT (A10.E16.4)
95  FORMAT (//33H CONDITIONS BEHIND STANDING SHOCK)
96  FORMAT (//43H MOLE FRACTIONS BEHIND SHOCK AT SECOND DIA.)
97  FORMAT (A10.E16.4)
98  FORMAT (//34H 5 CONDITIONS FOR FROZEN EXPANSION)
99  FORMAT (41H FROZEN EXPANSION--EQUILIBRIUM POST SHOCK)
100  FORMAT (37H FROZEN EXPANSION-- FROZEN POST SHOCK)
101  FORMAT (//39H 5 CONDITIONS FOR EQUILIBRIUM EXPANSION)
102  FORMAT (//42H STATIC(5S) CONDITIONS BEHIND NORMAL SHOCK)
103  FORMAT (46H EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK)
104  FORMAT (/109H  P      RHO      T      H      S/R
1Z  GAME      A      U      M      R5S/R5)
105  FORMAT (10E10.3)
106  FORMAT (//46H STAGNATION(T5) CONDITIONS BEHIND NORMAL SHOCK)
107  FORMAT (/85H  P      RHO      T      H      Z
1AME  A      QT      RN)
108  FORMAT (9E10.3)
109  FORMAT (IH1.A10/)
END
SUBROUTINE VISC (T1,VISMIX)
  DIMENSION VIS(6), W(6), XMF(6), PHI(6.6), SUM(6.6)
  COMMON /BLK4/ NUMSP,JINDX,IAR,IN2,IO2,IC02,BOZ,XAR,XN2,XO2,XC02
  COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
  VIS(1)=3.33E-7*T1**.739
  VIS(5)=3.92E-7*T1**.7
  IF (T1.GT.950.) GO TO 2
  VIS(2)=(-.973034+.5522198*T1-1.613866E-4*T1**2)*1.E-7
  VIS(3)=(22.99167+.5558644*T1-1.84356E-4*T1**2)*1.E-7
  VIS(4)=(19.93933+.6623589*T1-2.04096E-4*T1**2)*1.E-7
  VIS(6)=(23.877+.21918*T1-4.4304E-5*T1**2)*1.E-7
  GO TO 3
2  VIS(2)=(150.2874+.248903*T1-6.174675E-6*T1**2)*1.E-7
  VIS(3)=(163.8798+.2460075*T1-7.738745E-6*T1**2)*1.E-7
  VIS(4)=(230.3+.2559657*T1-2.264286E-6*T1**2)*1.E-7
  VIS(6)=(63.197+.14093*T1-8.6387E-6*T1**2)*1.E-7
  W(1)=39.944
  W(2)=44.011
  W(3)=28.016
3
1  B 1
   B 2
   B 3
   B 4
   B 5
   B 6
   B 7
   B 8
   B 9
   B 10
   B 11
   B 12
   B 13
   B 14
   B 15
   B 16
   B 17
   B 18
   B 19

```

```

20 W(4)=32.
21 W(5)=4.003
22 W(6)=2.016
23 XMF(1)=XAR
24 XMF(2)=XCO2
25 XMF(3)=XN2
26 XMF(4)=XO2
27 XMF(5)=XHE
28 XMF(6)=XH2
29 DO 5 I=1.6
30 DO 5 J=1.6
31 PHI(I,J)=(((1.+SQRT(VIS(I)/VIS(J))*(W(J)/W(I))**.25)**2)/(2.8284*S
32 I*QRT(1.+W(I)/W(J)))
33 IF (XMF(I).EQ.0.) GO TO 4
34 SUM(I,J)=PHI(I,J)*XMF(J)/XMF(I)
35 GO TO 5
36 SUM(I,J)=0.
37 CONTINUE
38 DO 6 I=1.6
39 SUM(I)=SUM(I,1)+SUM(I,2)+SUM(I,3)+SUM(I,4)+SUM(I,5)+SUM(I,6)
40 IF (SUM(I).NE.0.) GO TO 6
41 SUM(I)=1.
42 VIS(I)=0.
43 CONTINUE
44 VISMI=(VIS(1)/SUMM(1))+(VIS(2)/SUMM(2))+(VIS(3)/SUMM(3))+(VIS(4)/
45 1SUMM(4))+(VIS(5)/SUMM(5))+(VIS(6)/SUMM(6))
46 RETURN
47- END
1 SUBROUTINE SHOCK (BN,CN,DN,RN,UN,PN,HN)
2 BN=RN*UN
3 CN=PN+RN*UN**2
4 DN=HN+.5*UN**2
5 RETURN
6- END
1 FUNCTION FOFX (RN)
2 COMMON /BLK1/ BT4,CT4,RHOG,T1,GAM4,W4,T4,P4,P1,T11,A1,Z1,G1,SR
3 FOFX=RHOG-(BT4*RN**2+CT4*RN**3)
4 RETURN
5- END
1 FUNCTION FOFR (RN)
2 COMMON /BLK2/ BT1,CT1,T1,CVR1,S4R,SREF,DBT1,DCT1
3 A=CVRI#ALOG(T1)
4 B=BT1+T1*DBT1
5 C=CT1+T1*DCT1

```



# APPENDIX C - Continued

```

1      FOFR=A-ALOG(RNI)-(RNI*B)-(RNI**2/2.)*C+SREF-S4R
      RETURN
      END
      FUNCTION FOFMS (MSN)
      COMMON /BLK1/ BT4,CT4,RHOG,T1,GAM4,W4,T4,P4,P1,T11,AI,ZI,G1,SR
      COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
      COMMON /BLK7/ GE,WO
      REAL MSN
      A=P4/PI
      B=SQRT((GE*W4*T1)/(GAM4*WO*T4))
      C=(GAM4-1.)/(GE+1.)
      D=2.*GAM4/(GAM4-1.)
      E=(1.-B*C*(MSN-1./MSN))**D
      FOFMS=SQRT((A*(GE+1.)*E+GE-1.)/(2.*GE))
      RETURN
      END
      SUBROUTINE SIMR (TABX,TABY,N,NMAX,TABANS)
      DIMENSION TABX(NMAX), TABY(NMAX), TABANS(NMAX)
      DIMENSION NP(4)
      COMMON /BLK3/ LB,LD,LF,LG,NON,LU,NDRIV,ICOUNT,SAR,LCODE,DELU
      TABANS(1)=0
      DEN=2.
      K=2
      ICOUNT=0
      DO 2 J=K,N
      NON=J
      DELX=(TABX(J)-TABX(J-1))/DEN
      X=TARX(J-1)+DELX
      CALL FTLP (X,Y,2,N,TABX,TABY)
      SUM=(TABY(J-1)+4.*Y+TABY(J))*(ABS(DELX))/3.
      TABANS(J)=TABANS(J-1)+SUM
      IF (LU.NE.20) GO TO 1
      1      CONTINUE
      IF (LF.EQ.2.OR.LU.EQ.20) GO TO 2
      IF (TABANS(J).LT.DELU) GO TO 2
      ICOUNT=ICOUNT+1
      IF (ICOUNT.GT.3) GO TO 3
      2      CONTINUE
      3      RETURN
      END
      SUBROUTINE SNS (RX,UX,PX,HX,SX,TX,AX,ZX,GX,MX,R5X,U5X,P5X,H5X,HTX,
      IPTX,RTX,STX,TTX,ATX,7TX,GTX,WO)
      DIMENSION XMOLE(30), SPECIE(30)
      REAL M51,M2,M5,M55,MX,MN,MNS

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COMMON /BLK4/ NUMSP,JINDX,IAR,IN2,I02,IC02,BOZ,XAR,XN2,X02,XC02
COMMON /BLK5/ TMAX1,TMAX2,TMIN1,TMIN2,XMOLE,SPECIE
COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
CALL SHOCK (BSN,CSN,DSN,R5X,U5X,P5X,H5X)
RX=10.*R5X
HTX=DSN
UX=BSN/RX
PX=CSN-BSN*UX
HX=DSN-.5*UX**2
CALL FIND (PX,RNEW,HX,SX,TX,AX,ZX,GX,WO,2,2)
IF (ABS(1.-RX/RNEW).LE.001) GO TO 2
RX=RNEW
GO TO 1
MX=UX/AX
PTX=PX*(1.+(GX-1.)/2.)*MX**2)**(GX/(GX-1.))
CALL FIND (PTX,RTX,HTX,STX,TTX,ATX,ZTX,GTX,WO,2,2)
RETURN
END
SUBROUTINE BDT (BTM,CTM,DBM,DCM,D2BM,D2CM,TM)
COMMON /BLK3/ LB,LD,LF,LG,NON,LU,NDRIV,ICOUNT,SAR,LCODE,DELU
IF (NDRIV.EQ.1) GO TO 1
HELIUM USED AS DRIVER GAS
AMT1=15.8922-ALOG(TM)
AMT2=-3.7156E-3*TM
BTM=3.3565E-6*AMT1**3-2.0085E-3*EXP(AMT2)
CTM=.5.633E-12*AMT1**6
DBM=(-1.00695E-5/TM)*AMT1**2+7.4628E-6*EXP(AMT2)
DCM=(-3.3798E-11/TM)*AMT1**5
D2BM=(2.0139E-5/TM**2)*AMT1+(1.00695E-5/TM**2)*AMT1**2-2.7729E-8*E
1XP(AMT2)
D2CM=(1.6899E-10/TM**2)*AMT1**4+(3.3798E-11/TM**2)*AMT1**5
GO TO 2
HYDROGEN USED AS DRIVER GAS
BTM=1.6994E-3*TM**2.25
CTM=2.1E-4
DBM=4.2485E-4*TM**(-.75)
DCM=D2CM=0.
D2BM=-3.1864E-4*TM**(-1.75)
RETURN

```

# APPENDIX C - Continued

1	26-
1	1
2	2
3	3
4	4
5	5
6	6
7	7
8	8
9	9
10	10
11	11
12	12
13	13
14	14
15	15
16	16
17	17
18	18
19	19
20	20
21	21
22	22
23	23
24	24
25	25
26	26
27-	27-

```

END
SUBROUTINE SC (R2I,UI,P1,H1,R1I,US,P,H,WO)
  DIMENSION XMOLE(30), SPECIE(30)
  COMMON /BLK1/ BT4,CT4,RHOG,T1,GAM4,W4,T4,P4,P1,T1I,A1,Z1,G1,SR
  COMMON /BLK3/ LB,LD,LF,LG,NON,LU,NDRIV,ICOUNT,SAR,LCODE,DELU
  COMMON /BLK4/ NUMSP,JINDX,IAR,IN2,IO2,ICO2,BOZ,XAR,XN2,XO2,XCO2
  COMMON /BLK5/ TMAX1,TMAX2,TMIN1,TMIN2,XMOLE,SPECIE
  COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
  R2I=10.*R1I
  IF (LB.EQ.1) GO TO 2
  CALL SHOCK (B,C,D,R1I,US,P,H)
  UI=US*(1.-R1I/R2I)
  PI=C-(R2I*(US-UI)**2)
  HI=D-.5*(US-UI)**2
  CALL FIND (P1,RNEW,H1,SR,T1I,A1,Z1,G1,WO,2,2)
  IF (ABS(1.-RNEW/R2I),LE,.001) GO TO 3
  R2I=RNEW
  GO TO 1
2  US=SQRT((PI-P)/(R1I*(1.-R1I/R2I)))
  UI=US*(1.-R1I/R2I)
  HI=H+.5*(US**2-(US-UI)**2)
  CALL FIND (P1,RNEW,H1,SR,T1I,A1,Z1,G1,WO,2,2)
  IF (ABS(1.-RNEW/R2I),LE,.001) GO TO 3
  R2I=RNEW
  GO TO 2
3  R2I=RNEW
  RETURN
END
SUBROUTINE SOLUT (U3,P3,U2,P2,M,N,UR,P)
  DIMENSION U3(20), P3(20), U2(10), P2(10), U(2)
  FUNCD(PP,UU,R)=PP-UU*R
  FUNAR(P,PP,U,UU)=(P-PP)/(U-UU)

  USE END POINTS FOR FIRST INTERSECTION

  MR=1
  NR=1
  IF (P2(1).GT.P2(2)) NR=-NR
  IF (P3(1).GT.P3(2)) MR=-MR
  P31=P3(1)
  P32=P3(M)
  P21=P2(1)
  P22=P2(N)
  U21=U2(1)

```

```

17 K U22=U2(N)
18 K U31=U3(1)
19 K U32=U3(M)
20 K AA=FUNAB(P22,P21,U22,U21)
21 K BB=FUNAB(P32,P31,U32,U31)
22 K CC=FUNCD(P21,U21,AA)
23 K DD=FUNCD(P31,U31,BB)
24 K UR=(CC-DD)/(BB-AA)
25 K PR=CC+UR*AA
26 K CALL FTLUP (PR,U(1),NR,N,P2,U2)
27 K CALL FTLUP (PR,U(2),MR,M,P3,U3)
28 K IF (ABS((U(1)-U(2))/U(1))-0.0001) 3,3,2
29 K P31=P32
30 K P32=PR
31 K P21=P22
32 K P22=PR
33 K U31=U32
34 K U32=U(2)
35 K U21=U22
36 K U22=U(1)
37 K GO TO 1
38 K P=PR
39 K RETURN
40- K END
1 L SUBROUTINE FIND (P,RHO,H,SR,T,AM,ZM,GAME,MU,K,L)
2 L
3 L
4 L
5 L
6 L
7 L
8 L
9 L
10 L
11 L
12 L
13 L
14 L
15 L
16 L
17 L
18 L
19 L
20 L

C FIND OBTAINS THERMODYNAMIC PROPERTIES FROM SUBROUTINE ROGO WITH-
C (1) PRESSURE AND DENSITY (K=1)
C (2) PRESSURE AND ENTHALPY (K=2)
C (3) PRESSURE AND ENTROPY (K=3)
C (4) DENSITY AND ENTHALPY (K=4)

C UPPER LIMIT ON T AS REQUIRED IN ITERATION DENOTED BY L
C L=1 DENOTES TUP=TMAX1 FOR FREESTREAM CONDITIONS
C L=2 DENOTES TUP=TMAX2 FOR STATIC CONDITIONS BEHIND SHOCK

C IF TMAX1=0, THEN TUP=8000 DEG K
C IF TMAX2=0, THEN TUP=16,000 DEG K

C DIMENSION TABT(3), TABR(3), TABH(3), TABSR(3), TABAM(3), TABZM(3),
1 TABG(3), TABXM(3,30), TABXMO(80), TABFIT(30)
C DIMENSION TABPM(3), TABHM(3), TABSRM(3), TABTM(3), TABAMM(3), TABZ
1MM(3), TABGM(3)

```

```

21 DIMENSION XMOLE(30), SPECIE(30)
22 COMMON /BLK4/ NUMSP,JINDX,IAR,IN2,I02,ICO2,BOZ,XAR,XN2,XO2,XCO2
23 COMMON /BLK5/ TMAX1,TMAX2,TMIN1,TMIN2,XMOLE,SPECIE
24 COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
25 REAL MU
26 NN=C
27 IF (K.NE.4) GO TO 10
28 II=0
29 MN=0
30 PLOW=.01*RHO*ABS(H)
31 PPP=PLOW
32 PUP=.51*RHO*ABS(H)
33 P=(PUP-PLOW)/2.+PLOW
34 DELP=(PUP-PLOW)/2.
35 IF (MN.EQ.0) GO TO 2
36 P=PUP-DELP
37 PN=P/1.01325E+5
38 TLOW=0.
39 IF (L.EQ.1) GO TO 3
40 TUP=1.6E+4
41 GO TO 4
42 TUP=R.E+3
43 MN=MN+1
44 NN=0
45 GO TO 16
46 IF (ABS(1.-H/HK).LE..001) GO TO 41
47 IF (HK.LT.H) GO TO 6
48 PUP=D
49 PLOW=P-P-DELP
50 IF (NHELP.GT.PPP) GO TO 1
51 TABPM(1)=PUP
52 TABPM(3)=PLOW
53 NNN=-2
54 GO TO 7
55 PLOW=P
56 PUP=D+DELP
57 IF (NHELP.GT.PPP) GO TO 1
58 TABPM(1)=PLOW
59 TABPM(3)=PUP
60 NNN=2
61 TABHM(1)=HK
62 TABSRM(1)=SR
63 TABTM(1)=T
64 TABAMM(1)=AM

```

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65 TABZMM(1)=ZM
66 TABGM(1)=GAME
67 DELP=(TABPM(3)-TABPM(1))/2.
68 TABPM(2)=TABPM(1)+DELP
69 DO 9 JK=2,3
70 P=TABPM(JK)
71 I1=1
72 GO TO 2
73
74 TABHM(JK)=HK
75 TABSRM(JK)=SR
76 TABTM(JK)=T
77 TABAMM(JK)=AM
78 TABZMM(JK)=ZM
79 TABGM(JK)=GAME
80 CONTINUE
81 CALL FTLUP (H,SR,NNN,3,TABHM,TABSRM)
82 CALL FTLUP (H,AM,NNN,3,TABHM,TABAMM)
83 CALL FTLUP (H,ZM,NNN,3,TABHM,TABZMM)
84 CALL FTLUP (H,T,NNN,3,TABHM,TABTM)
85 CALL FTLUP (H,P,NNN,3,TABHM,TABPM)
86 CALL FTLUP (H,GAME,NNN,3,TABHM,TABGM)
87 GO TO 41
88
89 PN=P/1.01325E+5
90 IF (L.EQ.2) GO TO 12
91 IF (TMAX1.EQ.0.) GO TO 11
92 TUP=TMAX1
93 GO TO 14
94 TUP=R.E+3
95 GO TO 14
96 IF (TMAX2.EQ.0.) GO TO 13
97 TUP=TMAX2
98 GO TO 14
99 TUP=1.6E+4
100 IF (L.EQ.2) GO TO 15
101 TLOW=TMINI
102 GO TO 16
103 TLOW=TMINI2
104 T=(TUP-TLOW)/2.+TLOW
105 DELT=(TUP-TLOW)/2.
106 IF (NN.EQ.0) GO TO 18
107 T=TUP-DELT
108 CALL ROGO (PN,RHOA,HA,SAR,T,AM,ZM,GAME,MU)
109 NN=NN+1
110 IF (K.EQ.2) GO TO 23

```

```

C      IF (K.EQ.3) GO TO 24
C      CONVERGENCE TEST FOR K=1
C
19     IF (ABS(1.-RHO/RHOA).LE..001) GO TO 36
      IF (RHO.LT.RHOA) GO TO 21
      TUP=T
      TLOW=T-DELT
      IF (DELT.GT.250.) GO TO 17
      TABT(1)=TUP
      TABT(3)=TLOW
      IF (K.EQ.1.OR.K.EQ.4) GO TO 20
      N=-2
      GO TO 25
20     N=2
      GO TO 25
21     TLOW=T
      TUP=T+DELT
      IF (DELT.GT.250.) GO TO 17
      TABT(1)=TLOW
      TABT(3)=TUP
      IF (K.EQ.1.OR.K.EQ.4) GO TO 22
      N=2
      GO TO 25
22     N=-2
      GO TO 25
C      CONVERGENCE TEST FOR K=2
C
23     IF (ABS(1.-H/HA).LE..001) GO TO 37
      IF (HA.LT.H) GO TO 21
      GO TO 19
C      CONVERGENCE TEST FOR K=3
C
24     IF (ABS(1.-SR/SAR).LE..0001) GO TO 38
      IF (SAR.LT.SR) GO TO 21
      GO TO 19
C      INTERPOLATION FOR DELT LESS THAN 250 DEG K
C
25     TABR(1)=RHOA
      TABH(1)=HA
      TABSR(1)=SAR

```

```

TABAM(1)=AM
TABZM(1)=ZM
TABG(1)=GAME
DO 26 J=1,NUMSP
  TABXM(1,J)=XMOLE(J)
CONTINUE
26 DELT=(TABT(3)-TABT(1))/2.
  TABT(2)=TABT(1)+DELT
  DO 28 I=2,3
    T=TABT(I)
    CALL ROGO (PN,RHOA,HA,SAR,T,AM,ZM,GAME,MU)
    DO 27 J=1,NUMSP
      TABXM(I,J)=XMOLE(J)
CONTINUE
27 CONTINUE
  TABR(1)=RHOA
  TABH(1)=HA
  TABSR(1)=SAR
  TABAM(1)=AM
  TABZM(1)=ZM
  TABG(1)=GAME
CONTINUE
28 IJK=0
  DO 29 I=1,3
    DO 29 J=1,NUMSP
      IJK=IJK+1
      TABXMO(IJK)=TABXM(I,J)
CONTINUE
29 DO 30 J=1,NUMSP
  TABFIT(J)=J
CONTINUE
30 IY=3*NUMSP
  IF (K.EQ.2) GO TO 32
  IF (K.EQ.3) GO TO 34
  CALL FTLUP (RHO,T,N,3,TABR,TABT)
  CALL FTLUP (RHO,HK,N,3,TABR,TABH)
  CALL FTLUP (RHO,SR,N,3,TABR,TABSR)
  CALL FTLUP (RHO,AM,N,3,TABR,TABAM)
  CALL FTLUP (RHO,ZM,N,3,TABR,TABZM)
  CALL FTLUP (RHO,GAME,N,3,TABR,TABG)
  DO 31 JJ=1,NUMSP
    FIT=JJ
  CALL DISCOT (FIT,RHO,TABFIT,TABXMO,TABR,02,IY,3,XMOLE(JJ))
CONTINUE
31 IF (K.EQ.1) GO TO 40

```

L 153  
 L 154  
 L 155  
 L 156  
 L 157  
 L 158  
 L 159  
 L 160  
 L 161  
 L 162  
 L 163  
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 L 190  
 L 191  
 L 192  
 L 193  
 L 194  
 L 195  
 L 196



# APPENDIX C - Continued

32	IF (I1.EQ.1) GO TO 8	L 197
	GO TO 5	L 198
	CALL FTLUP (H,T,N,3,TABH,TABT)	L 199
	CALL FTLUP (H,RHO,N,3,TABH,TABR)	L 200
	CALL FTLUP (H,SR,N,3,TABH,TABSR)	L 201
	CALL FTLUP (H,AM,N,3,TABH,TABAM)	L 202
	CALL FTLUP (H,ZM,N,3,TABH,TABZM)	L 203
	CALL FTLUP (H,GAME,N,3,TABH,TABG)	L 204
	DO 33 JJ=1,NUMSP	L 205
	FIT=JJ	L 206
	CALL DISCOT (FIT,H,TABFIT,TABXMO,TABH,02,IY,3,XMOLE(JJ))	L 207
33	CONTINUE	L 208
	GO TO 41	L 209
34	CALL FTLUP (SR,RHO,N,3,TABSR,TABR)	L 210
	CALL FTLUP (SR,H,N,3,TABSR,TABH)	L 211
	CALL FTLUP (SR,T,N,3,TABSR,TABT)	L 212
	CALL FTLUP (SR,AM,N,3,TABSR,TABAM)	L 213
	CALL FTLUP (SR,ZM,N,3,TABSR,TABZM)	L 214
	CALL FTLUP (SR,GAME,N,3,TABSR,TABG)	L 215
	DO 35 JJ=1,NUMSP	L 216
	FIT=JJ	L 217
	CALL DISCOT (FIT,SR,TABFIT,TABXMO,TABSR,02,IY,3,XMOLE(JJ))	L 218
35	CONTINUE	L 219
	GO TO 41	L 220
36	IF (K.EQ.4) GO TO 39	L 221
	H=HA	L 222
	SR=SR	L 223
	GO TO 41	L 224
37	RHO=RHOA	L 225
	SR=SR	L 226
	GO TO 41	L 227
38	H=HA	L 228
	RHO=RHOA	L 229
	GO TO 41	L 230
39	HK=HA	L 231
	SR=SR	L 232
	GO TO 5	L 233
40	H=HK	L 234
41	RETURN	L 235
	END	L 236-
	SUBROUTINE ROGO (PN,RHOAN,HA,SOR,T,AM,XZ,GAMMAE,MU)	M 1
C		M 2
C	PROGRAM OF ALLISON(NASA TN D-3538) AND NEWMAN(NASA TN D-3540)	M 3
C	COMPUTES THERMOCHEMICAL EQUILIBRIUM PROPERTIES OF GAS MIXTURES	M 4

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C
C
C      REQUIRES INPUTS OF P AND T
COMMON /BLK4/ NUMSP,JINDX,IAR,IN2,I02,I02,BOZ,XAR,XN2,X02,XC02
COMMON /BLK5/ TMAX1,TMAX2,TMIN1,TMIN2,XMOLE,SPECIE
COMMON /BLK6/ IHE,IH2,IH,XHE,XH2
REAL NO,M,LAMB,LAMBDA,MU,NE,NEGFRT,LOGNE,MASSFR,LMIN
REAL INTENE,LGEORT,LGRORE
INTEGER F(30),V(30,I0)
DIMENSION LB(30), M(30), DELHF(30), BETA(30), NDEB(30), IPIVOT(1
10), R(10,10), SUMAY(10,1), G(30,30), E(30,30), BE(30,10), ALPHAE(3
20,10), OMEGA(30,10), OMEGAX(30,10), XOMEG(30,4), XOMEGX(30,4), Z(3
30), SIGMA(10), U(10), DELTA(10), GAMMA(10), XX(10), Q(30), Y(30),
4X(30), A(30,9), HORT(30), FORT(30), NEGFRT(30), PI(9,2), XPRIME(30
5), MASSFR(30), CAPX(50), YINT(30,5), CSUBP(30), PSI(30,2), CON(10,
62), DXDT(30), RR(10,10), O(10,10)
DIMENSION HEPG(30), DMSFRDT(30)
DIMENSION XMOLE(30), SPECIE(30)
H=6.62517E-27
XK=1.38044E-16
PREF=1.013250E+6
NO=6.02322E+23
C=2.99793E+10
IF (ROZ.EQ.1.) GO TO 3
BOZ=1.
EA=1.E-8
ER=1.E-1
DO 2 I=1,NUMSP
READ (5,76) SPECIE(I),LB(I),F(I),NDEB(1),M(I),DELHF(I),BETA(I)
IL=LR(I)
IF NDEB(1) EQUALS 0, NDEB
READ (5,77) (G(I,L),F(I,L),L=1,IL)
IF (F(I).EQ.0) GO TO 2
IF (F(I).EQ.2) GO TO 1
READ (5,78) (BE(I,L),ALPHAE(I,L),OMEGA(I,L),OMEGAX(I,L),V(I,L),L=1
1,IL)
GO TO 2
1 READ (5,77) BE(I,1),ALPHAE(I,1)
READ (5,77) (XOMEG(I,LW),XOMEGX(I,LW),LW=1,4)
CONTINUE
2 READ (5,79) ((A(I,J),J=1,JINDX),I=1,NUMSP)
DO 4 I=1,NUMSP
3 YINT(I,1)=1.E-20
4 YINT(I02,1)=1.E-5
IF (XAR.EQ.0.) GO TO 5

```

# APPENDIX C - Continued

5	YINT(IAR,1)=XAR/MU	M 49
	IF (XN2.EQ.0.) GO TO 6	M 50
	YINT(IN2,1)=XN2/MU	M 51
6	IF (X02.EQ.0.) GO TO 7	M 52
	YINT(I02,1)=X02/MU	M 53
7	IF (XC02.EQ.0.) GO TO 8	M 54
	YINT(IC02,1)=XC02/MU	M 55
8	IF (XHE.EQ.0.) GO TO 9	M 56
	YINT(IHE,1)=XHE/MU	M 57
9	IF (XH2.EQ.0.) GO TO 10	M 58
	YINT(IH2,1)=XH2/MU	M 59
10	RH00=PREF*MU/(NO*XK*273.15)	M 60
	DO 11 I=1,NUMSP	M 61
11	IF (YINT(I,1).EQ.0.) YINT(I,1)=1.E-20	M 62
	AO=SQRT(1.4*(PREF/RH00))	M 63
	NUMT=NCAPX=1	M 64
	LEEB0B=INDEF=0	M 65
	IF (INDEF.NE.0) GO TO 13	M 66
	DO 12 KP=1,NCAPX	M 67
12	CAPX(KP)=ALOG10(PN)	M 68
13	DO 75 KI=1,NUMT	M 69
	IF (LEEB0B.EQ.1) PUNCH 83, T	M 70
	NY=1	M 71
	PART=H*C/(XK*T)	M 72
	DO 21 I=1,NUMSP	M 73
	IL=LR(I)	M 74
	IF (F(I).EQ.1) GO TO 15	M 75
	IF (F(I).EQ.2) GO TO 18	M 76
	QSUM=0.	M 77
	FPOSUM=0.	M 78
	SPOSUM=0.	M 79
	DO 14 L=1,IL	M 80
	Z(L)=PART*E(1,L)	M 81
	GEZ=G(1,L)*EXP(-Z(L))	M 82
	QSUM=QSUM+GEZ	M 83
	FPOSUM=FPOSUM+GEZ*Z(L)	M 84
14	SPOSUM=SPOSUM+(Z(L)-2.)*GEZ*Z(L)	M 85
	FPOSUM=FPOSUM/T	M 86
	SPOSUM=SPOSUM/T**2	M 87
	QI=(M(1)*T*.32807618)**1.5*QSUM*.13623883*T	M 88
	GO TO 20	M 89
15	QSUM=0.	M 90
	FPOSUM=0.	M 91
	SPOSUM=0.	M 92

```

93 DO 17 L=1,IL
94 Z(L)=PART*(I,L)
95 SIGMA(L)=PART*(BE(I,L)-.5*ALPHA(I,L))
96 U(L)=PART*(OMEGA(I,L)-2.*OMEGAX(I,L))
97 DELTA(L)=ALPHA(I,L)*1./(BE(I,L)-.5*ALPHA(I,L))
98 GAMMA(L)=(BE(I,L)/OMEGA(I,L))*2*1./(1.-.5*ALPHA(I,L)/BE(I,L))
99 XX(L)=OMEGAX(I,L)/(OMEGA(I,L)-2.*OMEGAX(I,L))
100 THREE=0.
101 FOUR=0.
102 FIVE=0.
103 NV=V(I,L)+1
104 DO 16 IV=1,NV
105 W=IV-1
106 CC=(1.-W*DELTA(L))
107 AA=SIGMA(L)*CC
108 BB=U(L)*(W-XX(L)*W*(W-1.))
109 ONE1=1./AA+8.*GAMMA(L)/(AA**2*CC)+.33333333+AA/12.
110 TWO2=1./AA+16.*GAMMA(L)/(AA**2*CC)-AA/12.-384.*GAMMA(L)**2/(AA**3*
111 1CC**2)
112 THREE=THREE+ONE1*EXP(-BB)
113 FOUR=FOUR+(BB*ONE1+TWO2)*EXP(-BB)
114 FIVE=FIVE+((BB**2*ONE1+2.*BB*TWO2+GAMMA(L)/(AA**2*CC))*(48.-3456.*G
115 1AMMA(L)/(AA*CC)+46080.*GAMMA(L)**2/(AA**2*CC**2))+2./AA)*EXP(-BB))
116 GEZ=G(I,L)*EXP(-Z(L))
117 Q(L)=THREE/BETA(I)*GFZ
118 QSUM=QSUM+Q(L)
119 FPQSUM=FPQSUM+(FOUR+THREE*Z(L))*GEZ
120 SPOSUM=SPOSUM+(Z(L)*(Z(L)-2.)*THREE+2.)*(Z(L)-1.)*FOUR+FIVE)*GEZ
121 FPOSUM=FPOSUM/(T*BETA(I))
122 SPOSUM=SPOSUM/(T**2*BETA(I))
123 QI=(M(I)*T*.32807618)**1.5*QSUM*.13623883*T
124 GO TO 20
125 SIGMA(I)=PART*(BE(I,1)-.5*ALPHA(I,1))
126 PROD=1.
127 SUM1=0.
128 SUM2=0.
129 DO 19 LW=1,4
130 U(LW)=PART*(XOMEG(I,LW)-XOMEGX(I,LW))
131 PROD=PROD*(1.-EXP(-U(LW)))
132 BTM=EXP(U(LW))-1.
133 SUM1=SUM1+U(LW)/BTM
134 SUM2=SUM2+U(LW)**2*EXP(U(LW))/BTM**2
135 QSUM=G(I,1)/(BETA(I)*SIGMA(I)*PROD)
136 FPOSUM=(1.+SUM1)*QSUM/T

```

# APPENDIX C - Continued

```

20      SPQSUM=(SUM1**2+SUM2)*QSUM/T**2
        Q1=(M(1)*T*.32807618)**1.5*QSUM*.13623883*T
        HORT(1)=2.5+T/QSUM*FPQSUM+DELHF(1)/(NO*XK*T)
        HEPG(1)=HORT(1)*NO*XK*T/M(1)
        FORT(1)=DELHF(1)/(NO*XK*T)-ALOG(Q1)
21      NEGFT(1)=-FORT(1)
        CSUBP(1)=2.5+2.*T/QSUM*FPQSUM-(T*FPQSUM/QSUM)**2+T**2*SPQSUM/QSUM
        IF (LEEB0B.EQ.1) PUNCH 83, (CSUBP(1),HORT(1),I=1,NUMSP)
        NNN=1
        DO 74 KP=1,NCAPX
          IF (INDEP.EQ.2) SAVERHO=CAPX(KP)
          P=(10.**CAPX(KP))*PREF
          POPO=P/PREF
        DO 22 I=1,NUMSP
22      Y(I)=YINT(I,NY)
          NUMIT=0
          NUMITF=0
          MM=JINDX+1
          DO 24 J=1,JINDX
            O(J,MM)=0.
            DO 23 I=1,NUMSP
23      O(J,MM)=O(J,MM)+A(I,J)*Y(I)
            O(MM,J)=O(J,MM)
            CONTINUE
24      O(MM,MM)=0.
            CONTINUE
25      YBAR=Y(1)
          NUMIT=NUMIT+1
          IF (NUMIT.EQ.201) GO TO 61
          DO 26 I=2,NUMSP
            YBAR=YBAR+Y(I)
26      IF (INDEP.EQ.2) P=NO*XK*T*YBAR*CAPX(KP)
            DO 28 K=1,JINDX
              R(1,K)=0.
              DO 27 I=1,NUMSP
27      R(1,K)=R(1,K)+A(I,1)*A(I,K)*Y(I)
              CONTINUE
              ICOUNT=1
              JJ=2
              DO 32 J=JJ,JINDX
                DO 30 K=J,JINDX
                  R(J,K)=0.
28      DO 29 I=1,NUMSP
                  R(J,K)=R(J,K)+A(I,J)*A(I,K)*Y(I)
29

```

# APPENDIX C - Continued

30	CONTINUE	M 181
	DO 31 K=1,ICOUNT	M 182
31	R(J,K)=R(K,J)	M 183
	ICOUNT=ICOUNT+1	M 184
32	JJ=1+ICOUNT	M 185
	DO 33 J=1,MM	M 186
	R(J,MM)=O(J,MM)	M 187
33	R(MM,J)=O(J,MM)	M 188
	DO 34 J=1,MM	M 189
	DO 34 K=1,MM	M 190
34	RR(J,K)=R(J,K)	M 191
	PYBAR=PREF*YBAR	M 192
	DO 36 J=1,JINDX	M 193
	SUMAY(J,1)=0.	M 194
	DO 35 I=1,NUMSP	M 195
	THIS=P*Y(I)/PYBAR	M 196
	IF (THIS.LE.0.) GO TO 35	M 197
	SUMAY(J,1)=SUMAY(J,1)+A(I,J)*Y(I)*(FORT(I)+ALOG(THIS))	M 198
35	CONTINUE	M 199
36	CONTINUE	M 200
	SUMAY(MM,1)=0.	M 201
	DO 37 I=1,NUMSP	M 202
	THIS=P*Y(I)/PYBAR	M 203
	IF (THIS.LE.0.) GO TO 37	M 204
	SUMAY(MM,1)=SUMAY(MM,1)+Y(I)*(FORT(I)+ALOG(THIS))	M 205
37	CONTINUE	M 206
	MN=1	M 207
	NMAX=10	M 208
	CALL SIMEQ (R,MM,SUMAY,MN,DETERM,PIPOT,NMAX,ISCALE)	M 209
	DO 38 J=1,JINDX	M 210
38	PI(J,1)=SUMAY(J,1)	M 211
	U=SUMAY(MM,1)	M 212
	LMIN=1.	M 213
	LCOUNT=0	M 214
	DO 45 I=1,NUMSP	M 215
	API=0.	M 216
	DO 39 J=1,JINDX	M 217
39	API=API+A(I,J)*PI(J,1)	M 218
	THIS=P*Y(I)/PYBAR	M 219
	IF (THIS.LE.0.) GO TO 40	M 220
	X(I)=Y(I)*(NEGRT(I)-ALOG(THIS))+U+1.+API)	M 221
	GO TO 41	M 222
40	X(I)=0.	M 223
41	IF (X(I)) 42,44,45	M 224

# APPENDIX C - Continued

```

42  LAMB=-Y(I)/(X(I)-Y(I))
    IF (LAMB.GT.0.) GO TO 43
    Y(I)=0.
    GO TO 25
43  LCOUNT=1
    LMIN=AMINI(LMIN,LAMB)
    GO TO 45
44  IF (Y(I).EQ.0.) GO TO 45
    LCOUNT=1
    LAMB=1.
    LMIN=AMINI(LMIN,LAMB)
45  CONTINUE
    IF (LCOUNT.EQ.0) GO TO 47
    LAMBDA=.9999999999999999*LMIN
    DO 46 I=1,NUMSP
    Y(I)=(1.-LAMBDA)*Y(I)+LAMBDA*X(I)
    IF (Y(I).LT.1.E-100) Y(I)=0.
    GO TO 25
46  DO 48 I=1,NUMSP
    IF (Y(I).EQ.0.) GO TO 48
    IF (ABS(X(I)-Y(I))/Y(I).GE.ER.OR.ABS(X(I)-Y(I)).GE.EA) GO TO 49
    CONTINUE
    GO TO 56
47  XBAR=0.
    LAMBDA=1.
    LASTCT=0
48  DO 51 I=1,NUMSP
    XPRIME(I)=(1.-LAMBDA)*Y(I)+LAMBDA*X(I)
    XBAR=XBAR+XPRIME(I)
    DFLAMB=0.
    DO 52 I=1,NUMSP
    THIS=P*XPRIME(I)/(PRFF*XBAR)
    IF (THIS.LE.1.E-38) GO TO 52
    DFLAMB=DFLAMB+(X(I)-Y(I))*(FORT(I)+ALOG(THIS))
    CONTINUE
    IF (DFLAMB.GT.0.) GO TO 55
49  DO 54 I=1,NUMSP
    Y(I)=XPRIME(I)
    GO TO 25
50  LASTCT=LASTCT+1
    IF (LASTCT.EQ.4) GO TO 53
    LAMBDA=.9*LAMBDA
    XBAR=0.
    GO TO 50
51
52
53
54
55

```

# APPENDIX C - Continued

```

56 IF (NUMITF.EQ.1) GO TO 58
   NUMITO=0
   IF (INDEP.NE.2) GO TO 58
   NUMITF=1
   NUMITO=NUMIT
   INDEP=1
57 DO 57 I=1,NUMSP
   Y(I)=X(I)
   GO TO 25
58 XBAR=0.
   ONE=0.
   TWO=0.
   DO 59 I=1,NUMSP
   XBAR=XBAR+X(I)
   ONE=ONE+X(I)*HORT(I)
   MASSFR(I)=X(I)*M(I)
   IF (Y(I).EQ.0.) GO TO 59
   TWO=TWO+X(I)*(FORT(I)+ALOG(X(I)))
   CONTINUE
59 RECIPZ=1./(MU*XBAR)
   IF (NUMITF.EQ.1) CAPX(KP)=ALOG10(P/PREF)
   IF (NUMITF.EQ.1) INDFP=2
   CAPU=CAPX(KP)+ALOG10(RECIPZ*273.15/T)
   CHORT=MU*ONE
   SOR=CHORT-MU*(XBAR*ALOG(P/(PREF*XBAR)))+TWO
   RHO=P/(XBAR*NO*XK*T)
   NE=X(1)*RHO*NO
   IF (X(1).GT.10.**-20) GO TO 60
   LOGNF=-0.
   GO TO 62
60 LOGNF=ALOG10(NE)
   GO TO 62
61 WRITE (6,80) P
   GO TO 74
62 CONTINUE
   DO 64 I=1,NUMSP
   TEST=X(1)*P/(XBAR*PREF)
   IF (TEST.LT.10.**(-20)) GO TO 63
   PSI(1,1)=X(1)/T*(HORT(1)-FORT(1)-ALOG(TEST))
   PSI(1,2)=-X(I)
   GO TO 64
63 PSI(1,1)=0.
   PSI(1,2)=0.
64 CONTINUE

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# APPENDIX C - Continued

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M 313 DO 66 J=1,JINDX
M 314 CON(J,1)=A(1,J)*PSI(1,1)
M 315 CON(J,2)=A(1,J)*PSI(1,2)
M 316 DO 65 I=2,NUMSP
M 317 CON(J,1)=CON(J,1)+A(I,J)*PSI(I,1)
M 318 CON(J,2)=CON(J,2)+A(I,J)*PSI(I,2)
M 319 CONTINUE
M 320 CON(MM,1)=PSI(1,1)
M 321 CON(MM,2)=PSI(1,2)
M 322 DO 67 I=2,NUMSP
M 323 CON(MM,1)=CON(MM,1)+PSI(I,1)
M 324 CON(MM,2)=CON(MM,2)+PSI(I,2)
M 325 NC=2
M 326 CALL SIMEQ (RR,MM,CON,NC,DETERM,IPIVOT,NMAX,ISCALE)
M 327 DO 68 J=1,MM
M 328 PI(J,1)=CON(J,1)
M 329 PI(J,2)=CON(J,2)
M 330 DHDT=0.
M 331 DO 70 I=1,NUMSP
M 332 SUMAP=A(I,1)*PI(1,1)
M 333 DO 69 J=2,JINDX
M 334 SUMAP=SUMAP+A(I,J)*PI(J,1)
M 335 DXDT(I)=PSI(1,1)-X(I)*PI(MM,1)+SUMAP
M 336 DMSFRDT(I)=M(I)*DXDT(I)
M 337 DHDT=DHDT+(X(I)*CSUBP(I)+T*HORT(I)*DXDT(I))
M 338 DRHDT=T*PI(MM,1)-1.
M 339 DRHODP=1.+PI(MM,2)
M 340 CPOR=MU*DHDT
M 341 XZ=XRAR*MU
M 342 CVOR=CPOR-DRHDT**2/DRHODP*XZ
M 343 XGAMMA=CPOR/CVOR
M 344 GAMMAE=XGAMMA/DRHODP
M 345 RHOR=1./(10.**CAPU)
M 346 HPGRAM=CHORT*NO*XK*T/MU
M 347 TEST=(GAMMAE/1.4*P/PREF*RHOR)
M 348 IF (TEST.LE.0.) WRITE (6,82) CAPX(KP),CAPU,XZ,CHORT,SOR,LOGNE,DRHO
M 349 1DT,DRHODP,CPOR,CVOR,XGAMMA,GAMMAE,AOAO
M 350 AOAO=SQRT(TEST)
M 351 AM=AOAO*AO*.01
M 352 RHODN=(10.**CAPU)*RHOO*1.E+3
M 353 HA=CHORT*8.31469E+3*T/MU
M 354 INTENE=((CHORT-XZ)*NO*XK*T+3.93146E+12)/MU
M 355 GAMBAR=(INTENE+(P/RHO))/INTENE
M 356 EORTO=INTENE*28.9672/(NO*XK*273.15)

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# APPENDIX C - Continued

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M 387
M 388-

LGEORT=ALOG10(EORTO)
RORHOE=RHO/1.29233666E-3
LGRORE=ALOG10(RORHOE)
DO 71 I=1,NUMSP
  XMOLE(I)=MASSFR(I)*MU/(XZ*M(I))
  IF (NNN.EQ.10) GO TO 72
  GO TO 73
71 WRITE (6,81)
  NNN=0
72 NNN=NNN+1
  IF (INDEP.EQ.2) CAPX(KP)=SAVERHO
  IF (LEEB08.EQ.0) GO TO 74
  IF (KP.EQ.1) PUNCH 84, NCAFX
  PUNCH 83, POPO,CPOR
  PUNCH 85, (XMOLE(I),I=1,NUMSP)
  CONTINUE
73 CONTINUE
  RETURN
C
C
74 FORMAT (A6,3I5,3E14.8)
75 FORMAT (5E14.8)
76 FORMAT (4E14.8,15)
77 FORMAT (15E5.0)
78 FORMAT (1X,2HP=E15.8,2X,28H200 ITERATIONS-NONCONVERGENT)
79 FORMAT (/)
80 FORMAT (/F9.4,F10.4,F9.4,F11.4,F10.4,F9.3,F10.3,F10.3,F10.3,
81 1F8.3,F8.3,F9.3)
82 FORMAT (2E16.8)
83 FORMAT (15)
84 FORMAT (5E16.8)
85 END

- ,
$INP T1=300,T4=600,P4=6,B948E+7,LB=2,LF=1,U5=12192,P1=3447.4,PMIX=1,
PHE=.5,PH2=.5,NUMSP=7,JINPX=3,IH=5,IH2=7,IHE=2,NDRIV=1$
E- 1 0 0 54847000-03 00000000+00 00000000+00
20000000+01 00000000+00
HE 8 0 0 40026000+01 00000000+00 00000000+00
10000000+01 00000000+00 30000000+01 15986700+06 13000000+02
16909900+06 36000000+02 18571700+06 64000000+02 19137100+06
64000000+02 19388800+06 64000000+02 19524900+06 64000000+02
19606900+06
HE+ 7 0 0 40026000+01 23719600+14 00000000+00
20000000+01 00000000+00 80000000+01 32938100+06 14000000+02

```

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38999400+06 22000000+02 41152100+06 32000000+02 42161000+06
44000000+02 42676200+06 58000000+02 42999600+06
HE++ 1 0 0 40026000+01 76216100+14 00000000+00
10000000+01 00000000+00
H 1 0 0 10080000+01 21602828+13 00000000+00
10000000+01 00000000+00
H+ 1 0 0 10080000+01 15211700+14 00000000+00
10000000+00 00000000+00
H2 1 1 0 20160000+01 00000000+00 20000000+01
10000000+01 00000000+00
60800000+02 29930000+01 43953000+04 11790000+03 5
1 0 0 0 1 0 -1 1 0 -2 1 0 0 0 1
-1 0 1 0 0 2
$INP T1=300,T4=600,P4=6.8948E+7,LB=2,LF=1,US=12192,P1=3447.4,PMIX=1,
PHE=.2,PH2=.8,NUMSP=7,JINDEX=3,IH=5,IH2=7,IHE=2$
- ,

```

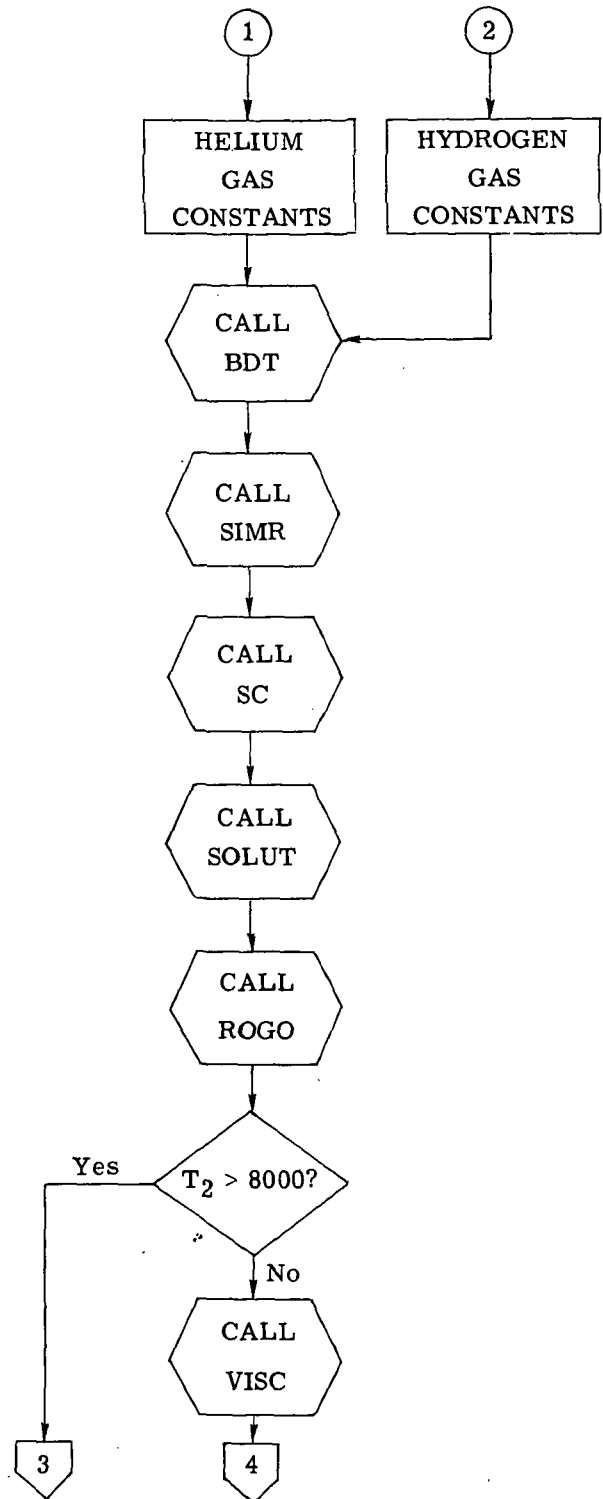
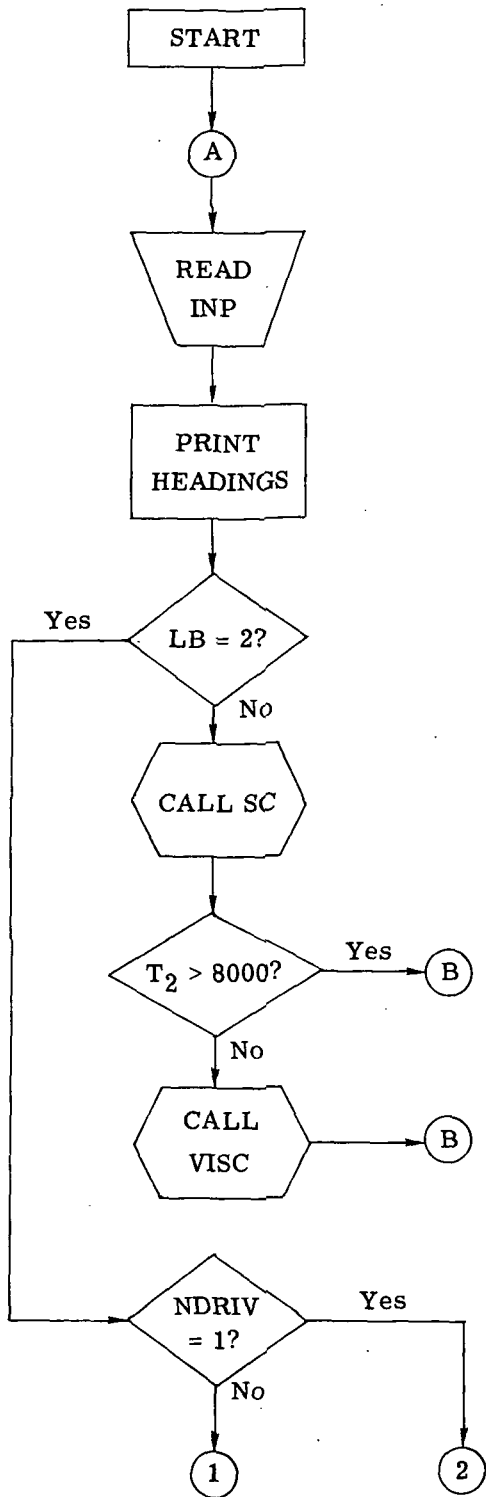
## APPENDIX C – Continued

The basic subroutines of this program are as follows:

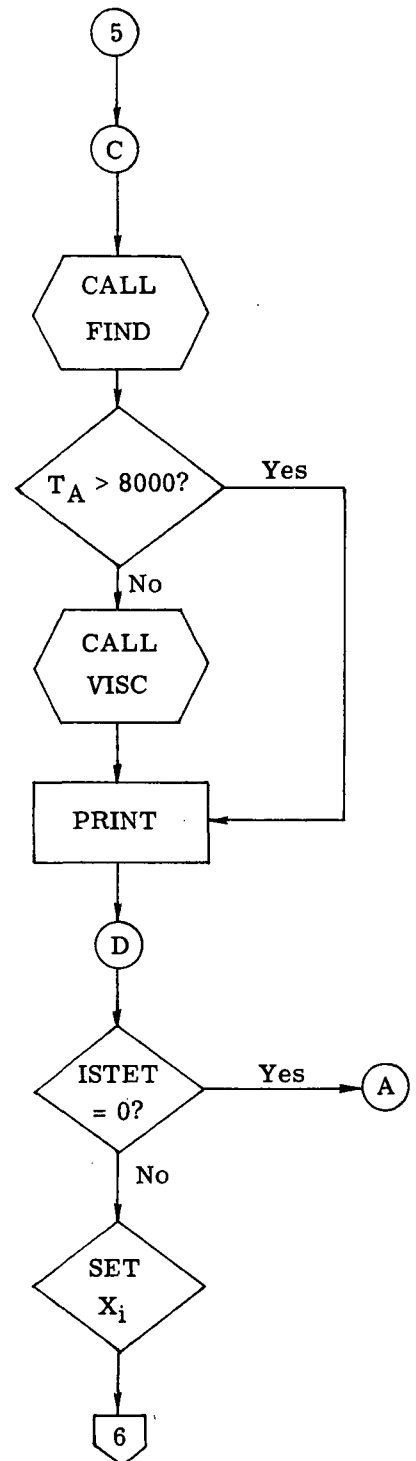
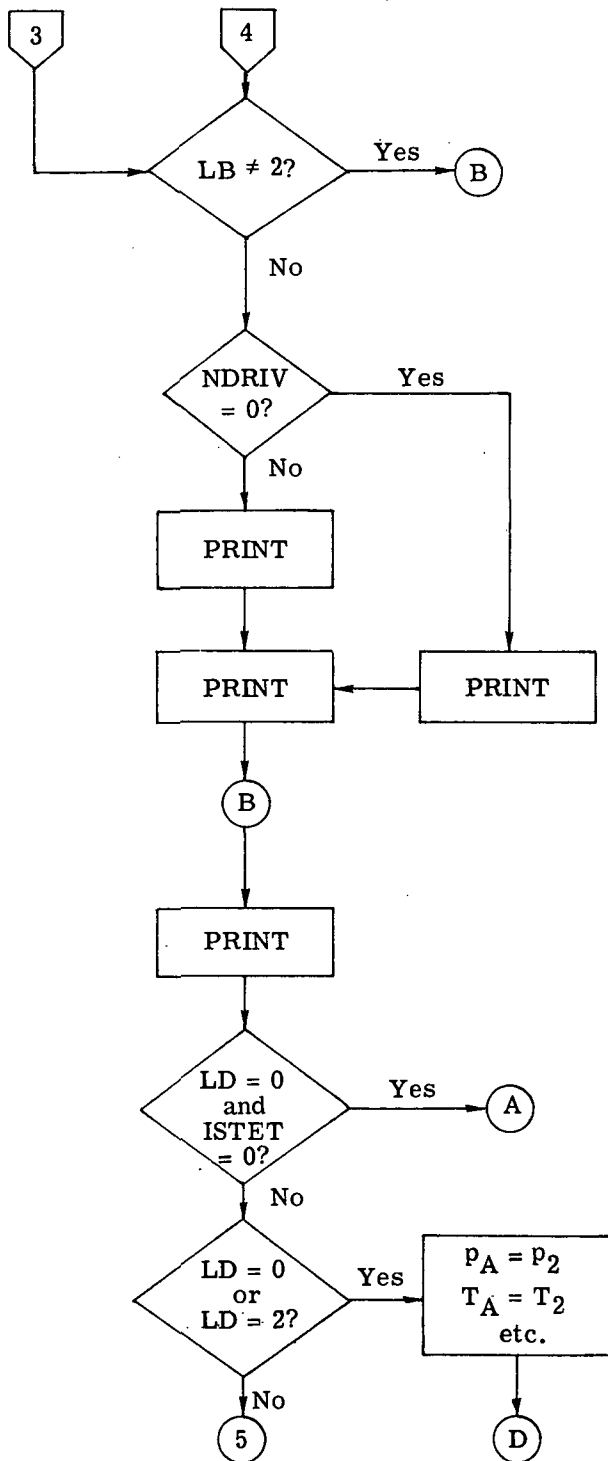
- (1) ROGO – computes thermodynamic quantities  $a$ ,  $h$ ,  $sW_0/R$ ,  $X_i$ ,  $Z^*$ ,  $\gamma_E$ , and  $\rho$  for given  $p$ ,  $T$ , and  $W_0$
- (2) FIND – iterative-interpolation procedure for obtaining thermodynamic quantities from ROGO with combinations:
  1.  $p$  and  $\rho$
  2.  $p$  and  $h$
  3.  $p$  and  $sW_0/R$
  4.  $h$  and  $\rho$
- (3) VISC – computes  $\mu$  for given  $T$  and  $X_i$
- (4) BDT – computes  $B$  and  $C$  for helium or hydrogen for given  $T$
- (5) SOLUT – given  $(p_2, U_2)$  and  $(p_3, U_3)$ , finds solution to curves
- (6) SC – iterative procedure for solving conservation relations for a moving normal shock
- (7) SNS – iterative procedure for solving conservation relations for a standing normal shock
- (8) SIMR – computes  $\int \left( \frac{dh}{a} \right)_{sW_0/R}$  by Simpson's rule

A flow chart of this program is given in the following pages.

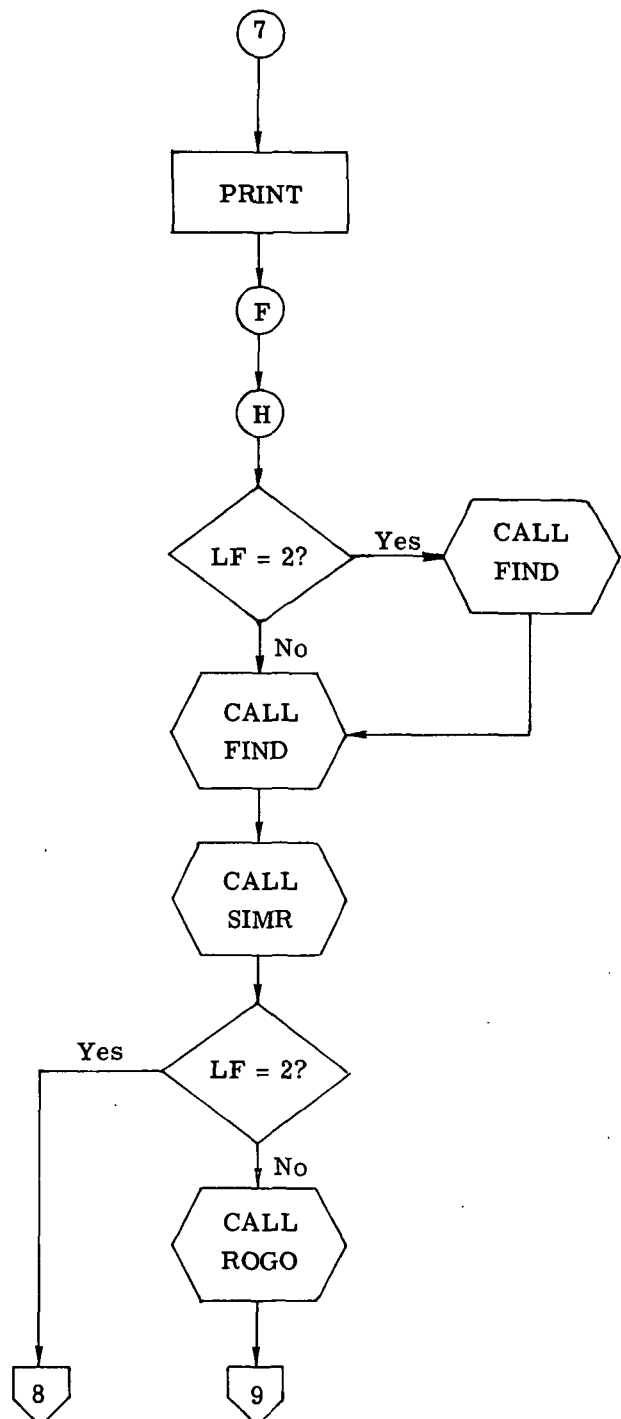
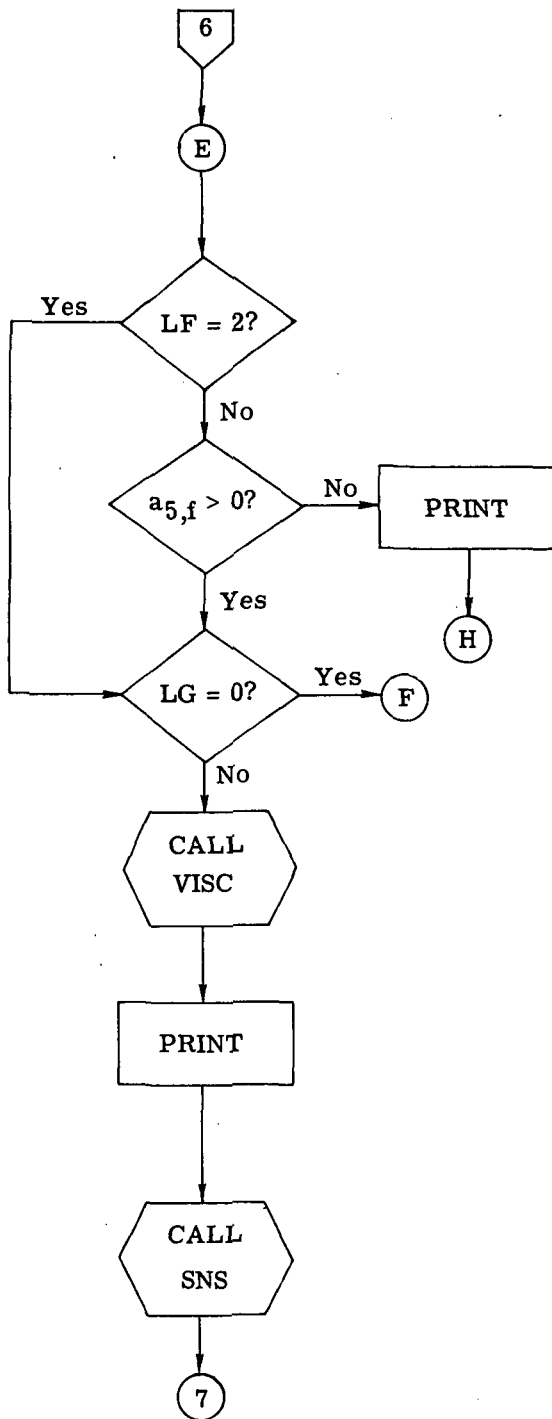
# APPENDIX C - Continued



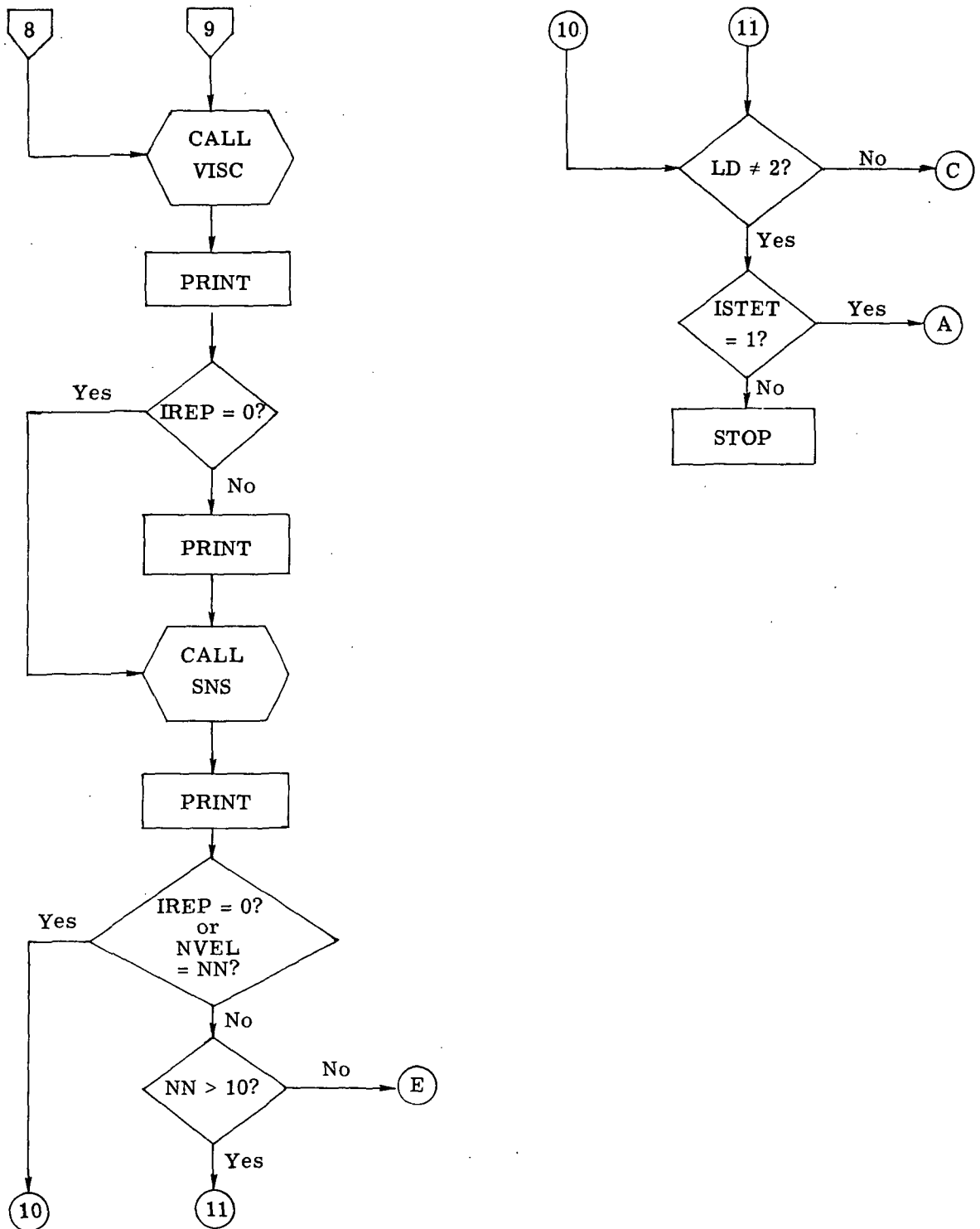
# APPENDIX C – Continued



# APPENDIX C -- Continued



# APPENDIX C - Continued





# APPENDIX C - Continued

The procedure for running a program with all 26 species for CO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, and Ar is discussed in detail in reference 18. Also, modifications required when the number of species is varied are illustrated by example in reference 18. For convenience, an additional example is now presented. A mixture of CO<sub>2</sub> and Ar, which may represent the Mars atmospheric model, is considered with second ionization neglected. Now, the number of atoms of a particular component per particle of a species A(I,J) must be designated. For electrons, a charge constraint is used instead of a mass constraint. Constructing a table of A(I,J) for this CO<sub>2</sub>-Ar mixture gives

		1	2	3	4
		1	2	3	4
Species (I)	Component (J)	e <sup>-</sup>	Ar	O	C
1	e <sup>-</sup>	1	0	0	0
2	Ar	0	1	0	0
3	Ar <sup>+</sup>	-1	1	0	0
4	O	0	0	1	0
5	O <sup>+</sup>	-1	0	1	0
6	O <sup>-</sup>	1	0	1	0
7	O <sub>2</sub>	0	0	2	0
8	O <sub>2</sub> <sup>+</sup>	-1	0	2	0
9	O <sub>2</sub> <sup>-</sup>	1	0	2	0
10	C	0	0	0	1
11	C <sup>+</sup>	-1	0	0	1
12	C <sup>-</sup>	1	0	0	1
13	CO	0	0	1	1
14	CO <sup>+</sup>	-1	0	1	1
15	CO <sub>2</sub>	0	0	2	1

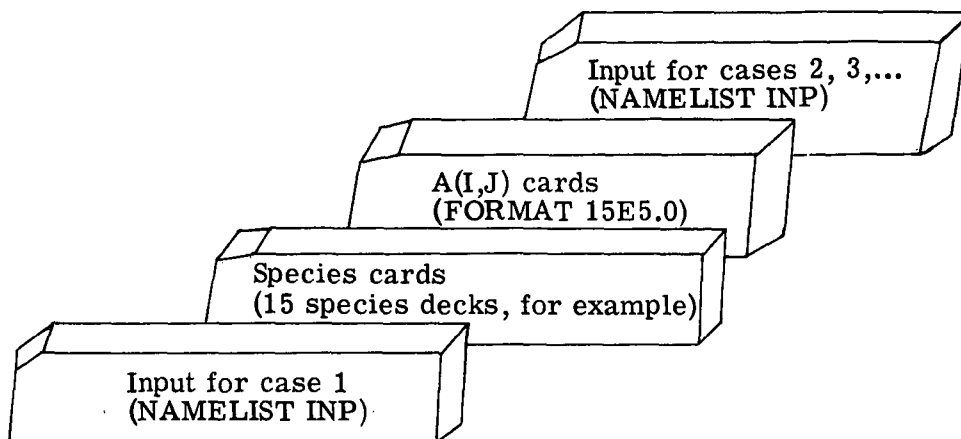
The sequence 0, 1, 0, 0 for species Ar denotes that the only component contained in this species is Ar. (A zero denotes that a particular component does not appear in that species.) In the sequence -1, 1, 0, 0 for Ar<sup>+</sup>, the -1 denotes that Ar<sup>+</sup> is a positive ion, and so forth. For this mixture, NUMSP = 15, JINDX = 4, IAR = 2, IC = 10, ICØ = 13, ICØ2 = 15, IØ = 4, and IØ2 = 7.

Only the species decks for the 15 species considered are included, and these are placed in the order that they appear in the A(I,J) table. The A(I,J) are read in as illustrated by the following listing:

1	0	0	0	0	1	0	0	-1	1	0	0	0	0	1
0	-1	0	1	0	1	0	1	0	0	0	2	0	-1	0
2	0	1	0	2	0	0	0	0	1	-1	0	0	1	1
0	0	1	0	0	1	1	-1	0	1	1	0	0	2	1

## APPENDIX C – Continued

The first four numbers represent the  $A(I,J)$  sequence, from the  $A(I,J)$  table, for  $e^-$ ; the next four numbers represent the  $A(I,J)$  sequence for  $Ar$ ; and so forth. The sequence of cards following the main program and subroutine is as follows:



Sample data printouts are included that illustrate program usage for hypothetical tests in an expansion tube with a Mars model atmosphere at moderate velocity and with Venus and Jovian model atmospheres at high velocity.

The headings for the various flow regions correspond to those in the section entitled "SYMBOLS." The units of these flow quantities are as given in the definitions of the symbols, except where explicitly specified in the printout. The sample printouts are as follows:

02/15/72

MARS

EXPANSION TUBE PROGRAM OF MILLER FOR GAS MIXTURES  
ALL PHYSICAL QUANTITIES IN MKS UNITS- NASA SP-7012

SHOCK TUBE PHASE OF PROGRAM

MEASURED INPUTS FOR SHOCK TUBE PHASE

RUN	P1	T1	US1	P2	P4	T4
1.000E+00	3.447E+03	3.000E+02	0.	0.	3.447E+07	3.000E+02

WO	XC02	XN2	XO2	XAR	XHE	XF2
4.340E+01	8.500E-01	0.	0.	1.500E-01	0.	0.

1 CONDITIONS - QUIESCENT TEST GAS

P	RHO	T	H	GAM	A
3.447E+03	5.958E-02	3.000E+02	7.458E+06	1.313E+00	2.746E+02

IMPERFECT HELIUM DRIVER GAS

4 CONDITIONS

P	PHG	T	H	S/R	Z	A	W
3.447E+07	4.758E+01	3.000E+02	1.665E+06	9.261E+00	1.153E+00	1.160E+03	4.003E+00

2 CONDITIONS- REAL GAS MIXTURES

P	PHG	T	H	S/R	Z	GAME	A	U	M	NRE
2.518E+05	5.907E-01	2.195E+03	5.178E+06	3.566E+01	1.014E+00	1.134E+00	6.953E+02	1.928E+03	2.774E+00	1.620E+07

RATIO- 2 CONDITIONS TO 1 CONDITIONS

P	PHG	T	H	PSI	US1
7.303E+01	9.847E+00	7.316E+00	6.942E-01	7.815E+00	2.146E+03

## MOLE FRACTIONS IN REGION 2

MARS

## SPECIE MOLE FRACTION

A 1.4797E-01  
 O 1.9085E-04  
 O2 1.3354E-02  
 C 1.2842E-17  
 CO 2.6043E-02  
 CO2 8.1244E-01

## CONDITIONS BEHIND STANDING SHOCK

P RHC T H S/R Z GAME A U M NRE  
 2.065E+06 3.385E+00 2.943E+03 3.375E+06 3.711E+01 1.082E+00 1.120E+00 8.266E+02 3.366E+02 4.072E-01 1.303E+07

## MOLE FRACTIONS BEHIND SHOCK AT SECOND CIA.

## SPECIE MOLE FRACTION

A 1.3862E-01  
 O 5.4200E-03  
 O2 7.0475E-02  
 C 1.3032E-12  
 CO 1.4557E-01  
 CO2 6.3992E-01

## 5 CONDITIONS FOR FROZEN EXPANSION

P RHC T H S/R Z GAME A U M NRE  
 5.174E-05 3.815E-08 6.542E+00 8.249E+02 3.711E+01 1.082E+00 1.334E+00 4.253E+01 5.486E+03 1.290E+02 6.520E+02

 STATIC(55) CONDITIONS BEHIND NORMAL SHOCK  
 FROZEN EXPANSION--EQUILIBRIUM POST SHOCK

P RHC T H S/R Z GAME A U M R5S/R5  
 1.074E+00 5.919E-07 4.413E+03 1.531E+07 8.771E+01 2.147E+00 1.079E+00 1.399E+03 3.537E+02 2.528E-01 1.551E+01

 STAGNATION(15) CONDITIONS BEHIND NORMAL SHOCK  
 FROZEN EXPANSION--EQUILIBRIUM POST SHOCK

# APPENDIX C - Continued

P	RHO	T	H	Z	GAME	A	QT	RN
1.112E+00	6.112E-07	4.419E+03	1.538E+07	2.149E+00	1.079E+00	1.4C1E+03	9.489E+C4	1.270E-02

## MARS

STATIC(55) CONDITIONS BEHIND NORMAL SHOCK  
FROZEN EXPANSION-- FROZEN POST SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M	R5S/R5
9.841E-01	2.666E-07	1.780E+04	2.245E+07	5.886E+01	1.082E+00	1.324E+00	2.219E+C3	7.850E+02	3.538E-01	6.989E+00

STAGNATION(15) CONDITIONS BEHIND NORMAL SHOCK  
FROZEN EXPANSION-- FROZEN POST SHOCK

P	RHO	T	H	Z	GAME	A	QT	RN
1.069E+00	2.837E-07	1.818E+04	1.504E+07	1.082E+00	1.334E+00	2.242E+00	9.167E+04	1.270E-02

## 5 CONDITIONS FOR EQUILIBRIUM EXPANSION

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRE
2.389E+02	1.275E-03	9.775E+02	6.816E+C6	3.711E+01	1.000E+00	1.205E+00	4.751E+02	5.486E+03	1.155E+01	1.724E+05

## MOLE FRACTIONS IN REGION 5

SPECIE	MOLE FRACTION
A	1.4992E-01
O	2.3572E-11
O2	4.3383E-04
C	4.2866E-46
CO	2.3280E-08
CO2	8.4963E-01

STATIC(55) CONDITIONS BEHIND NORMAL SHOCK  
EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M	R5S/R5
3.634E+04	2.150E-02	4.783E+03	8.181E+06	5.558E+01	1.845E+00	1.352E+00	1.512E+03	3.254E+02	1.155E+01	1.686E+01

STAGNATION(15) CONDITIONS BEHIND NORMAL SHOCK  
EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK

# APPENDIX C - Continued

P	RHC	T	H	Z	GAME	A	QT	RN
3.749E+04	2.200E-02	4.821E+03	8.234E+06	1.845E+00	1.354E+00	1.519E+03	1.197E+07	1.270E-02

MOLE FRACTIONS IN REGION 15

MARS

SPECIE MOLE FRACTION

A	8.1293E-02
n	4.5554E-01
n2	2.5091E-03
C	1.0558E-04
C2	4.5987E-01
CN2	6.8025E-04

03/03/72

EXPANSION TUBE PROGRAM OF MILLER FOR GAS MIXTURES  
ALL PHYSICAL QUANTITIES IN MKS UNITS- NASA SP-7012

VENUS

## SHOCK TUBE PHASE OF PROGRAM

## MEASURED INPUTS FOR SHOCK TUBE PHASE

RUN	P1	T1	LS1	P2	P4	T4
1.000E+00	3.447E+03	3.0CCE+02	0.	0.	6.895E+07	6.000E+02

WD	XCO2	XN2	XO2	XAR	XHE	XH2
4.321E+01	5.500E-01	5.00CE-02	0.	0.	0.	0.

## 1 CONDITIONS - QUIESCENT TEST GAS

P	RHO	T	H	GAM	A
3.447E+03	5.972E-02	3.0CCE+02-E	386E+06	1.250E+00	2.729E+02

## IMPERFECT HELIUM DRIVER GAS

## 4 CONDITIONS

P	RHO	T	F	S/R	Z	A	W
6.895E+07	4.858E+01	6.00CE+02	3.31E+06	1.040E+01	1.139E+00	1.613E+03	4.003E+00

## 2 CONDITIONS- REAL GAS MIXTURES

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRE
4.874E+05	8.272E-01	2.752E+03-4	4.42E+06	4.042E+01	1.097E+00	1.107E+00	8.076E+02	2.742E+02	3.395E+00	2.844E+07

## RATIO- 2 CONDITIONS TO 1 CONDITIONS

P	RHO	T	H	MS1	US1
1.414E+02	1.385E+01	9.3C7E+CC	4.820E-01	1.083E+01	2.955E+03

## MOLE FRACTIONS IN REGION 2

## VENUS

SPECIE MOLE FRACTION

E-	9.9109E-1C
A	1.1821E-1E
A+	1.4651E-35
A++	1.3877E-74
N	3.1053E-C7
N+	2.3632E-22
N++	3.3090E-65
N2	4.2888E-02
N2+	4.0451E-19
N	6.7022E-03
O+	4.6853E-17
O++	2.5384E-6C
O-	3.6017E-11
O2	7.8751E-C2
O2+	8.0586E-13
O2-	1.6275E-1C
N3	5.4072E-C3
N3+	1.1890E-C9
C	4.5055E-13
C+	8.2381E-23
C++	7.7964E-57
C-	9.7942E-22
CO	1.6882E-01
CO+	9.3975E-16
CN	1.3376E-11
CO2	6.9743E-01

CONDITIONS BEHIND STANDING SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRE
5.890E+06	6.308E+00	3.791E+C3	-3.482E+05	4.335E+01	1.280E+00	1.134E+00	1.029E+00	3.596E+02	3.495E-01	2.257E+07

MOLE FRACTIONS BEHIND SHOCK AT SECCND DIA.



# APPENDIX C - Continued

## VENUS

SPECIE	MOLE FRACTION
F-	9.2727E-C8
A	1.0126E-18
A++	6.7632E-31
N	-2.6005E-58
N+	1.7939E-C5
N++	1.5273E-16
N2	-2.4764E-46
N2+	3.0123E-02
N	1.3661E-14
O+	5.0589E-02
O++	1.7404E-12
O-	-5.9480E-45
O2	2.8406E-C8
O2+	1.5937E-01
O2-	1.5586E-C9
NO	5.9187E-C8
NO+	1.7847E-02
C	1.7874E-C7
C+	2.7466E-09
C++	1.3460E-16
C-	-2.9732E-40
CO	6.9447E-16
CO+	3.8651E-01
CN	1.7564E-11
CO2	1.2612E-C8
	3.5554E-01

ASF IS NEGATIVE - FROZEN FLOW NOT CALCULATED

## 5 CONDITIONS FOR EQUILIBRIUM EXPANSION

P	RHO	T	F	S/R	Z	GAME	A	U	M	NRE
1.556E-01	1.195E-06	6.765E+02	-8.050E+06	4.335E+01	1.00CE+00	1.209E+00	3.968E+02	1.097E+04	2.765E+01	4.375E+02

## MOLE FRACTIONS IN REGION 5

SPECIE	MOLE FRACTION
--------	---------------

## VENUS

E-	6.2308E-55
A	1.2958E-18
A+	2.6673E-74
A++	0.
N	7.0939E-32
N+	7.5299E-75
N++	0.
N2	4.9978E-02
N2+	7.1814E-57
O	1.3441E-15
O+	2.1215E-56
O++	0.
O-	1.0380E-65
O2	4.3192E-04
O2+	6.6382E-33
O2-	2.3622E-57
NO	2.1880E-09
NO+	5.1831E-18
C	2.4817E-65
C+	1.9305E-92
C++	0.
C-	0.
CN	1.8813E-13
CO+	1.1911E-56
CN	8.4516E-56
CO2	9.4959E-01

STATIC(S5) CONDITIONS BEHIND NORMAL SHOCK  
EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK

P	RHC	T	H	S/R	Z	GAME	A	U	M	R5S/R5
1.375E+02	2.688E-05	7.847E+03	5.20CE+07	1.126E+02	3.388E+00	1.147E+00	2.422E+03	4.875E+02	2.765E+01	2.250E+01

STAGNATION(T5) CONDITIONS BEHIND NORMAL SHOCK  
EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK

P	RHO	T	H	Z	GAME	A	QT	RN
1.407E+02	2.743E-05	7.864E+03	5.212E+07	3.391E+00	1.147E+00	2.426E+03	2.729E+06	1.270E-02

MOLE FRACTIONS IN REGION T5

## VENUS

SPECIE	MOLE FRACTION
E-	1.2986E-01
A	3.7866E-19
A+	3.6284E-21
A+	2.0861E-31
N	2.8883E-02
N+	6.0619E-04
N+	8.4244E-16
N2	1.7803E-07
N2+	1.2332E-09
O	5.5125E-01
O+	9.2424E-03
O+	1.3228E-17
O-	1.5704E-07
O2	9.3945E-08
O2+	2.9507E-08
O2-	4.1198E-14
NO	1.3768E-07
NO+	5.7027E-07
C	1.6008E-01
C+	1.2001E-01
C+	9.5579E-11
C-	3.1327E-08
CO	6.6521E-05
CO+	2.9096E-06
CN	1.2830E-07
CO2	2.8311E-12

03/06/72

## JOVIAN

EXPANSION TUBE PROGRAM OF MILLER FOR GAS MIXTURES.  
ALL PHYSICAL QUANTITIES IN MKS. UNITS- NASA SP-7012

## SHOCK TUBE PHASE OF PROGRAM

## MEASURED INPUTS FOR SHOCK TUBE PHASE

RUN	P1	T1	U1	P2	P4	T4
1.000E+00	3.447E+03	3.000E+02	0.	0.	6.895E+07	6.000E+02

WO	XC02	0.	XN2	0.	XO2	0.	XAP	XHE	XH2
3.009E+00	0.	0.	0.	0.	0.	0.	5.000E-01	5.000E-01	5.000E-01

## 1 CONDITIONS - QUIESCENT TEST GAS

P	RHO	T	H	GAM	A
3.447E+03	4.159E-03	3.000E+02	2.486E+06	1.500E+00	1.115E+03

## IMPERFECT HYDROGEN CRIVER GAS

## 4 CONDITIONS

P	RHO	T	H	S/R	Z	A	M
6.895E+07	2.173E+01	6.000E+02	9.245E+06	1.160E+01	1.282E+00	2.402E+03	2.016E+00

## 2 CONDITIONS- REAL GAS MIXTURES

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRE
1.542E+05	2.086E-02	2.657E+03	2.422E+07	2.266E+01	1.007E+00	1.306E+00	3.107E+03	5.387E+03	1.734E+00	1.705E+06

## RATIO- 2 CONDITIONS TO 1 CONDITIONS

P	RHO	T	H	WSI	USI
4.473E+01	5.016E+00	8.857E+00	9.740E+00	6.034E+00	6.728E+03

## MOLE FRACTIONS IN REGION 2

SPECIE MOLE FRACTION									
JOVIAN									
E-	6.8683E-14								
HE	4.9660E-01								
HE+	5.3516E-32								
HE++	0.								
H	1.3606E-02								
H+	6.8683E-14								
H2	4.8580E-01								
CONDITIONS BEHIND STANDING SHOCK									
P	PHO	T	H	S/R	Z	GAME	A	U	M
5.209E+05	5.288E-02	3.433E+03	3.647E+07	2.287E+01	1.038E+00	1.233E+00	3.484E+03	2.124E+03	6.096E-01
									1.432E+06
MOLE FRACTIONS BEHIND SHOCK AT SECOND DIA.									
SPECIE MOLE FRACTION									
E-	9.4645E-11								
HE	4.8148E-01								
HE+	6.2390E-25								
HE++	-5.5034E-91								
H	7.4C80E-02								
H+	9.4645E-11								
H2	4.4444E-01								
5 CONDITIONS FOR FROZEN EXPANSION									
P	RHO	T	H	S/R	Z	GAME	A	U	M
7.559E+02	7.063E-04	3.730E+02	3.729E+06	2.287E+01	1.038E+00	1.514E+00	1.273E+03	1.219E+04	9.577E+00
									5.064E+05
STATIC(55) CONDITIONS BEHIND NORMAL SHOCK									
FROZEN EXPANSION--EQUILIBRIUM POST SHOCK									
P	RHO	T	H	S/R	Z	GAME	A	U	M
9.437E+04	6.511E-03	4.123E+03	7.933E+07	2.886E+01	1.272E+00	1.206E+00	4.181E+03	1.322E+03	3.161E-01
									R55/R5
									9.218E+00
STAGNATION(15) CONDITIONS BEHIND NORMAL SHOCK									
FROZEN EXPANSION--EQUILIBRIUM POST SHOCK									
P	RHO	T	H	S/R	Z	GAME	A	QT	RN
1.002E+05	6.843E-03	4.153E+03	8.021E+07	1.276E+01	1.208E+00	4.206E+03	4.138E+07	1.270E-02	

## JOVIAN

STATIC(5S) CONDITIONS BEHIND NORMAL SHOCK  
FROZEN EXPANSION-- FROZEN POST SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M	R5S/R5
8.336E+04	3.313E-03	8.771E+03	8.768E+07	2.747E+01	1.038E+00	1.514E+00	6.173E+03	2.600E+03	4.211E-01	4.690E+00

STAGNATION(T5) CONDITIONS BEHIND NORMAL SHOCK  
FROZEN EXPANSION-- FROZEN POST SHOCK

P	RHO	T	H	Z	GAME	A	OT	RN
9.506E+04	3.613E-03	9.171E+03	7.805E+07	1.038E+00	1.514E+00	6.312E+03	3.919E+07	1.270E-02

5 CONDITIONS FOR EQUILIBRIUM EXPANSION

P	RHO	T	H	S/R	Z	GAME	A	U	M	NRE
3.630E+03	1.416E-03	9.278E+02	7.684E+06	2.287E+01	1.000E+00	1.489E+00	1.954E+03	1.219E+04	6.241E+00	5.354E+05

MOLE FRACTIONS IN REGION 5

SPECIE	MOLE FRACTION
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E-	9.5169E-63
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HE	5.0000E-01
----	------------

HE+	1.5027E-69
-----	------------

HE++	0.
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H	5.2877E-10
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H+	9.0285E-20
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H2	5.0000E-01
----	------------

STATIC(5S) CONDITIONS BEHIND NORMAL SHOCK  
EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK

P	RHO	T	H	S/R	Z	GAME	A	U	M	R5S/R5
1.903E+05	1.251E-02	4.337E+03	8.105E+07	2.811E+01	1.270E+00	1.218E+00	4.304E+03	1.380E+03	6.241E+00	8.833E+00

STAGNATION(T5) CONDITIONS BEHIND NORMAL SHOCK  
EQUILIBRIUM EXPANSION--EQUILIBRIUM POST SHOCK

P	RHO	T	H	Z	GAME	A	OT	RN
2.025E+05	1.316E-02	4.373E+03	8.201E+07	1.273E+00	1.220E+00	4.332E+03	6.019E+07	1.270E-02

MOLE FRACTIONS IN REGION T5

SPECIE	MOLE FRACTION
--------	---------------

E-	6.8156E-08	JOVIAN
HE	3.9264E-01	
HE+	2.3530E-19	
HE++	4.0286E-72	
H	4.2944E-01	
H+	6.8156E-08	
H2	1.7792E-01	

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TABLE I.- CALCULATED EXPANSION-TUBE FLOW QUANTITIES FOR SIX-SPECIES

## AIR MODEL IN THERMOCHEMICAL EQUILIBRIUM

[78% N<sub>2</sub>, 21% O<sub>2</sub>, 1% Ar, by volume;  $p_4 = 34.474 \text{ MN/m}^2$ ;

$T_4 = T_1 = T_{10} = 300 \text{ K}$ ;  $W_4 = W_{10} = 4.003 \text{ kg/kmol}$ ;

$W_1 = 28.97 \text{ kg/kmol}$ ]

$U_5$ , km/sec	$P_5$ , kN/m <sup>2</sup>	$T_5$ , K	$Z^*_5$	$\gamma_{E,5}$	$M_5$	$N_{Re,5}$ , m <sup>-1</sup>	$P_{5,t}$ , kN/m <sup>2</sup>	$\dot{q}_{5,t}$ , MW/m <sup>2</sup>	$P_{10}$ , N/m <sup>2</sup>
$p_1 = 861.9 \text{ N/m}^2$ ; $p_2 = 58.25 \text{ kN/m}^2$ ; $T_2 = 2766 \text{ K}$ ; $Z^*_2 = 1.013$ ; $U_{s,1} = 2.579 \text{ km/sec}$ ; $U_2 = 2.223 \text{ km/sec}$ ; $p_{2,s} = 326.2 \text{ kN/m}^2$ ; $T_{2,s} = 3680 \text{ K}$ ; $Z^*_{2,s} = 1.071$									
4.267	3.727	1924	1.000	1.271	5.094	$4.547 \times 10^5$	119.2	12.74	120.2 to 123.3
4.877	1.396	1545	1.000	1.301	6.420	2.803	72.62	12.03	31.20 to 35.65
5.486	.4560	1184	1.000	1.323	8.183	1.587	39.18	10.64	7.476 to 9.248
6.096	.1229	852.1	1.000	1.349	10.61	.8080	18.12	8.663	2.016 to 2.028
$p_1 = 3.447 \text{ kN/m}^2$ ; $p_2 = 190.4 \text{ kN/m}^2$ ; $T_2 = 2495 \text{ K}$ ; $Z^*_2 = 1.002$ ; $U_{s,1} = 2.345 \text{ km/sec}$ ; $U_2 = 1.991 \text{ km/sec}$ ; $p_{2,s} = 940.4 \text{ kN/m}^2$ ; $T_{2,s} = 3450 \text{ K}$ ; $Z^*_{2,s} = 1.028$									
4.267	5.871	1305	1.000	1.315	6.079	$13.59 \times 10^5$	276.8	18.03	189.4 to 194.2
4.877	1.706	962.5	1.000	1.339	8.019	7.316	142.5	15.97	38.11 to 43.55
5.486	.3869	652.9	1.000	1.370	10.83	3.536	60.29	12.71	6.343 to 7.847
6.096	.05869	386.8	1.000	1.396	15.48	1.475	19.06	8.656	.9621 to .9679
$p_1 = 6.895 \text{ kN/m}^2$ ; $p_2 = 335.9 \text{ kN/m}^2$ ; $T_2 = 2291 \text{ K}$ ; $Z^*_2 = 1.001$ ; $U_{s,1} = 2.207 \text{ km/sec}$ ; $U_2 = 1.861 \text{ km/sec}$ ; $p_{2,s} = 1.559 \text{ MN/m}^2$ ; $T_{2,s} = 3243 \text{ K}$ ; $Z^*_{2,s} = 1.013$									
4.267	6.016	1002	1.000	1.336	6.885	$21.20 \times 10^5$	369.4	20.11	194.1 to 199.0
4.877	1.415	688.3	1.000	1.366	9.389	10.52	165.2	16.79	31.62 to 36.13
5.486	.2283	416.1	1.000	1.394	13.45	4.541	55.82	12.04	3.742 to 4.630
6.096	.01908	205.1	1.000	1.401	21.23	1.481	11.69	6.712	.3129 to .3148

TABLE II. - CALCULATED EXPANSION-TUBE FLOW QUANTITIES FOR FIVE-SPECIES  
PURE CO<sub>2</sub> IN THERMOCHEMICAL EQUILIBRIUM

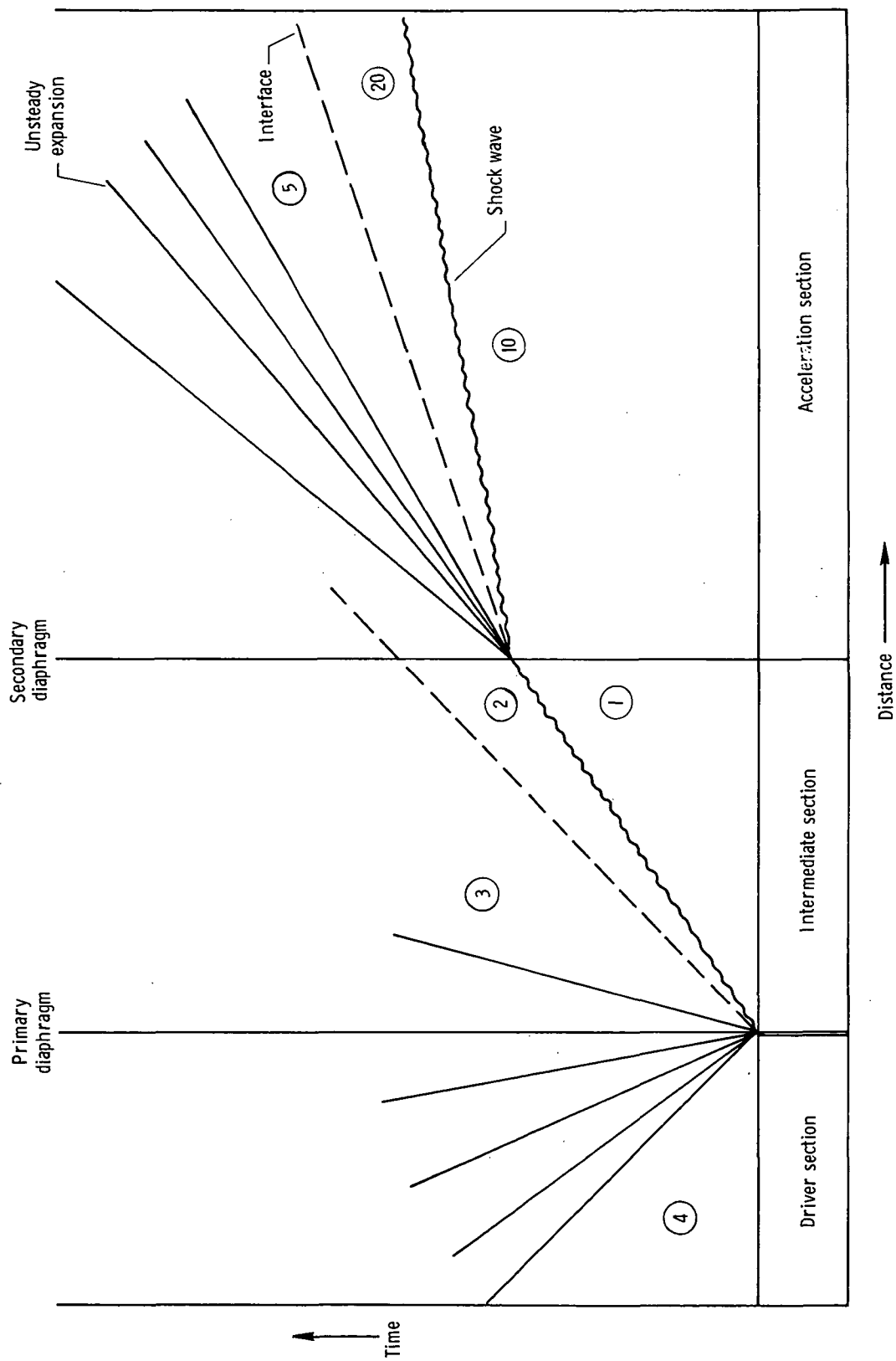
$$\left[ p_4 = 34.474 \text{ MN/m}^2; T_4 = T_1 = T_{10} = 300 \text{ K}; W_4 = W_{10} = 4.003 \text{ kg/kmol}; \right. \\ \left. W_1 = 44.011 \text{ kg/kmol} \right]$$

$U_5$ , km/sec	$p_5$ , kN/m <sup>2</sup>	$T_5$ , K	$Z^*_5$	$\gamma_{E,5}$	$M_5$	$N_{Re,5}$ , m <sup>-1</sup>	$p_{5,t}$ , kN/m <sup>2</sup>	$\dot{q}_{5,t}$ , MW/m <sup>2</sup>	$p_{10}$ , N/m <sup>2</sup>
$p_1 = 861.9 \text{ N/m}^2; p_2 = 79.10 \text{ kN/m}^2; T_2 = 2275 \text{ K}; Z^*_2 = 1.032; U_{s,1} = 2.371 \text{ km/sec};$ $U_2 = 2.169 \text{ km/sec}; p_{2,s} = 797.9 \text{ kN/m}^2; T_{2,s} = 2990 \text{ K}; Z^*_{2,s} = 1.138$									
4.267	2.131	1933	1.019	1.107	6.649	$4.016 \times 10^5$	101.2	13.71	68.75 to 70.51
4.877	.7220	1749	1.008	1.122	7.977	1.864	49.99	11.70	16.13 to 18.44
5.486	.2251	1534	1.002	1.147	9.506	.8214	22.62	9.478	3.689 to 4.565
6.096	.06330	1291	1.001	1.169	11.41	.3428	9.352	7.272	1.038 to 1.044
$p_1 = 3.447 \text{ kN/m}^2; p_2 = 253.2 \text{ kN/m}^2; T_2 = 2084 \text{ K}; Z^*_2 = 1.009; U_{s,1} = 2.130 \text{ km/sec};$ $U_2 = 1.927 \text{ km/sec}; p_{2,s} = 2.230 \text{ MN/m}^2; T_{2,s} = 2844 \text{ K}; Z^*_{2,s} = 1.070$									
4.267	3.336	1479	1.001	1.162	7.485	$10.08 \times 10^5$	210.7	18.33	107.6 to 110.4
4.877	.9050	1226	1.000	1.173	9.352	4.267	90.07	14.80	20.22 to 23.10
5.486	.2127	985.6	1.000	1.182	11.69	1.608	33.33	11.00	3.486 to 4.313
6.096	.04114	759.3	1.000	1.197	14.71	.5373	10.33	7.390	.6744 to .6784
$p_1 = 6.895 \text{ kN/m}^2; p_2 = 441.6 \text{ kN/m}^2; T_2 = 1929 \text{ K}; Z^*_2 = 1.003; U_{s,1} = 1.993 \text{ km/sec};$ $U_2 = 1.793 \text{ km/sec}; p_{2,s} = 3.634 \text{ MN/m}^2; T_{2,s} = 2713 \text{ K}; Z^*_{2,s} = 1.042$									
4.267	3.300	1185	1.000	1.175	8.321	$14.41 \times 10^5$	260.3	19.61	106.5 to 109.2
4.877	.7534	946.4	1.000	1.184	10.60	5.447	97.17	14.96	16.84 to 19.24
5.486	.1405	722.3	1.000	1.200	13.56	1.800	30.05	10.23	2.304 to 2.850
6.096	.01944	511.0	1.000	1.227	17.71	.5133	7.255	6.105	.3188 to .3206

TABLE III.- CALCULATED EXPANSION-TUBE FLOW QUANTITIES FOR  
THREE-SPECIES PURE Ar IN THERMOCHEMICAL EQUILIBRIUM

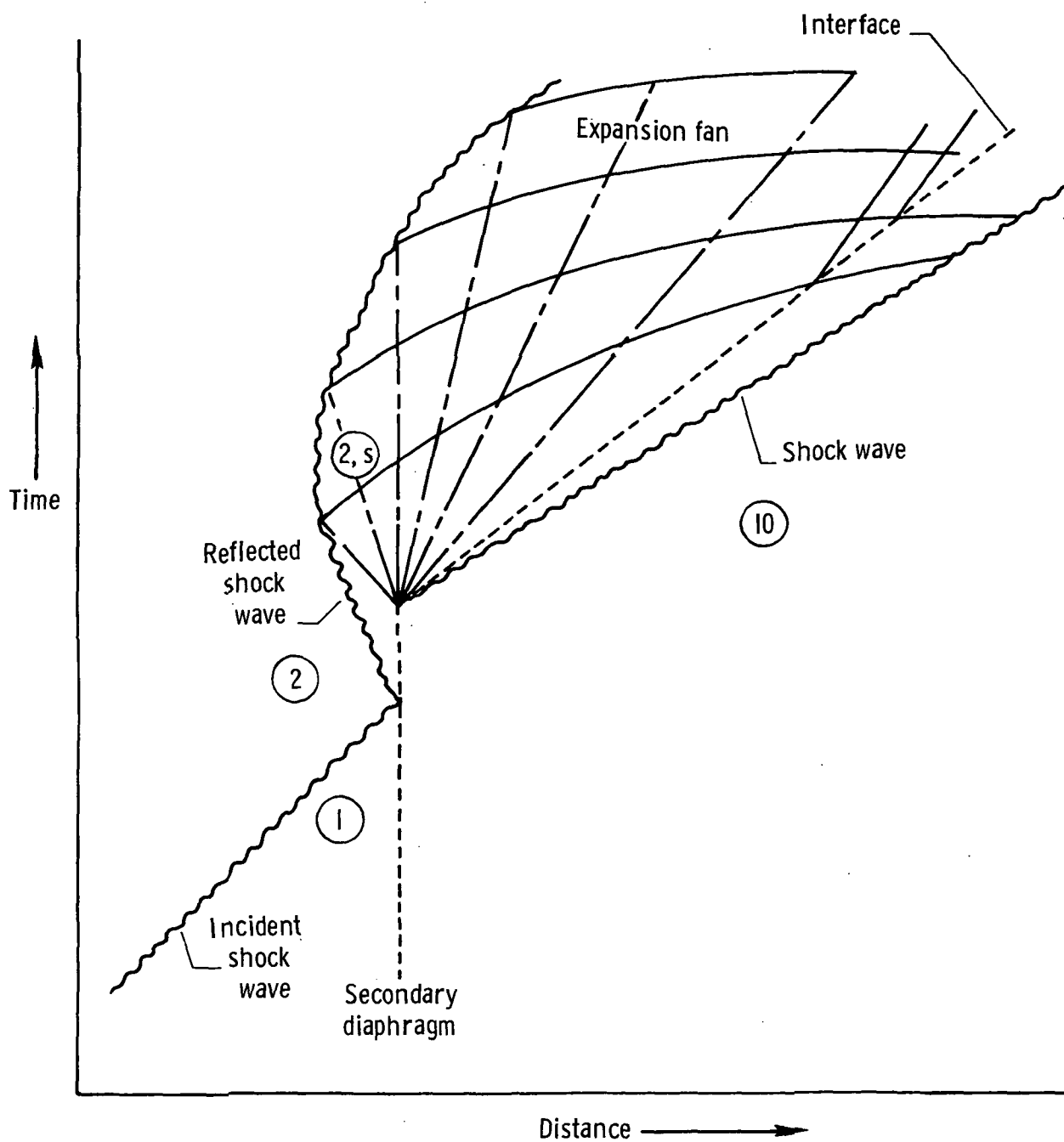
$$\left[ p_4 = 34.474 \text{ MN/m}^2; T_4 = T_1 = T_{10} = 300 \text{ K}; W_4 = W_{10} = 4.003 \text{ kg/kmol}; \right. \\ \left. W_1 = 39.944 \text{ kg/kmol} \right]$$

$U_5$ , km/sec	$p_5$ , N/m <sup>2</sup>	$T_5$ , K	$Z^*_5$	$\gamma_{E,5}$	$M_5$	$N_{Re,5}$ , m <sup>-1</sup>	$p_{5,t}$ , kN/m <sup>2</sup>	$\dot{q}_{5,t}$ , MW/m <sup>2</sup>	$p_{10}$ , N/m <sup>2</sup>
$p_1 = 861.9 \text{ N/m}^2; p_2 = 86.82 \text{ kN/m}^2; T_2 = 7723 \text{ K}; Z^*_2 = 1.001; U_{s,1} = 2.893 \text{ km/sec};$ $U_2 = 2.153 \text{ km/sec}; p_{2,s} = 192.9 \text{ kN/m}^2; T_{2,s} = 9779 \text{ K}; Z^*_{2,s} = 1.012$									
4.267	5602	2659	1.000	1.667	4.443	$3.820 \times 10^5$	178.8	21.23	180.6 to 185.3
4.877	1706	1653	1.000	1.667	6.440	3.041	114.4	20.71	38.13 to 43.57
5.486	357.6	884.7	1.000	1.667	9.903	2.125	56.70	17.77	5.863 to 7.254
6.096	36.36	354.6	1.000	1.667	17.38	1.177	17.76	12.05	.5961 to .5997
$p_1 = 3.447 \text{ kN/m}^2; p_2 = 275.4 \text{ kN/m}^2; T_2 = 6267 \text{ K}; Z^*_2 = 1.000; U_{s,1} = 2.583 \text{ km/sec};$ $U_2 = 1.907 \text{ km/sec}; p_{2,s} = 518.2 \text{ kN/m}^2; T_{2,s} = 8065 \text{ K}; Z^*_{2,s} = 1.001$									
4.267	6245	1389	1.000	1.667	6.146	$13.17 \times 10^5$	381.4	29.04	201.4 to 206.6
4.877	1106	695.1	1.000	1.667	9.931	8.884	176.3	24.70	24.70 to 28.22
5.486	76.52	238.8	1.000	1.667	19.06	4.433	44.94	15.48	1.255 to 1.552
6.096	.1675	20.61	1.000	1.667	72.08	.7637	1.407	3.362	.002746 to .002762
$p_1 = 6.895 \text{ kN/m}^2; p_2 = 477.2 \text{ kN/m}^2; T_2 = 5469 \text{ K}; Z^*_2 = 1.000; U_{s,1} = 2.405 \text{ km/sec};$ $U_2 = 1.771 \text{ km/sec}; p_{2,s} = 871.6 \text{ kN/m}^2; T_{2,s} = 6999 \text{ K}; Z^*_{2,s} = 1.000$									
4.267	4775	873.0	1.000	1.667	7.754	$22.59 \times 10^5$	464.1	31.14	154.0 to 158.0
4.877	476.8	347.3	1.000	1.667	14.05	12.80	152.1	22.60	10.65 to 12.17
5.486	5.837	59.69	1.000	1.667	38.13	3.770	13.72	8.498	.09569 to .1184
6.096	.07358	10.37	1.000	1.667	101.6	1.108	1.229	3.141	.001206 to .001213



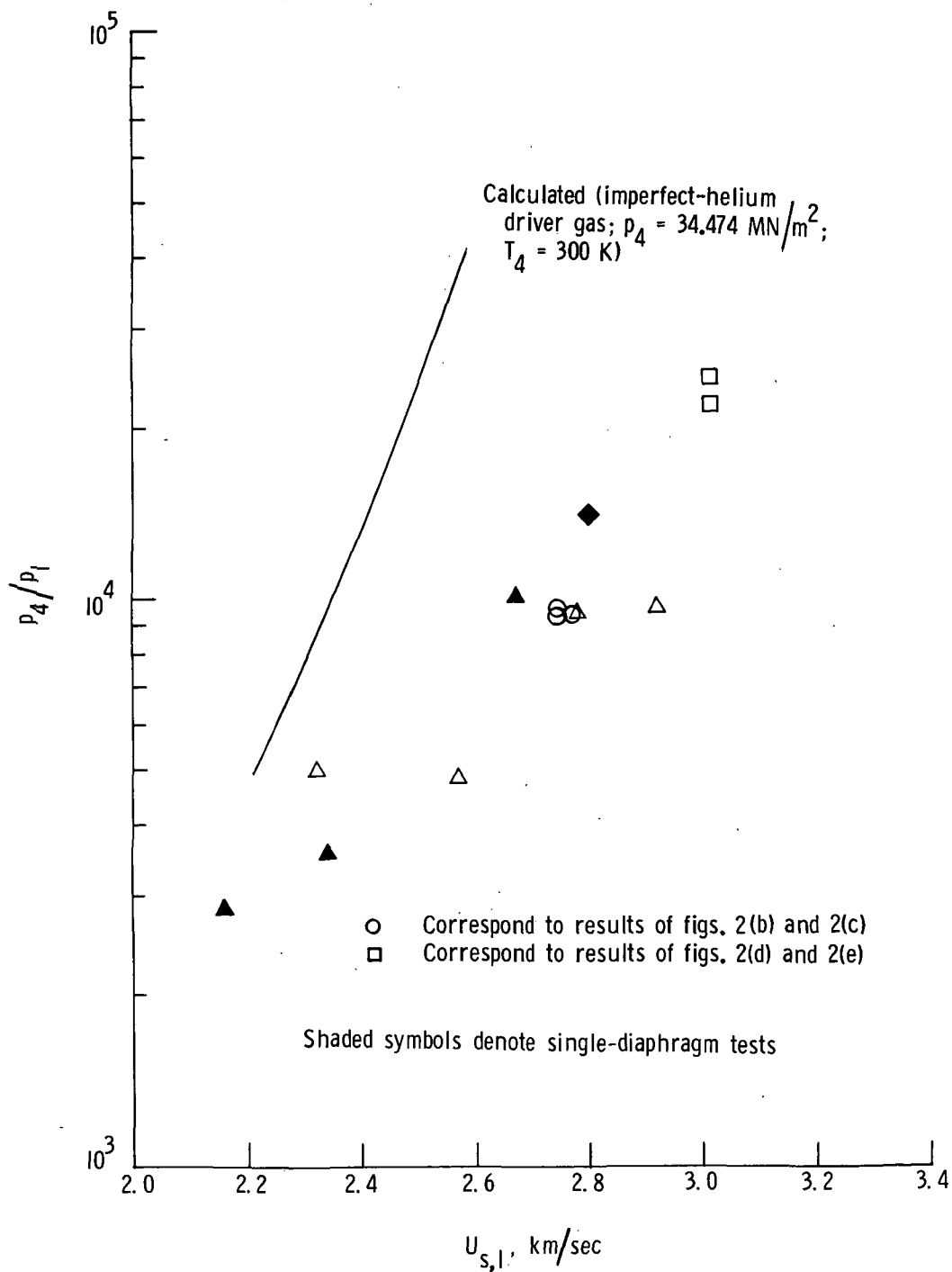
(a) No reflected shock at secondary diaphragm.

Figure 1.- Schematic diagram of expansion-tube flow sequence.



(b) Reflected shock at secondary diaphragm.

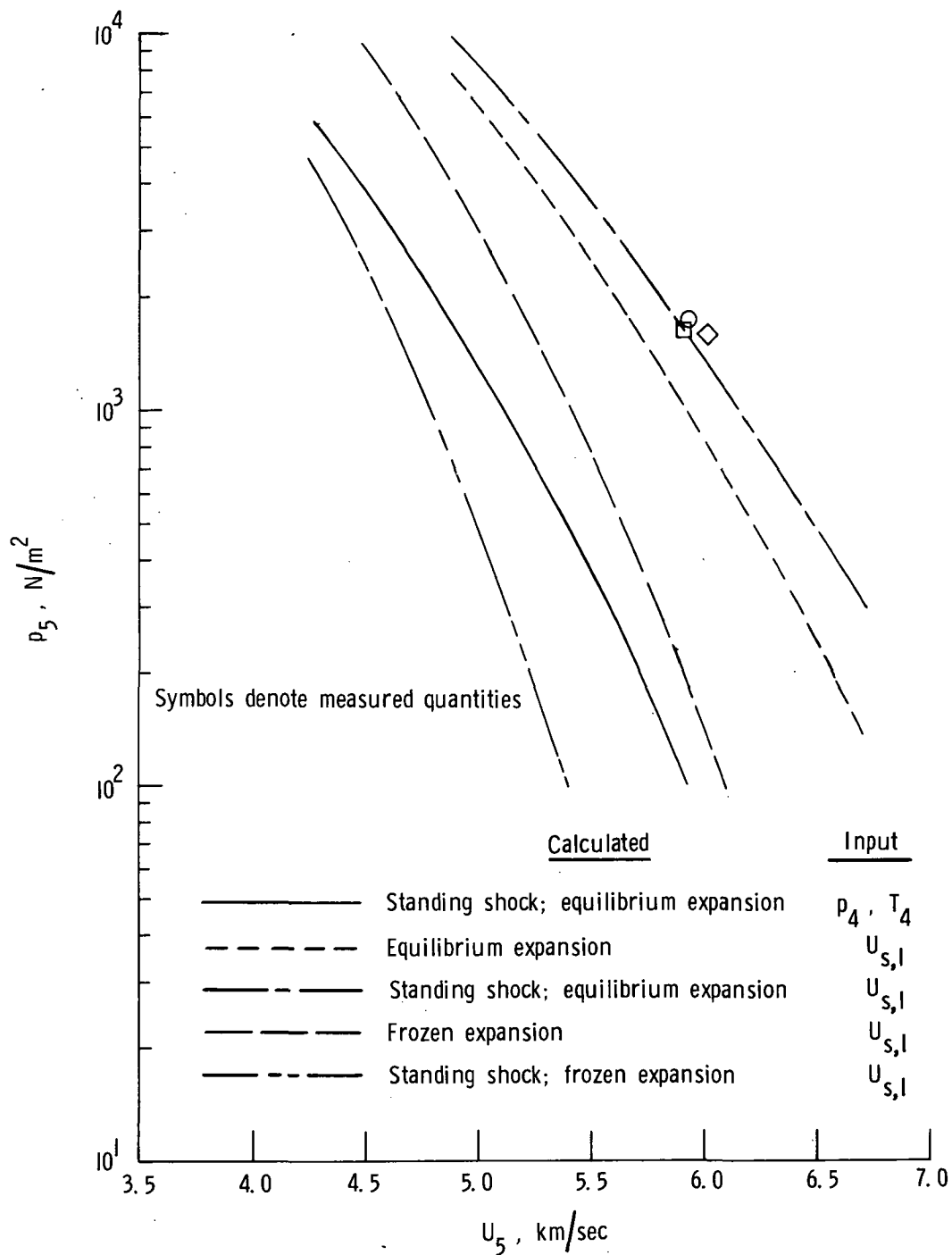
Figure 1.- Concluded.



(a) Incident-shock velocity as function of pressure ratio across primary diaphragm.

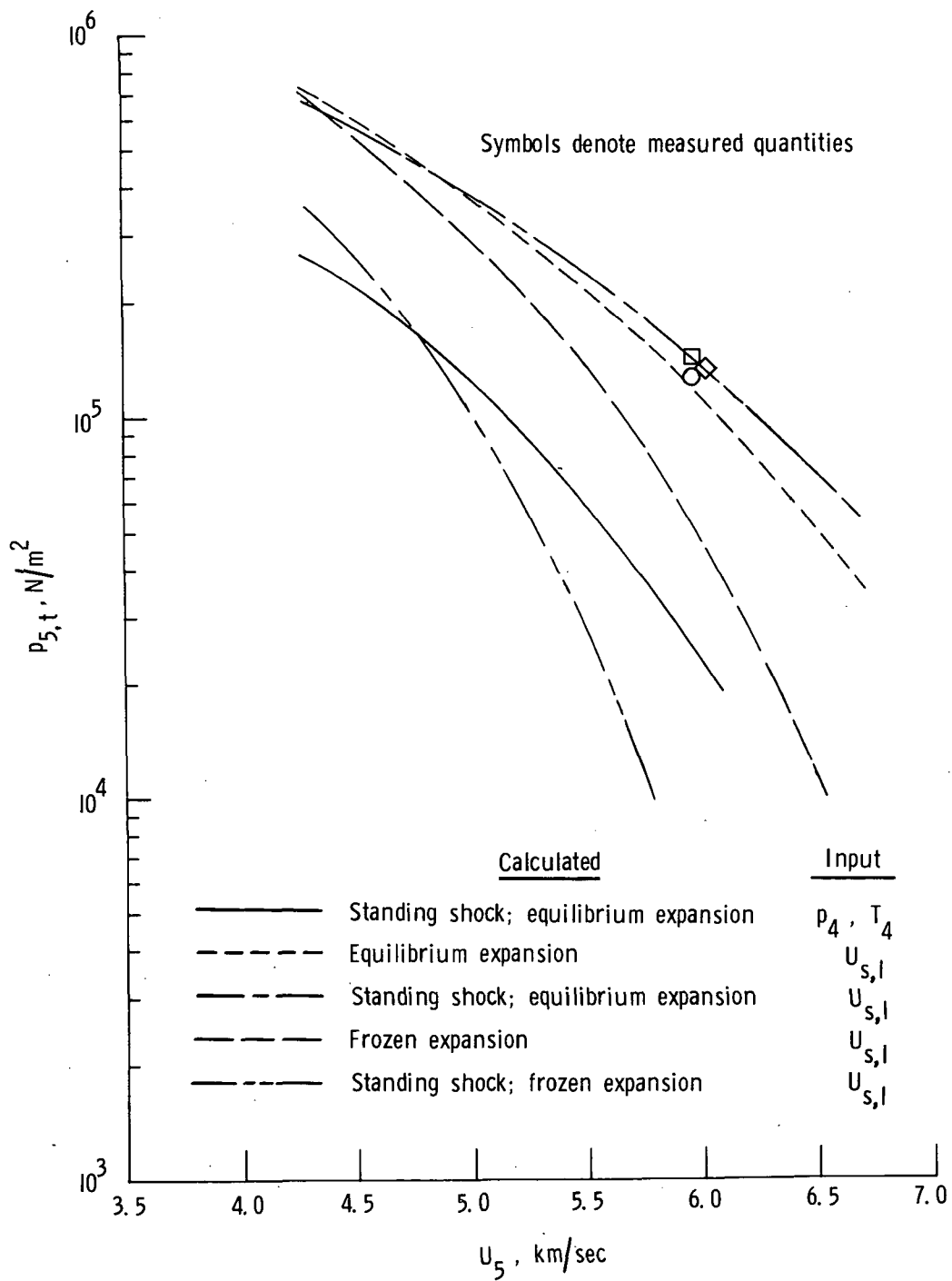
Figure 2.- Comparison of calculated and measured expansion-tube flow quantities for unheated helium driver gas and air test gas.





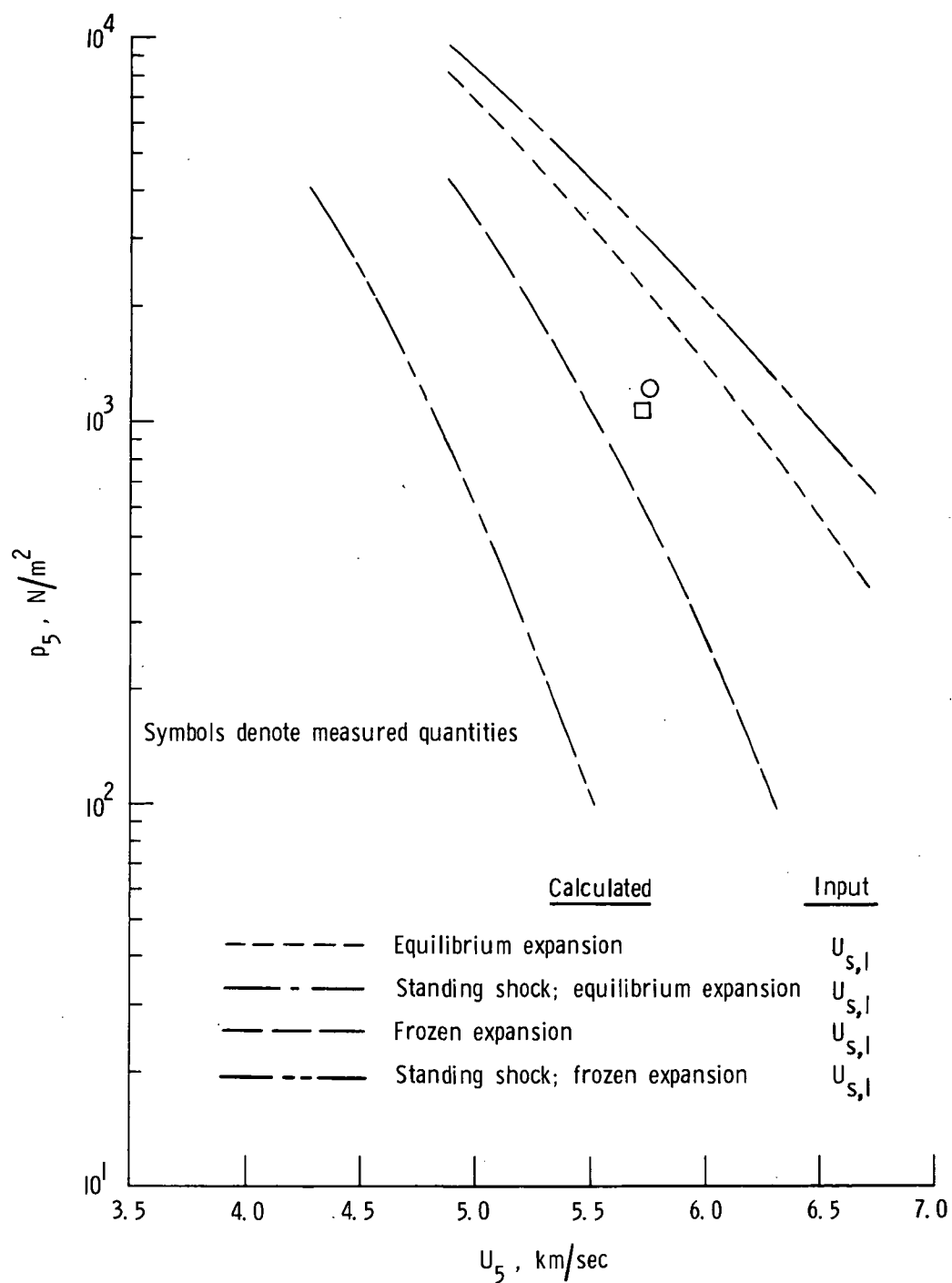
(b) Free-stream static pressure as function of free-stream velocity;  
 $p_1 = 3.447 \text{ kN/m}^2$ .

Figure 2.- Continued.



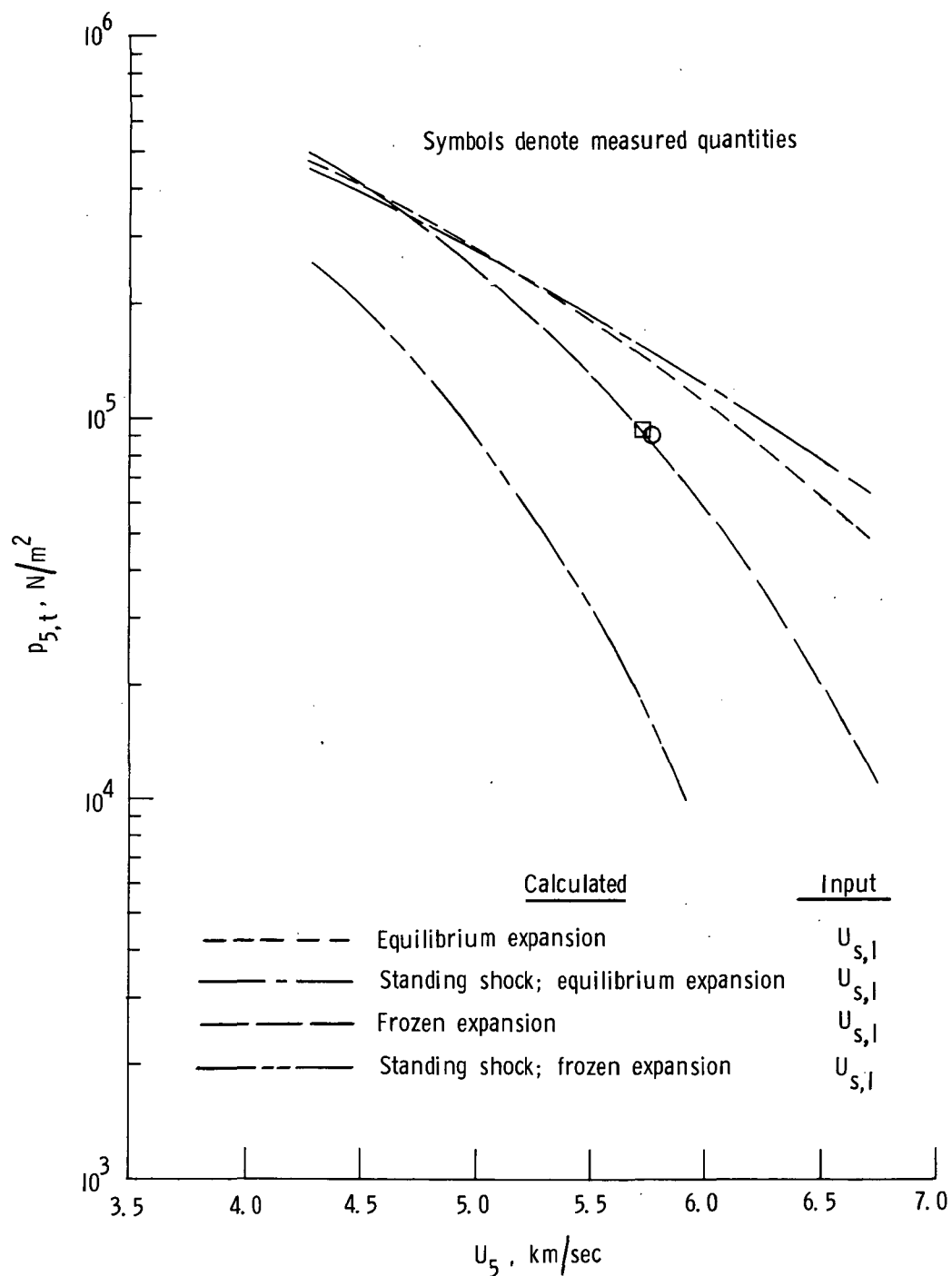
(c) Pitot pressure as function of free-stream velocity;  $p_1 = 3.447 \text{ kN/m}^2$ .

Figure 2.- Continued.



(d) Free-stream static pressure as function of free-stream velocity;  
 $p_1 = 1.379 \text{ kN/m}^2$ .

Figure 2.- Continued.



(e) Pitot pressure as function of free-stream velocity;  $p_1 = 1.379 \text{ kN/m}^2$ .

Figure 2.- Concluded.

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